

EOG Resources, Inc. 600 Seventeenth Street Suite 1000N Denver. CO 80202

Main: 303-572-9000 Fax: 303-824-5400

July 20, 2015

Attn: Cole Anderson, NSR Program Manager Wyoming Department of Environmental Quality Air Quality Division Herschler Building, 2-E 122 West 25th Street Cheyenne, Wyoming 82002

RE: E

EOG Resources, Inc.

Air Permit Application - Equipment Update at Fairway CS and Water Transfer Facility

Laramie County, Wyoming

Dear Mr. Anderson:

EOG Resources, Inc. (EOG) is submitting the enclosed application to update the equipment list at the Fairway Compressor Station to reflect the as built configuration by accounting for two (2) existing 0.50 MMBtu/hr tank heaters which were not included in the original permit application. This application is also requesting to include five (5) 6,000 gallon chemical storage tanks and an additional 400-bbl condensate storage tank with a 0.50 MMBtu/hr heater, include emissions associated with condensate liquid production, and to also include 500 hours of flaring due to routine maintenance. Emissions from the facility have been updated using new gas and condensate samples.

In addition, EOG is requesting to add a water transfer facility at the Fairway Compressor Station to store produced water from the wells in the surrounding field. This produced water will be stored in five (5) 500-bbl tanks prior to being pumped either to frac operations at new wells in the field or to the disposal facility in Colorado. The liquid in the tanks will be blanketed with natural gas and any emissions from the tanks will be routed to a 48" x 12' Cimarron enclosed combustion device for destruction. The transfer facility will also have a 0.25 MMBtu/hr line heater. This facility will handle up to 20,000-bbls per day of produced water.

The Fairway Compressor Station and Water Transfer Facility is located in the SW1/4NE1/4 of Section 36, T13N, R65W approximately thirteen (13) miles east-southeast of Chevenne, in Laramie County, Wyoming.

Attachment A contains a flow diagram/plot plan of the facility. Gas and oil analyses from the inlet of the compressor station are contained in Attachment B, and detailed emission calculations and supporting documentation are provided in Attachment C.

We trust the attached permit application package will meet your expectations and that you will not hesitate to call me at (303) 262-9946 or Mark Smith at (307) 823-6208 if you have any questions or need additional information. We appreciate your prompt attention to this most important project.

Sincerely,

Curtis Rice

EOG Environmental - Denver Division

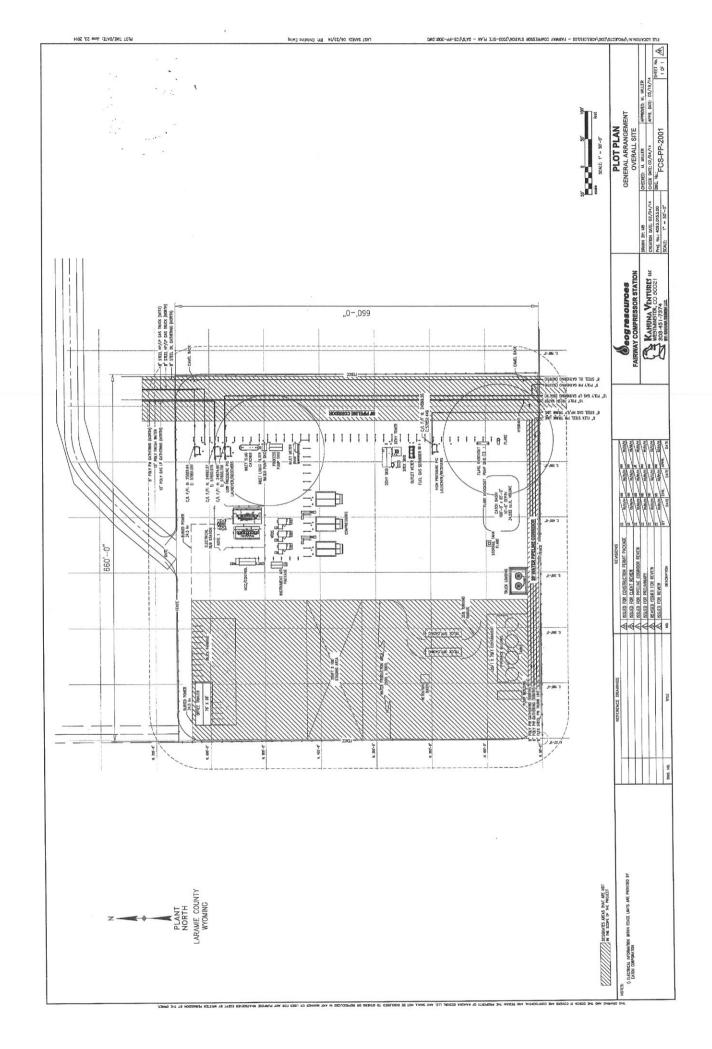
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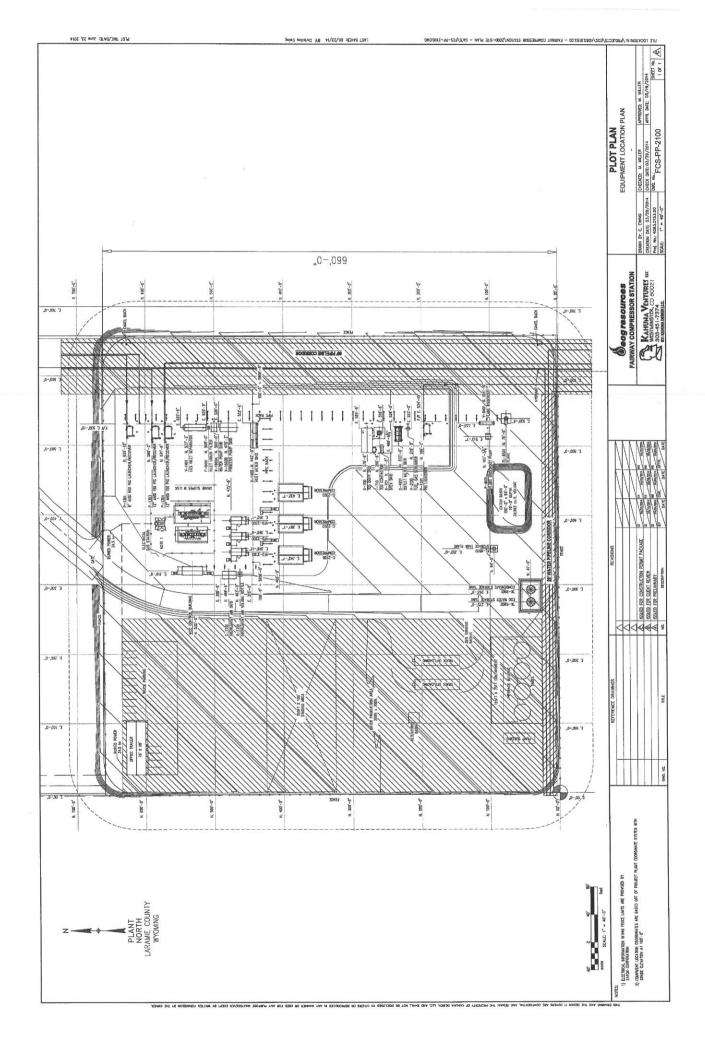
File - Well

Attachments: As stated

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Attachment A – Flow Diagram and Plot Plan of Emission Units and/or Facility





Attachment B – Gas/Oil Analyses



GAS MEASUREMENT EMISSIONS TESTING LABORATORY

307.856.0866 www.precision-labs.com

Client: EOG Resources Analysis Date: 2/6/2015

Sample ID: Pairway LCS Inlet Date Sampled: 2/6/2015

Unique #: 0 Purpose: NI

Sample Temperature: 44.5 DEG F Sample Pressure: 48.5 PSI

Sampled By: Don Heesch Type Sample: SPOT

County: Laramie

| Components | Mole % | Weight % | Liq. Vol. % |
|------------------------|---------|----------|-------------|
| Carbon Dioxide | 2.6062 | 4.136 | 2.082 |
| Nitrogen | 0.9044 | 0.914 | 0.466 |
| Methane | 60.5243 | 35.017 | 48.037 |
| Ethane | 12.5469 | 13.606 | 15.709 |
| Propane | 12.6560 | 20.126 | 16.324 |
| iso-Butane | 1.3642 | 2.860 | 2.090 |
| n-Butane | 4.9501 | 10.376 | 7.306 |
| iso-Pentane | 1.0322 | 2.686 | 1.767 |
| n-Pentane | 1.2482 | 3.248 | 2.118 |
| Cyclopentane | 0.0942 | 0.238 | 0.131 |
| n-Hexane | 0.4213 | 1.309 | 0.811 |
| Cyclohexane | 0.2358 | 0.716 | 0.375 |
| Other Hexanes | 0.4817 | 1.497 | 0.927 |
| Heptanes | 0.6081 | 2.197 | 1.313 |
| Methylcyclohexane | 0.1090 | 0.386 | 0.205 |
| 2,2,4-Trimethylpentane | 0.0002 | 0.001 | 0.000 |
| Benzene | 0.1382 | 0.389 | 0.181 |
| Toluene | 0.0386 | 0.128 | 0.060 |
| Ethylbenzene | 0.0020 | 0.008 | 0.004 |
| Xylenes | 0.0045 | 0.017 | 0.008 |
| Octanes | 0.0258 | 0.106 | 0.062 |
| Nonanes | 0.0061 | 0.028 | 0.016 |
| Decanes+ | 0.0021 | 0.011 | 0.006 |
| Totals | 100.000 | 100.000 | 100.000 |

ADDITIONAL BTEX DATA

| Components | Mole % | Weight % | Liq. Vol. % |
|------------------------|--------|----------|-------------|
| Cyclopentane | 0.094 | 0.238 | 0.131 |
| Cyclohexane | 0.236 | 0.716 | 0.375 |
| 2-Methylpentane | 0.303 | 0.942 | 0.584 |
| 3-Methylpentane | 0.179 | 0.555 | 0.344 |
| n-Hexane | 0.421 | 1.309 | 0.811 |
| Methylcyclohexane | 0.109 | 0.386 | 0.205 |
| 2,2,4-Trimethylpentane | 0.000 | 0.001 | 0.000 |
| Benzene | 0.138 | 0.389 | 0.181 |
| Toluene | 0.039 | 0.128 | 0.060 |
| Ethylbenzene | 0.002 | 800.0 | 0.004 |
| m-Xylene | 0.001 | 0.003 | 0.001 |
| p-Xylene | 0.003 | 0.012 | 0.005 |
| o-Xylene | 0.001 | 0.003 | 0.001 |

| SPECIFIC GRAVITY @ 60/60 F, calculated | 0.9574 |
|---------------------------------------------------------|----------|
| TOTAL GPM (Ethane Inclusive) | 10.522 |
| CALCULATED BTU / REAL CF @ 14.73 PSIA, dry basis | 1565.088 |
| CALCULATED BTU / REAL CF @ 14.73 PSIA, wet basis | 1538.579 |
| AVERAGE MOLECULAR WEIGHT | 27.729 |
| MOLAR MASS RATIO | 0.9570 |
| RELATIVE DENSITY (G x Z (Air) / Z), calculated | 0.9637 |
| IDEAL GROSS HEATING VALUE, BTU / IDEAL CF @ 14.696 PSIA | 1551.238 |
| COMPRESSIBILITY FACTOR (Z) | 0.99343 |
| | |
| | |
| PROPANE GPM | 3.4778 |
| BUTANE GPM | 2.0019 |
| GASOLINE GPM (PENTANE AND HEAVIER) | 1.6952 |
| VOC WEIGHT FRACTION | 0.463 |

NOTATION: ALL CALCULATIONS PERFORMED USING PHYSICAL CONSTANTS FROM GPA 2145-09, THE TABLES OF PHYSICAL CONSTANTS FOR HYDROCARBONS AND OTHER COMPOUNDS OF INTEREST TO THE NATURAL GAS INDUSTRY.



GAS MEASUREMENT EMISSIONS TESTING LABORATORY

307.856.0866 www.precision-labs.com

EXTENDED HYDROCARBON LIQUID STUDY CERTIFICATE OF ANALYSIS

Company:

EOG Resources-DJ Basin

Sample Name:

Condensate Fairway

Compressor Station Outlet

Date Sampled:

05/13/2015

Sample Number:

15051810-02

Sample Location:

Colorado

Date Tested:

05/18/2015

Sample Pressure:

25 PSI

Test Method:

GPA 2186M

Sample Temperature:

73 DEG F

Date Reported:

05/20/2015

County: Sample Source:

Separator Outlet

Note: Due to the nature of H2S, the values of

Sampling Method:

GPA-2174

H2S reported may be lower than actual.

Type Sample:

SPOT

Weld

| Carbon Dioxide 0.6524 0.327 0.271 Nitrogen 0.0577 0.018 0.015 Methane 1.1139 0.203 0.460 Ethane 2.0732 0.709 1.352 Propane 5.2406 2.629 3.520 iso-Butane 1.4738 0.975 1.176 n-Butane 8.4355 5.579 6.483 iso-Pentane 5.5618 4.566 4.959 n-Pentane 9.3226 7.654 8.238 Hexanes 8.7403 8.570 8.762 Heptanes 22.8087 26.006 25.654 Octanes 11.2371 14.606 14.034 Nonanes 2.2733 3.318 3.119 Decanes+ 1.9549 4.933 4.105 Benzene 1.3291 1.181 0.906 Toluene 5.5196 5.787 4.504 Ethylbenzene 0.3913 0.473 0.368 Xylenes 2.0472 2.473< | Components | Mole % | Weight % | Liq. Vol. % |
|--------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------|------------------------|---------|----------|-------------|
| Carbon Dioxide 0.6524 0.327 0.271 Nitrogen 0.0577 0.018 0.015 Methane 1.1139 0.203 0.460 Ethane 2.0732 0.709 1.352 Propane 5.2406 2.629 3.520 iso-Butane 1.4738 0.975 1.176 n-Butane 8.4355 5.579 6.483 iso-Pentane 5.5618 4.566 4.959 n-Pentane 9.3226 7.654 8.238 Hexanes 8.7403 8.570 8.762 Heptanes 22.8087 26.006 25.654 Octanes 11.2371 14.606 14.034 Nonanes 2.2733 3.318 3.119 Decanes+ 1.9549 4.933 4.105 Benzene 1.3291 1.181 0.906 Toluene 5.5196 5.787 4.504 Ethylbenzene 0.3913 0.473 0.368 Xylenes 2.0472 2.473< | Hydrogen Sulfide | 0.0000 | 0.000 | 0.000 |
| Nitrogen 0.0577 0.018 0.015 Methane 1.1139 0.203 0.460 Ethane 2.0732 0.709 1.352 Propane 5.2406 2.629 3.520 iso-Butane 1.4738 0.975 1.176 n-Butane 8.4355 5.579 6.483 iso-Pentane 5.5618 4.566 4.959 n-Pentane 9.3226 7.654 8.238 Hexanes 8.7403 8.570 8.762 Heptanes 22.8087 26.006 25.654 Octanes 11.2371 14.606 14.034 Nonanes 2.2733 3.318 3.119 Decanes+ 1.9549 4.933 4.105 Benzene 1.3291 1.181 0.906 Toluene 5.5196 5.787 4.504 Ethylbenzene 0.3913 0.473 0.368 Xylenes 2.0472 2.473 1.939 n-Hexane 8.4654 8.301 8.487 2,4-Trimethylpentane 1.3016 1.692 1.64 | Oxygen | 0.0000 | 0.000 | 0.000 |
| Methane 1.1139 0.203 0.460 Ethane 2.0732 0.709 1.352 Propane 5.2406 2.629 3.520 iso-Butane 1.4738 0.975 1.176 n-Butane 8.4355 5.579 6.483 iso-Pentane 5.5618 4.566 4.959 n-Pentane 9.3226 7.654 8.238 Hexanes 8.7403 8.570 8.762 Heptanes 22.8087 26.006 25.654 Octanes 11.2371 14.606 14.034 Nonanes 2.2733 3.318 3.119 Decanes+ 1.9549 4.933 4.105 Benzene 1.3291 1.181 0.906 Toluene 5.5196 5.787 4.504 Ethylbenzene 0.3913 0.473 0.368 Xylenes 2.0472 2.473 1.939 n-Hexane 8.4654 8.301 8.487 2,2,4-Trimethylpentane 1.3016 1.692 1.649 | Carbon Dioxide | 0.6524 | 0.327 | 0.271 |
| Ethane 2.0732 0.709 1.352 Propane 5.2406 2.629 3.520 so-Butane 1.4738 0.975 1.176 n-Butane 8.4355 5.579 6.483 so-Pentane 5.5618 4.566 4.959 n-Pentane 9.3226 7.654 8.238 Hexanes 8.7403 8.570 8.762 Heptanes 22.8087 26.006 25.654 Octanes 11.2371 14.606 14.034 Nonanes 2.2733 3.318 3.119 Decanes+ 1.9549 4.933 4.105 Benzene 1.3291 1.181 0.906 Toluene 5.5196 5.787 4.504 Ethylbenzene 0.3913 0.473 0.368 Xylenes 2.0472 2.473 1.939 n-Hexane 8.4654 8.301 8.487 2,2,4-Trimethylpentane 1.3016 1.692 1.649 | Nitrogen | 0.0577 | 0.018 | 0.015 |
| Propane 5.2406 2.629 3.520 so-Butane 1.4738 0.975 1.176 n-Butane 8.4355 5.579 6.483 so-Pentane 5.5618 4.566 4.959 n-Pentane 9.3226 7.654 8.238 Hexanes 8.7403 8.570 8.762 Heptanes 22.8087 26.006 25.654 Octanes 11.2371 14.606 14.034 Nonanes 2.2733 3.318 3.119 Decanes+ 1.9549 4.933 4.105 Benzene 1.3291 1.181 0.906 Toluene 5.5196 5.787 4.504 Ethylbenzene 0.3913 0.473 0.368 Xylenes 2.0472 2.473 1.939 n-Hexane 8.4654 8.301 8.487 2,2,4-Trimethylpentane 1.3016 1.692 1.649 | Methane | 1.1139 | 0.203 | 0.460 |
| so-Butane 1.4738 0.975 1.176 n-Butane 8.4355 5.579 6.483 so-Pentane 5.5618 4.566 4.959 n-Pentane 9.3226 7.654 8.238 Hexanes 8.7403 8.570 8.762 Heptanes 22.8087 26.006 25.654 Octanes 11.2371 14.606 14.034 Nonanes 2.2733 3.318 3.119 Decanes+ 1.9549 4.933 4.105 Benzene 1.3291 1.181 0.906 Toluene 5.5196 5.787 4.504 Ethylbenzene 0.3913 0.473 0.368 Xylenes 2.0472 2.473 1.939 n-Hexane 8.4654 8.301 8.487 2,2,4-Trimethylpentane 1.3016 1.692 1.649 | Ethane | 2.0732 | 0.709 | 1.352 |
| n-Butane 8.4355 5.579 6.483 so-Pentane 5.5618 4.566 4.959 n-Pentane 9.3226 7.654 8.238 Hexanes 8.7403 8.570 8.762 Heptanes 22.8087 26.006 25.654 Octanes 11.2371 14.606 14.034 Nonanes 2.2733 3.318 3.119 Decanes+ 1.9549 4.933 4.105 Benzene 1.3291 1.181 0.906 Toluene 5.5196 5.787 4.504 Ethylbenzene 0.3913 0.473 0.368 Kylenes 2.0472 2.473 1.939 n-Hexane 8.4654 8.301 8.487 2,2,4-Trimethylpentane 1.3016 1.692 1.649 | Propane | 5.2406 | 2.629 | 3.520 |
| so-Pentane 5.5618 4.566 4.959 n-Pentane 9.3226 7.654 8.238 Hexanes 8.7403 8.570 8.762 Heptanes 22.8087 26.006 25.654 Octanes 11.2371 14.606 14.034 Nonanes 2.2733 3.318 3.119 Decanes+ 1.9549 4.933 4.105 Benzene 1.3291 1.181 0.906 Toluene 5.5196 5.787 4.504 Ethylbenzene 0.3913 0.473 0.368 Xylenes 2.0472 2.473 1.939 n-Hexane 8.4654 8.301 8.487 2,2,4-Trimethylpentane 1.3016 1.692 1.649 | so-Butane | 1.4738 | 0.975 | 1.176 |
| n-Pentane 9.3226 7.654 8.238 Hexanes 8.7403 8.570 8.762 Heptanes 22.8087 26.006 25.654 Octanes 11.2371 14.606 14.034 Nonanes 2.2733 3.318 3.119 Decanes+ 1.9549 4.933 4.105 Benzene 1.3291 1.181 0.906 Toluene 5.5196 5.787 4.504 Ethylbenzene 0.3913 0.473 0.368 Kylenes 2.0472 2.473 1.939 n-Hexane 8.4654 8.301 8.487 2,2,4-Trimethylpentane 1.3016 1.692 1.649 | n-Butane | 8.4355 | 5.579 | 6.483 |
| Hexanes 8.7403 8.570 8.762 Heptanes 22.8087 26.006 25.654 Octanes 11.2371 14.606 14.034 Nonanes 2.2733 3.318 3.119 Decanes+ 1.9549 4.933 4.105 Benzene 1.3291 1.181 0.906 Toluene 5.5196 5.787 4.504 Ethylbenzene 0.3913 0.473 0.368 Kylenes 2.0472 2.473 1.939 n-Hexane 8.4654 8.301 8.487 2,2,4-Trimethylpentane 1.3016 1.692 1.649 | so-Pentane | 5.5618 | 4.566 | 4.959 |
| Heptanes 22.8087 26.006 25.654 Octanes 11.2371 14.606 14.034 Nonanes 2.2733 3.318 3.119 Decanes+ 1.9549 4.933 4.105 Benzene 1.3291 1.181 0.906 Toluene 5.5196 5.787 4.504 Ethylbenzene 0.3913 0.473 0.368 Kylenes 2.0472 2.473 1.939 n-Hexane 8.4654 8.301 8.487 2,2,4-Trimethylpentane 1.3016 1.692 1.649 | n-Pentane | 9.3226 | 7.654 | 8.238 |
| Octanes 11.2371 14.606 14.034 Nonanes 2.2733 3.318 3.119 Decanes+ 1.9549 4.933 4.105 Benzene 1.3291 1.181 0.906 Toluene 5.5196 5.787 4.504 Ethylbenzene 0.3913 0.473 0.368 Kylenes 2.0472 2.473 1.939 n-Hexane 8.4654 8.301 8.487 2,2,4-Trimethylpentane 1.3016 1.692 1.649 | Hexanes | 8.7403 | 8.570 | 8.762 |
| Nonanes 2.2733 3.318 3.119 Decanes+ 1.9549 4.933 4.105 Benzene 1.3291 1.181 0.906 Foluene 5.5196 5.787 4.504 Ethylbenzene 0.3913 0.473 0.368 Kylenes 2.0472 2.473 1.939 n-Hexane 8.4654 8.301 8.487 2,2,4-Trimethylpentane 1.3016 1.692 1.649 | Heptanes | 22.8087 | 26.006 | 25.654 |
| Decanes+ 1.9549 4.933 4.105 Benzene 1.3291 1.181 0.906 Toluene 5.5196 5.787 4.504 Ethylbenzene 0.3913 0.473 0.368 Kylenes 2.0472 2.473 1.939 n-Hexane 8.4654 8.301 8.487 2,2,4-Trimethylpentane 1.3016 1.692 1.649 | Octanes | 11.2371 | 14.606 | 14.034 |
| Benzene 1.3291 1.181 0.906 Toluene 5.5196 5.787 4.504 Ethylbenzene 0.3913 0.473 0.368 Xylenes 2.0472 2.473 1.939 n-Hexane 8.4654 8.301 8.487 2,2,4-Trimethylpentane 1.3016 1.692 1.649 | Nonanes | 2.2733 | 3.318 | 3.119 |
| Toluene 5.5196 5.787 4.504 Ethylbenzene 0.3913 0.473 0.368 Xylenes 2.0472 2.473 1.939 n-Hexane 8.4654 8.301 8.487 2,2,4-Trimethylpentane 1.3016 1.692 1.649 | Decanes+ | 1.9549 | 4.933 | 4.105 |
| Ethylbenzene 0.3913 0.473 0.368 Kylenes 2.0472 2.473 1.939 n-Hexane 8.4654 8.301 8.487 2,2,4-Trimethylpentane 1.3016 1.692 1.649 | Benzene | 1.3291 | 1.181 | 0.906 |
| Xylenes 2.0472 2.473 1.939 n-Hexane 8.4654 8.301 8.487 2,2,4-Trimethylpentane 1.3016 1.692 1.649 | Toluene | 5.5196 | 5.787 | 4.504 |
| n-Hexane 8.4654 8.301 8.487 2,2,4-Trimethylpentane 1.3016 1.692 1.649 | Ethylbenzene | 0.3913 | 0.473 | 0.368 |
| 2,2,4-Trimethylpentane 1.3016 1.692 1.649 | Xylenes | 2.0472 | 2.473 | 1.939 |
| | n-Hexane | 8.4654 | 8.301 | 8.487 |
| Totals 100,000 100,000 100.00 | 2,2,4-Trimethylpentane | 1.3016 | 1.692 | 1.649 |
| | Γotals | 100.000 | 100.000 | 100.000 |

ADDITIONAL BTEX DATA

| Components | Mole % | Weight % | Liq. Vol. % |
|------------------------|--------|----------|-------------|
| 2-Methylpentane | 6.249 | 6.128 | 6.265 |
| 3-Methylpentane | 2.491 | 2.443 | 2.497 |
| n-Hexane | 8.465 | 8.301 | 8.487 |
| 2,2,4-Trimethylpentane | 1.302 | 1.692 | 1.649 |
| Benzene | 1.329 | 1.181 | 0.906 |
| Toluene | 5.520 | 5.787 | 4.504 |
| Ethylbenzene | 0.391 | 0.473 | 0.368 |
| m-Xylene | 0.235 | 0.284 | 0.223 |
| p-Xylene | 1.464 | 1.768 | 1.386 |
| o-Xylene | 0.348 | 0.420 | 0.330 |

| RELATIVE SPECIFIC GRAVITY OF DECANES+ (C10+) FRACTION, calculated | 0.81583 |
|-------------------------------------------------------------------|------------|
| AVERAGE MOLECULAR WEIGHT | 87.883 |
| AVERAGE MOLECULAR WEIGHT OF DECANES+ (C10+) FRACTION, calculated | 221.759 |
| TRUE VAPOR PRESSURE AT 100 F, PSIA, calculated | 91.595 |
| AVERAGE BOILING POINT, F, calculated | 154.684 |
| CUBIC FEET OF GAS / GALLON OF LIQUID, as Ideal Gas, calculated | 24.634 |
| BTU / GALLON OF LIQUID AT 14.73 PSIA, calculated | 115,985.04 |
| LBS / GALLON OF LIQUID, calculated | 5.660 |

NOTATION: ALL CALCULATIONS PERFORMED USING PHYSICAL CONSTANTS FROM GPA 2145-09, THE TABLES OF PHYSICAL CONSTANTS FOR HYDROCARBONS AND OTHER COMPOUNDS OF INTEREST TO THE NATURAL GAS INDUSTRY.

FLASHED CRUDE OIL LIQUID STUDIES CERTIFICATE OF ANALYSIS

Sample Name:

Condensate Fairway Compressor Station Outlet

Sample Number:

15051810-02

| TEST PERFORMED | RESULTS | DATE TESTED |
|-----------------------------------------------------------|---------|-------------|
| API GRAVITY AT 60/60 F, (ASTM D-7777), calculated from SG | 66.5 | 05/20/2015 |
| REID VAPOR PRESSURE (ASTM D5191), PSI AT 100 F, measured | 10.41 | 05/20/2015 |

Attachment C – Emissions Calculations and Supporting Documentation

| Well Name: | Fairway CS Inlet | Composite Gas Analysis | | | |
|--------------------------------|------------------|------------------------|--------|-----------------|---------|
| Date Sampled: | 2/6/2015 | | | | |
| Component: | %low | %lom | M.W. | (mol% X MW)/100 | %LM |
| Hydrogen Sulfide (H2S) | 0.0000 | 0.0000 | 34.08 | 0.0000 | 0.00000 |
| Oxygen (O2) | 0.0000 | 0.0000 | 32.00 | 0.0000 | 0.00000 |
| Carbon Dioxide (CO2) | 2.6062 | 2.6062 | 44.01 | 1.1470 | 0.04137 |
| Nitrogen (N2) | 0.9044 | 0.9044 | 28.02 | 0.2534 | 0.00914 |
| Methane (C1) | 60.5243 | 60.5243 | 16.04 | 9.7081 | 0.35019 |
| Ethane (C2) | 12.5469 | 12.5469 | 30.07 | 3.7729 | 0.13609 |
| Propane (C3) | 12.6560 | 12.6560 | 44.09 | 5.5800 | 0.20128 |
| iso-Butane (i-C4) | 1.3642 | 1.3642 | 58.12 | 0.7929 | 0.02860 |
| n-Butane (nC-4) | 4.9501 | 4.9501 | 58.12 | 2.8770 | 0.10378 |
| iso-Pentane (i-C5) | 1.0322 | 1.0322 | 72.15 | 0.7447 | 0.02686 |
| n-Pentane (n-C5) | 1.2482 | 1.2482 | 72.15 | 9006.0 | 0.03249 |
| Cyclopentane | 0.0942 | 0.0942 | 70.1 | 0.0660 | 0.00238 |
| n-Hexane (n-C6) | 0.4213 | 0.4213 | 86.17 | 0.3630 | 0.01310 |
| Cyclohexane | 0.2358 | 0.2358 | 84.16 | 0.1984 | 0.00716 |
| Other Hexanes | 0.4817 | 0.4817 | 85.00 | 0.4094 | 0.01477 |
| Heptanes | 0.6081 | 0.6081 | 100.20 | 0.6093 | 0.02198 |
| Methylcyclohexane | 0.1090 | 0.1090 | 98.18 | 0.1070 | 0.00386 |
| 2,2,4-Trimethylpentane | 0.0002 | 0.0002 | 114.22 | 0.0002 | 0.00001 |
| Benzene | 0.1382 | 0.1382 | 78.11 | 0.1079 | 0.00389 |
| Toluene | 0.0386 | 0.0386 | 92.14 | 0.0356 | 0.00128 |
| Ethylbenzene | 0.0020 | 0.0020 | 106.17 | 0.0021 | 0.00008 |
| Xylene | 0.0045 | 0.0045 | 106.17 | 0.0048 | 0.00017 |
| Octanes | 0.0258 | 0.0258 | 120.00 | 0.0310 | 0.00112 |
| Nonanes | 0.0061 | 0.0061 | 128.26 | 0.0078 | 0.00028 |
| Decanes+ | 0.0021 | 0.0021 | 142.29 | 0.0030 | 0.00011 |
| Total | 100.000 | 100.0001 | M.W.= | 27.72 | |
| | | 1 | | | |
| Temperature (F) | 44.5 | 44.50 | | | |
| Pressure (psig) | 48.5 | 48.50 | | | |
| Molecular WT | 27.729 | 27.73 | | | |
| Higher Heating Value (Btu/scf) | 1565.09 | 1565.09 | | | |
| | | | | | |

46.32

Total VOC Weight Percent Total HAP Weight Percent

| v 103 | U. 1 SS 055000 | <u>190</u> |
|-------------------------|----------------|------------|
| Well Name: | Fairway CS | Composite |
| Date Sampled: | 5/18/2015 | |
| Component: | mole% | mole % |
| Hydrogen Sulfide (H2S) | 0.0000 | 0.0000 |
| Oxygen (O2) | 0.0000 | 0.0000 |
| Carbon Dioxide (CO2) | 0.6524 | 0.6524 |
| Nitrogen (N2) | 0.0577 | 0.0577 |
| Methane (C1) | 1.1139 | 1.1139 |
| Ethane (C2) | 2.0732 | 2.0732 |
| Propane (C3) | 5.2406 | 5.2406 |
| iso-Butane (i-C4) | 1.4738 | 1.4738 |
| n-Butane (nC-4) | 8.4355 | 8.4355 |
| iso-Pentane (i-C5) | 5.5618 | 5.5618 |
| n-Pentane (n-C5) | 9.3226 | 9.3226 |
| 2-Methylpentane (C6) | 6.2490 | 6.2490 |
| 3-Methylpentane (C6) | 2.4910 | 2.4910 |
| Heptanes (C7) | 22.8087 | 22.8087 |
| Octanes (C8) | 11.2371 | 11.2371 |
| Nonanes (C9) | 2.2733 | 2.2733 |
| Benzene | 1.3291 | 1.3291 |
| Toluene | 5.5196 | 5.5196 |
| Ethylbenzene | 0.3913 | 0.3913 |
| m-Xylene | 0.2350 | 0.2350 |
| p-Xylene | 1.4640 | 1.4640 |
| o-Xylene | 0.3480 | 0.3480 |
| n-Hexane | 8.4654 | 8.4654 |
| 2,2,4-Trimethylpentane | 1.3016 | 1.3016 |
| Decanes+ (C10+) | 1.9549 | 1.9549 |
| Total | 100.000 | 100.000 |
| Total | 100.000 | 100.000 |
| MW C10+ | 221.7590 | 221.7590 |
| Specific Gravity C10+ | 0.8158 | 0.8158 |
| API Gravity (sales oil) | 66.5 | 66.5000 |
| RVP (sales oil) | 10.41 | 10.4100 |
| Temperature (F) | 73 | 73.0 |
| Pressure (psig) | 25 | 25.0 |
| riessure (baig) | 23 | 25.0 |

Heater Emission Calculations

AP-42 Emission Factors for Natural Gas Combustion, Table 1.4-1

| Process Unit: | Heat I | nput Rating |
|-----------------------------|--------|-------------|
| Reboiler Heater | 0.600 | MMBtu/hr |
| Tank Heater | 0.500 | MMBtu/hr |
| Tank Heater | 0.500 | MMBtu/hr |
| Tank Heater | 0.500 | MMBtu/hr |
| Line Heater | 0.250 | MMBtu/hr |
| NA | 0.000 | MMBtu/hr |
| Fuel Heat Value: | 1565.1 | Btu/scf |
| Annual Operating Hours: | 8760 | hrs |
| NO _x Emissions = | 1.5 | TPY |
| CO Emissions = | 1.3 | TPY |
| VOC Emissions= | 0.1 | TPY |

| | Fuel Consumed (Comb. Size, MMBtu/hr Heat Input) |
|-----------------|-------------------------------------------------|
| | Natural Gas |
| NO _x | 100 |
| CO | 84 |
| VOC | 5.5 |

| | | Estim | nated Heater NOx E | missions | | | |
|------------------|---------------|------------------|--------------------|-----------------|-------------------------------|--------------------|------------------------|
| Heater Number | Heater Rating | Emissions Factor | Emissions Factor | Fuel Heat Value | Corrected Emissions Factor | Operating Hours | Estimated Emissions |
| () | (MMBtu/hr) | (lb/MMCF) | (lb/hr) | (Btu/scf) | (lb/hr) | (hrs) | (TPY) |
| 1 | 0.600 | 100 | 0.059 | 1565 | 0.090 | 8760 | 0.395 |
| 2 | 0.500 | 100 | 0.049 | 1565 | 0.075 | 8760 | 0.329 |
| 3 | 0.500 | 100 | 0.049 | 1565 | 0.075 | 8760 | 0.329 |
| 4 | 0.500 | 100 | 0.049 | 1565 | 0.075 | 8760 | 0.329 |
| 5 | 0.250 | 100 | 0.025 | 1565 | 0.038 | 8760 | 0.165 |
| 6 | 0.000 | 100 | 0.000 | 1565 | 0.000 | 8760 | 0.000 |
| 7 | 0.000 | 100 | 0.000 | 1565 | 0.000 | 8760 | 0.000 |
| 8 | 0.000 | 100 | 0.000 | 1565 | 0.000 | 8760 | 0.000 |
| 9 | 0.000 | 100 | 0.000 | 1565 | 0.000 | 8760 | 0.000 |
| 10 | 0.000 | 100 | 0.000 | 1565 | 0.000 | 8760 | 0.000 |

| Total NO _x Emissions = | 1.5 | TPY | |
|-----------------------------------|------|-------|--|
| Total NO _x Emissions = | 0.35 | lb/hr | |

| | | Estir | nated Heater CO E | missions | | | |
|------------------|---------------|------------------|-------------------|-----------------|-------------------------------|--------------------|------------------------|
| Heater Number | Heater Rating | Emissions Factor | Emissions Factor | Fuel Heat Value | Corrected Emissions Factor | Operating Hours | Estimated Emissions |
| () | (MMBtu/hr) | (lb/MMCF) | (lb/hr) | (Btu/scf) | (lb/hr) | (hrs) | (TPY) |
| 1 | 0.600 | 84 | 0.049 | 1565 | 0.076 | 8760 | 0.332 |
| 2 | 0.500 | 84 | 0.041 | 1565 | 0.063 | 8760 | 0.277 |
| 3 | 0.500 | 84 | 0.041 | 1565 | 0.063 | 8760 | 0.277 |
| 4 | 0.500 | 84 | 0.041 | 1565 | 0.063 | 8760 | 0.277 |
| 5 | 0.250 | 84 | 0.021 | 1565 | 0.032 | 8760 | 0.138 |
| 6 | 0.000 | 84 | 0.000 | 1565 | 0.000 | 8760 | 0.000 |
| 7 | 0.000 | 84 | 0.000 | 1565 | 0.000 | 8760 | 0.000 |
| 8 | 0.000 | 84 | 0.000 | 1565 | 0.000 | 8760 | 0.000 |
| 9 | 0.000 | 84 | 0.000 | 1565 | 0.000 | 8760 | 0.000 |
| 10 | 0.000 | 84 | 0.000 | 1565 | 0.000 | 8760 | 0.000 |

| Total CO Emissions = | 1.3 | TPY | |
|--------------------------|------|-------|------|
| Total CO Emissions = | 0.30 | lb/hr | |
| Total CO Emissions = | 0.30 | - 1 | b/hr |

| Estimated Heater VOC Emissions | | | | | | | |
|--------------------------------|---------------|------------------|------------------|-----------------|-------------------------------|---------------------|------------------------|
| Heater Number | Heater Rating | Emissions Factor | Emissions Factor | Fuel Heat Value | Corrected Emissions Factor | Annual Operating | Estimated Emissions |
| () | (MMBtu/hr) | (lb/MMCF) | (lb/hr) | (Btu/scf) | (lb/hr) | (hrs) | (TPY) |
| 1 | 0.600 | 5.5 | 0.003 | 1565 | 0.005 | 8760 | 0.022 |
| 2 | 0.500 | 5.5 | 0.003 | 1565 | 0.004 | 8760 | 0.018 |
| 3 | 0.500 | 5.5 | 0.003 | 1565 | 0.004 | 8760 | 0.018 |
| 4 | 0.500 | 5.5 | 0.003 | 1565 | 0.004 | 8760 | 0.018 |
| 5 | 0.250 | 5.5 | 0.001 | 1565 | 0.002 | 8760 | 0.009 |
| 6 | 0.000 | 5.5 | 0.000 | 1565 | 0.000 | 8760 | 0.000 |
| 7 | 0.000 | 5.5 | 0.000 | 1565 | 0.000 | 8760 | 0.000 |
| 8 | 0.000 | 5.5 | 0.000 | 1565 | 0.000 | 8760 | 0.000 |
| 9 | 0.000 | 5.5 | 0.000 | 1565 | 0.000 | 8760 | 0.000 |
| 10 | 0.000 | 5.5 | 0.000 | 1565 | 0.000 | 8760 | 0.000 |

| Total VOC Emissions = | 0.1 | TPY | |
|-----------------------|------|-------|--|
| Total VOC Emissions = | 0.02 | lb/hr | |

Maintenance Flaring

Sample Identification: EOG Resources

DATE: 17-Jul-15

Facility: Fairway Compressor Station

| COMPO | TNENT | mol % | M.W. | (mol % X MW)/100 | WT% of i | |
|----------------|-------------|----------|------------------------------------|-----------------------------|----------|---|
| H2 | 2S | 0 | 34.08 | 0 | 0 | X |
| 0 | | 0 | 32.00 | 0 | 0.0000 | Х |
| CC | | 2.6062 | 44.01 | 1.1470 | 0.0414 | Х |
| Ν | | 0.9044 | 28.02 | 0.2534 | 0.0091 | Х |
| Metha | | 60.5243 | 16.04 | 9.7081 | 0.3502 | Х |
| Ethan | ne C2 | 12.5469 | 30.07 | 3.7729 | 0.1361 | X |
| Propai | ne C3 | 12.656 | 44.09 | 5.5800 | 0.2013 | X |
| i-Butan | | 1.3642 | 58.12 | 0.7929 | 0.0286 | X |
| n-Butan | ne n-C4 | 4.9501 | 58.12 | 2.8770 | 0.1038 | X |
| i-Penta | ne iC5 | 1.0322 | 72.15 | 0.7447 | 0.0269 | X |
| n-Penta | ne nC5 | 1.2482 | 72.15 | 0.9006 | 0.0325 | X |
| Cyclope | entane | 0.0942 | 70.1 | 0.0660 | 0.0024 | Χ |
| n-Hexar | ne n-C6 | 0.4213 | 86.17 | 0.3630 | 0.0131 | Χ |
| Cycloh | exane | 0.2358 | 84.16 | 0.1984 | 0.0072 | X |
| other H | exanes | 0.4817 | 85.00 | 0.4094 | 0.0148 | X |
| Hept | | 0.6081 | 100.20 | 0.6093 | 0.0220 | X |
| Methylcyc | | 0.109 | 98.18 | 0.1070 | 0.0039 | X |
| 2,2,4 Trime | thylpentane | 0.0002 | 114.22 | 0.0002 | 0.0000 | X |
| Benz | zene | 0.1382 | 78.11 | 0.1079 | 0.0039 | X |
| Tolu | | 0.0386 | 92.14 | 0.0356 | 0.0013 | X |
| Ethylbe | | 0.002 | 106.17 | 0.0021 | 0.0001 | X |
| Xyle | | 0.0045 | 106.17 | 0.0048 | 0.0002 | X |
| C8+ H | | 0.0258 | 120.00 | 0.0310 | 0.0011 | X |
| nona | | 0.0061 | 128.26 | 0.0078 | 0.0003 | X |
| C ₁ | 0+ | 0.0021 | 142.29 | 0.0030 | 0.0001 | X |
| | | 100.0001 | | | 1.0000 | |
| | MOLECULA | AR WEIGH | IT (lb/lb-mol)= | 27.7223 | | |
| Т | TOTAL VOC | s WEIGHT | PERCENT = | 0.4632 | | |
| TOTA | L HAPs WE | IGHT PER | CENT = | 0.0185 | | |
| V | VEIGHT PEI | ROENT H2 | 2S = | 0.0000 | | |
| Flow rate | 10000000 | scf/day | VOC TPY | 3529.3 | | |
| Downtime | 500 | hours | controlled | 70.6 | | |
| Btu/scf | 1565.09 | | HAP TPY controlled NOx CO | 141.2 2.8 22.8 5.7 | | |

EOG will limit flaring gas during maintenance events to 10.0 MMCFD for up to 500 hours per year.

Pigging/Compressor Blowdowns

Sample Identification: EOG Resources

DATE: 17-Jul-15

Facility: Fairway Compressor Station

| | | 170 | | | |
|-----------------------------------------------------|-------------|------------------|-----------------------|------------|---|
| COMPONENT | mol % | M.W. | (mol % X MW)/100 | WT% of i | |
| H2S | 0 | 34.08 | 0 | 0 | X |
| 02 | 0 | 32.00 | 0 | 0.0000 | X |
| CO2 | 2.6062 | 44.01 | 1.1470 | 0.0414 | X |
| N2 | 0.9044 | 28.02 | 0.2534 | 0.0091 | X |
| Methane C1 | 60.5243 | 16.04 | 9.7081 | 0.3502 | Х |
| Ethane C2 | 12.5469 | 30.07 | 3.7729 | 0.1361 | X |
| Propane C3 | 12.656 | 44.09 | 5.5800 | 0.2013 | X |
| i-Butane i-C4 | 1.3642 | 58.12 | 0.7929 | 0.0286 | X |
| n-Butane n-C4 | 4.9501 | 58.12 | 2.8770 | 0.1038 | X |
| i-Pentane iC5 | 1.0322 | 72.15 | 0.7447 | 0.0269 | X |
| n-Pentane nC5 | 1.2482 | 72.15 | 0.9006 | 0.0325 | X |
| Cyclopentane | 0.0942 | 70.1 | 0.0660 | 0.0024 | X |
| n-Hexane n-C6 | 0.4213 | 86.17 | 0.3630 | 0.0131 | X |
| Cyclohexane | 0.2358 | 84.16 | 0.1984 | 0.0072 | X |
| other Hexanes | 0.4817 | 85.00 | 0.4094 | 0.0148 | X |
| Heptanes | 0.6081 | 100.20 | 0.6093 | 0.0220 | X |
| Methylcyclohexane | 0.109 | 98.18 | 0.1070 | 0.0039 | X |
| 2,2,4 Trimethylpentane | 0.0002 | 114.22 | 0.0002 | 0.0000 | X |
| Benzene | 0.1382 | 78.11 | 0.1079 | 0.0039 | X |
| Toluene | 0.0386 | 92.14 | 0.0356 | 0.0013 | X |
| Ethylbenzene | 0.002 | 106.17 | 0.0021 | 0.0001 | X |
| Xylenes | 0.0045 | 106.17 | 0.0048 | 0.0002 | X |
| C8+ Heavies | 0.0258 | 120.00 | 0.0310 | 0.0011 | X |
| nonanes | 0.0061 | 128.26 | 0.0078 | 0.0003 | X |
| C ₁₀ + | 0.0021 | 142.29 | 0.0030 | 0.0001 | X |
| | 100.0001 | | | 1.0000 | |
| MOLECUL | AR WEIGHT | (lb/lb-mol)= | 27.7223 | | |
| TOTAL VO | Cs WEIGHT F | PERCENT = | 0.4632 | | |
| TOTAL HAPs WE | IGHT PERCE | NT = | 0.0185 | | |
| WEIGHT PER | RCENT H2S = | near description | 0.0000 | | |
| Compressor Blowdowns 2600 scf/hr 93600 scf/yr | (1 blowdowr | n per compres | ssor per month, 3 com | npressors) | |
| | | | | | |

C

Pigging Events 50,000 scf/hr

(assumed 100 hours per year of pigging)

5000000 scf/yr

| Flow rate | 5093600 scf/yr | | |
|-----------|----------------|------------|------|
| | | VOC TPY | 86.3 |
| Btu/scf | 1565.09 | controlled | 1.7 |
| | | HAP TPY | 3.5 |
| | | controlled | 0.1 |
| | | NOx | 0.6 |
| | | CO | 0.1 |

Condensate Tank Combustor Emission Calculations

Emission Source:

Tank Vent Gas Flowrate: 4.6 Mcf/day (from Promax)

Tank Vent Gas Flowrate: 191.6 scf/hr

(Btu content of tank flash from Promax) 2308.7 Btu/scf Estimated Heating Value:

Pilot Gas Flowrate: 0.28 scf/min (one combustor)

Pilot Gas Flowrate: 16.8 scf/hr

Lb.8 scr/nr Estimated Heating Value: 1565.1 Btu/scf

5002.3 scf/day

Total Flow to Flare:

 Pollutant
 lb/hr
 ton/yr

 NO_x
 0.07
 0.3

 CO
 0.02
 0.1

Emission Factors (From Ch. 6, Sec. 2 Guidance)

 NO_{x} 0.14 lb/MMBtu CO 0.035 lb/MMBtu

Water Transfer Facility - Blanket Gas Calculation

Sample Identification: EOG Resources DATE: 17-Jul-15

Facility: Water Transfer Facility

| COMPONENT | mol % | M.W. | (mol % X MW)/100 | WT% of i | |
|--------------------|--------------|-----------------|------------------|----------|---|
| H2S | 0 | 34.08 | 0 | 0 | Х |
| 02 | 0 | 32.00 | 0 | 0.0000 | X |
| CO2 | 2.6062 | 44.01 | 1.1470 | 0.0414 | Х |
| N2 | 0.9044 | 28.02 | 0.2534 | 0.0091 | X |
| Methane C1 | 60.5243 | 16.04 | 9.7081 | 0.3502 | X |
| Ethane C2 | 12.5469 | 30.07 | 3.7729 | 0.1361 | X |
| Propane C3 | 12.656 | 44.09 | 5.5800 | 0.2013 | X |
| i-Butane i-C4 | 1.3642 | 58.12 | 0.7929 | 0.0286 | X |
| n-Butane n-C4 | 4.9501 | 58.12 | 2.8770 | 0.1038 | X |
| i-Pentane iC5 | 1.0322 | 72.15 | 0.7447 | 0.0269 | X |
| n-Pentane nC5 | 1.2482 | 72.15 | 0.9006 | 0.0325 | Χ |
| Cyclopentane | 0.0942 | 70.1 | 0.0660 | 0.0024 | Χ |
| n-Hexane n-C6 | 0.4213 | 86.17 | 0.3630 | 0.0131 | Χ |
| Cyclohexane | 0.2358 | 84.16 | 0.1984 | 0.0072 | Χ |
| other Hexanes | 0.4817 | 85.00 | 0.4094 | 0.0148 | Χ |
| Heptanes | 0.6081 | 100.20 | 0.6093 | 0.0220 | Χ |
| Methylcyclohexai | ne 0.109 | 98.18 | 0.1070 | 0.0039 | Χ |
| 2,2,4 Trimethylpen | tane 0.0002 | 114.22 | 0.0002 | 0.0000 | Χ |
| Benzene | 0.1382 | 78.11 | 0.1079 | 0.0039 | Χ |
| Toluene | 0.0386 | 92.14 | 0.0356 | 0.0013 | X |
| Ethylbenzene | 0.002 | 106.17 | 0.0021 | 0.0001 | X |
| Xylenes | 0.0045 | 106.17 | 0.0048 | 0.0002 | X |
| C8+ Heavies | 0.0258 | 120.00 | 0.0310 | 0.0011 | Х |
| nonanes | 0.0061 | 128.26 | 0.0078 | 0.0003 | X |
| C ₁₀ + | 0.0021 | 142.29 | 0.0030 | 0.0001 | Х |
| | 100.0001 | | | 1.0000 | |
| MOLE | CULAR WEIGH | IT (lb/lb-mol)= | 27.7223 | | |
| TOTAL | VOCs WEIGHT | PERCENT = | 0.4632 | | |
| TOTAL HAP | WEIGHT PER | CENT | 0.0185 | | |
| WEIGH | T PERCENT H2 | Song and | 0.0000 | | |
| E1 | 504 f! ! | | | | |
| Flow rate | 504 scf/day | VOC TOV | 2.4 | | |
| • | 21 scf/hr | VOC TPY | 3.1 | | |
| 8 | 760 hours | controlled | 0.1 | | |
| Dhulaaf | F0F | HAP TPY | 0.1 | | |
| Btu/scf 1 | 565 | controlled | 0.0 | | |
| | | NOx | 0.02 | | |

CO

0.01

Flare Emission Calculations (Dehy control)

Emission Source:

Estimated Heating Value: 1565.1 Btu/scf (assumed same heat content as field gas)
Flash Tank Gas Flowrate: 4160.0 scf/hr

Pilot Gas Flowrate: 1.08 scf/min Filot Gas Flowrate: 64.8 scf/hr

(flare)

Estimated Heating Value: 1565.1 Btu/scf Total Flow to Flare: 101395.2 scf/day Emission Factors (From Ch. 6, Sec. 2 Guidance) 0.14 lb/MMBtu 0.035 lb/MMBtu Š 00 4.1 ton/yr 0.93 0.23 lb/hr Pollutant NO× 8

The emissions associated with the flare include full time control of the dehydration unit flash tank. The flash tank will primarily be routed to the compression inlet.

Truck Loading Emission Calculations

VOC Emissions from Truck Loading - AP-42 Chapter 5.2

| STORE CHARLE OF SUPPLIANCE CONTRIBUTION AND ADMINISTRA | |
|--------------------------------------------------------|-------------------------------------------------------------------|
| 0.5 | Submerged loading; barges |
| 0.2 | Marine vessels, submerged loading; ships |
| 1 | Splash loading; dedicated vapor balance service |
| 1.45 | Splash loading; dedicated normal service |
| 1.45 | Splash loading of a clean cargo tank |
| 7 | Submerged loading; dedicated vapor balance service |
| 0.6 | Submerged loading; dedicated normal service |
| 0.5 | Tank trucks and rail cars submerged loading of a clean cargo tank |
| | AP-42 Chapter 5.2, Table 5.2-1 |
| | |

Equation 1 for loading losses: (12.46) * (SPM / T) = L_L

Where:

 $L_{\rm L}$ = loading losses, lbs/1000 gal of liquid loaded

S = saturation factor

P = true vapor pressure of liquid loaded (psia). Source: 10.41 RVP of condensate (from Precision Analysis) converted to TVP @50°F using Figure 7.1-13a of AP-42 Chapter 7 (11/06).

M = Molecular wt of vapors, lb/lb-mol (from Promax)

T = temperature of bulk liquids loaded $^{\circ}$ R ($^{\circ}$ F = 460)

| 0.09 | 60.0 barrels/day | (production rates) |
|----------------|------------------|--------------------|
| 21900 bbl | bbls/yr | |
| 919800 gallons | gallons/yr | |

| | | 44.10 lb/lb-mol (taken from Promax) | | llons |
|------|----------|-------------------------------------|-----------|----------------------|
| 0.0 | 6.0 psia | 44.10 lb/lb-mol | 510 °R | 3.88 lb/1000 gallons |
| NI O | P= | = | <u> </u> | -_= |

| Incontrolled VOC Emissions: | 1.3 TPY |
|-----------------------------|---------|
| Jncontrolled HAP Emissions: | 0.1 TPY |

1.8 TPY TOC

Total Loss=

| | WT% of i | 0 | 0.0000 | 0.0752 | 0.0051 | 0.0533 | 0.1340 | 0.2657 | 0.0459 | 0.1875 | 0.0628 | 0.0777 | 0.0232 | 0.0000 | 0.0325 | 0.0229 | 0.0000 | 0.0017 | 0.0033 | 0.0042 | 0.0001 | 0.0005 | 0.0040 | 0.0003 | 0.0000 | | 1.0000 | |
|---------------------|------------------|-------|--------|--------|--------|------------|-----------|------------|---------------|---------------|---------------|---------------|---------------|-------------|---------------|----------|-------------------|------------------------|---------|---------|--------------|---------|-------------|---------|-------------------|--------|---------|-------------------------------|
| | (mol % X MW)/100 | 0 | 0 | 3.3155 | 0.2227 | 2.3484 | 5.9084 | 11.7123 | 2.0246 | 8.2661 | 2.7704 | 3.4276 | 1.0247 | 0.0000 | 1.4348 | 1.0111 | 0.0000 | 0.0736 | 0.1458 | 0.1865 | 0.0047 | 0.0208 | 0.1777 | 0.0118 | 0.0000 | | | 44.0873 |
| Promax) | M.W. | 34.08 | 32.00 | 44.01 | 28.02 | 16.04 | 30.07 | 44.09 | 58.12 | 58.12 | 72.15 | 72.15 | 86.17 | 84.16 | 85.00 | 100.20 | 98.18 | 114.22 | 78.11 | 92.14 | 106.17 | 106.17 | 120.00 | 128.26 | 142.29 | | | =(lom-dl/dl |
| (Taken from Promax) | % lom | 0 | 0.0000 | 7.5335 | 0.7949 | 14.6410 | 19.6488 | 26.5646 | 3.4835 | 14.2224 | 3.8397 | 4.7506 | 1.1891 | 0.0000 | 1.6880 | 1.0090 | 0.0000 | 0.0644 | 0.1867 | 0.2024 | 0.0044 | 0.0196 | 0.1480 | 0.0092 | 0.0000 | 0.0000 | 100.000 | R WEIGHT (|
| | COMPONENT | H2S | 02 | CO2 | N2 | Methane C1 | Ethane C2 | Propane C3 | i-Butane i-C4 | n-Butane n-C4 | i-Pentane iC5 | n-Pentane nC5 | n-Hexane n-C6 | Cyclohexane | other Hexanes | Heptanes | Methylcyclohexane | 2,2,4 Trimethylpentane | Benzene | Toluene | Ethylbenzene | Xylenes | C8+ Heavies | nonanes | C ₁₀ + | Water | | MOLECULAR WEIGHT (lb/lb-mol)= |

TOTAL VOCs WEIGHT PERCENT = 0.7325

0.0330

TOTAL HAPS WEIGHT PERCENT =

Fugitive Emissions Calculations

EPA Average Emission Factors for Total Hydrocarbon (THC)Emissions from O&G Production Operations (lb/component-day)

Equipment Service Category

| | | | | The second secon |
|-----------------|-------|------------|------------|--------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------|
| | | Heavy Oil | Light Oil | |
| Equipment Type | Gas | (<20° API) | (>20° API) | Water/Light Oil |
| connector | 0.011 | 0.0004 | 0.011 | 0.0058 |
| flange | 0.021 | 0.000021 | 0.0058 | 0.00015 |
| open ended line | 0.11 | 0.0074 | 0.074 | 0.013 |
| other | 0.47 | 0.0017 | 0.4 | 0.74 |
| dwnd | 0.13 | 0 | 69.0 | 0.0013 |
| valve | 0.24 | 0.00044 | 0.13 | 0.0052 |

Speciated Fugitive Emission Factors (Estimated weight fractions of THC emissions in each category)

| | | | | | | | Ethyl- | | |
|----------------|---------|-------|-------|---------|---------|---------|---------|---------|--|
| | Methane | NMHC | VOC | +90 | Benzene | Toluene | Benzene | Xylenes | |
| ght Crude | 0.613 | 0.387 | 0.292 | 0.0243 | 0.00037 | 0.00075 | 0.00017 | 0.00036 | |
| eavy Crude | 0.942 | 0.058 | 0.030 | 0.0752 | 0.00935 | 0.00344 | 0.00051 | 0.00372 | |
| ias Production | 0.92 | 0.080 | 0.035 | 0.00338 | 0.00023 | 0.00039 | 0.00002 | 0.0001 | |

| Ē | |
|---|---|
| | |
| 3 | ĺ |
| 7 | |
| | |

| | | Service | | |
|--------------------|-------|-----------|-----------|-----------------|
| Туре | Gas | Heavy Oil | Light Oil | Water/Light Oil |
| connector | 20 | 0 | 90 | 0 |
| flange | 250 | 0 | 250 | 250 |
| open ended line | 5 | 0 | 5 | 0 |
| other | 10 | 0 | 10 | 10 |
| dwnd | 0 | 0 | 0 | 0 |
| valve | 20 | 0 | 10 | 10 |
| Emissions (Ib/day) | 15.85 | 0 | 7.67 | 7.4895 |

VOC concentration - light crude from Promax VOC concentration - gas sample

0.732

days lbs

365

Using Site Specific Data

STATE OF WYOMING

Department of Environmental Quality - Air Quality Division Oil and Gas Production Facilities C6 S2 Permit Application



| Prom Di Al | 1001 | ONI | CII | | ARY |
|------------|------|-------|-----|-----------|-----|
| I\/I | 1551 | () [| - | I IVA IVA | ARY |

| Company Name | EOG Resources, Inc. |
|---------------|--------------------------------------------------------|
| Facility Name | Fairway Compressor Station and Water Transfer Facility |

This form must be completed for each emission source at the facility. A list of the emission sources which must be considered is found in Appendix B of the C6 S2 O&G Production Facilities Permitting Guidance.

UNCONTROLLED EMISSIONS (Tons Per Year)

These are the total uncontrolled, potential emissions from each source.

| EMISSION SOURCE (i.e., tank, natural gas-fired heater, reboiler still vent, glycol flash separator, pneumatic pump, separator gas vent, water knockout vent, etc.) | VOCs | total HAPs | NO _X | со | SO ₂ | H₂S |
|--------------------------------------------------------------------------------------------------------------------------------------------------------------------|--------|------------|-----------------|-----|-----------------|-----|
| two (2) 400-bbl condensate tanks | 73.6 | 3.3 | | | | |
| Maintenance Flaring (uncontrolled) | 3529.3 | 141.2 | | | | |
| truck loading (updated) | 1.3 | 0.1 | | | | |
| fugitives (updated) | 3.0 | 0.1 | | | | |
| 20.0 MMCFD TEG Dehydration Unit (updated) | 900.8 | 170.6 | | | | |
| three (3) 0.5 MMBtu/hr tank heaters | 0.1 | insig | 1.0 | 0.8 | | |
| one (1) 0.25 MMBtu/hr line heater | 0.0 | insig | 0.2 | 0.1 | | |
| five (5) 500-bbl produced water tanks (blanket gas routed to combustor) | 3.1 | 0.1 | | | | |
| blowdown/pigging | 86.3 | 3.5 | | | | |
| 0.6 MMBtu/hr reboiler heater | 0.0 | insig | 0.4 | 0.3 | | |
| two (2) 6,000 gallon methanol tanks | 0.1 | insig | | | | |
| three (3) 6,000 gallon chemical tanks | insig | insig | | | | |
| Total | 4597.6 | 318.8 | 1.5 | 1.3 | | |

CONTROLLED EMISSIONS (Tons Per Year)

These are the total emissions from each source. Include controlled emissions from each controlled source and uncontrolled emissions from each source which does not require control, such as process equipment burners.

| EMISSION SOURCE | VOCs | total HAPs | NO_X | СО | SO ₂ | H ₂ S |
|-------------------------------------------------------------------------|-------|--------------|------------|-----|-----------------|------------------|
| two (2) 400-bbl condensate tanks | | See Cimarron | Combustor | | | |
| Cimmaron Combustor (Condensate Tanks) | 1.5 | 0.1 | 0.3 | 0.1 | | |
| Maintenance Flaring (500 hours) | 70.6 | 2.8 | 22.8 | 5.7 | | |
| truck loading (updated) | 1.3 | 0.1 | | | | |
| 20.0 MMCFD TEG Dehydration Unit | | See Facil | ity Flare | | | |
| Facility Flare | 14.1 | 1.0 | 4.1 | 1.0 | | |
| three (3) 0.5 MMBtu/hr tank heaters | 0.1 | insig | 1.0 | 0.8 | | |
| one (1) 0.25 MMBtu/hr line heater | 0.0 | insig | 0.2 | 0.1 | | |
| five (5) 500-bbl produced water tanks (blanket gas routed to combustor) | | See Cimarror | n Combusto | | | |
| Cimmaron Combustor (Water Transfer) | 0.1 | 0.0 | 0.0 | 0.0 | | |
| blowdown/pigging (routed to facility flare) | 1.7 | 0.1 | 0.6 | 0.1 | | |
| 0.6 MMBtu/hr reboiler heater | 0.0 | insig | 0.4 | 0.3 | | |
| two (2) 6,000 gallon methanol tanks | 0.1 | insig | | | | |
| three (3) 6,000 gallon chemical tanks | insig | insig | | | | |
| Total | 88.0 | 4.0 | 29.0 | 8.2 | | |

HAZARDOUS AIR POLLUTANT SUMMARY (Tons Per Year)

| SOURCE | Benzene | Toluene | Ethyl-Benzene | Xylenes | Othe |
|--------|---------|---------|---------------|----------|------|
| JRCE | Benzene | roluene | Ethyl-benzene | Ayleries | |

Form AQD-OG6

Emission Summary September 2013



STATE OF WYOMING
Department of Environmental Quality - Air Quality Division
Oil and Gas Production Facilities C6 S2 Permit Application



Equipment List

| Company Name | EOG Resources, Inc. |
|---------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------|---------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------|
| Facility Name | Fairway Compressor Station |
| *************************************** | |
| tanks, all dehydration units, all pneumatic pur the potential for flash emissions are all vesse and 3-phase separators, heater treaters, gun (MMBtu/hr, SCFH). Provide size of productic | ding all pressurized vessels with the potential for flash emissions, all hydrocarbon liquids and produced water storage nps, all natural gas-fired burners and heaters and all emission control equipment and devices. Pressurized vessels with its that vent vapors to the atmosphere during times other than upset or emergency conditions (water knockouts, 2-phase barrels, scrubber pots, etc). Provide design ratings for dehys (MMCFD), process heaters, burners and pilots on & water storage tanks (BPD), For dehydration units indicate if the unit includes a glycol flash separator and/or reboiler mbustors/flares indicate design rating (MMBtu/hr, SCFD) and combustor/flare height (ft). Provide pneumatic pump |
| | If more space is required, continue on page 2 of this sheet. |
| PROVIDE INSTALLATION | DATES OF ALL EMISSION CONTROL EQUIPMENT & MONITORING DEVICES/SYSTEMS !!! |
| one (1) 400-barrel (bbl) condensate sto | orage tank w/0.50 MMBtu/hr tank heater (routed to Cimmaron ECD) (existing) |
| | e tank w/0.50 MMBtu/hr tank heater (routed to Cimmaron ECD) (existing) |
| one (1) 48"x12' Cimmaron LV enclosed (controls produced water and condens | d combustion device (ECD) with continuous pilot and thermocouple monitored through Cygnet sate storage tank emissions) |
| one (1) 60' Flare Industries flare with c | ontinuous pilot and thermocouple monitored through Cygnet (controls TEG dehydration unit flash intenance events, i.e. pigging, compressor blowdown) |
| one (1) 20.0 million cubic foot per day | (MMCFD) tri-ethylene glycol (TEG) dehydration unit with 0.6 MMBtu/hr reboiler heater, reboiler k, and three (3) Kimray model 21015PV glycol circulation pumps (one backup) |
| three (3) electric motor driven compre | |
| one (1) unheated 9'x30' horizontal inle | t separator (slug catcher) |
| one (1) unheated 60"x20' horizontal se | parator (flare knockout) |
| truck loadout | |
| one (1) 400-barrel (bbl) condensate sto | orage tank w/0.50 MMBtu/hr tank heater (routed to Cimmaron ECD) (proposed) |
| five (5) 6,000 gallon chemical storage | tanks (methanol, emulsion breaker, paraffin inhibitor, corrosion inhibitor) (proposed) |
| fugitives | |
| compressor blowdowns/pigging (route | ed to facility flare) |
| | |
| | |
| | |
| | |
| Example: | |
| 1 2-phase high pressure separator (unheate | d) |
| 1 3-phase low pressure separator w/ 0.5 MN | lBtu/hr heater |
| 2 0.5 MMBtu/hr line heaters | |
| 1 5 MMCFD TEG dehydration unit w/ 0.5 MM | lBtu/hr reboiler heater, glycol flash separator(0.5 MMBtu/hr heater) and overheads condenser |
| 2 400-bbl condensate tanks | |
| 1 400-bbl produced water tank | |
| 1 30-ft enclosed combustor (3.0 MMBtu/hr, | 5 MCFD) for flashing & reboiler vent/glycol flash separator emissions control installed 1/1/2007 |
| | Form AQD-OG2 |

Equipment List September 2013



STATE OF WYOMING
Department of Environmental Quality - Air Quality Division
Oil and Gas Production Facilities C6 S2 Permit Application



Equipment List - continued

| Company | EOG Pagaurage Ing | - |
|--------------------------------------------------------------------------|--------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------|---|
| Company Name | EOG Resources, Inc. | |
| Facility Name | Water Transfer Facility | |
| | | |
| | | |
| | | |
| | | |
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| | | |
| | | |
| | | |
| five (5) 500-bbl produced water storage ta | inke | |
| one (1) 0.25 MMBtu/hr line heater | | |
| | | |
| various electric driven pumps | The state of the s | |
| one (1) 48"x12' Cimmaron LV enclosed co water storage tank emissions) | ombustion device (ECD) with continuous pilot and thermocouple monitored through Cygnet (control | s |
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| | | |
| | Form AQD-OG2 | |

Equipment List, Page 2 September 2013



Simulation Report

Project: Fairway CS update - outlet sample.pmx

Licensed to EOG Resources, Inc. and Affiliates

Client Name: EOG

Location: Fairway Compressor Station

Job:

ProMax Filename: M:\ProMax\Fairway CS update - outlet sample.pmx

ProMax Version: 3.2.12198.0

Simulation Initiated: 6/17/2015 8:08:25 AM

Bryan Research & Engineering, Inc.

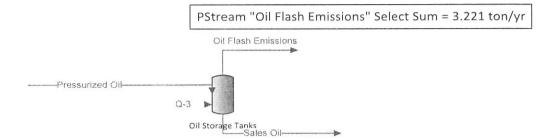
Chemical Engineering Consultants P.O. Box 4747 Bryan, Texas 77805 Office: (979) 776-5220 FAX: (979) 776-4818 mailto:sales@bre.com/ http://www.bre.com/

Report Navigator can be activated via the ProMax Navigator Toolbar.

An asterisk (*), throughout the report, denotes a user specified value.

A question mark (?) after a value, throughout the report, denotes an extrapolated or approximate value.

Stream Oil Flash Emissions C3+ Mass Flow =71.45 ton/yr



| Names | Units | Sales Oil |
|----------------------------|-------|-----------|
| Std Liquid Volumetric Flow | bbl/d | 60 |

| Process Streams | Status: | Oil Flash Emissions Solved |
|------------------------------------|-------------|-------------------------------|
| Composition Phase: Total | From Block: | Oil Storage Tanks |
| Wass Flow | To Block: | lb/h |
| Hydrogen Sulfide | - | 10/11 |
| Oxygen | 1 | |
| J. Aygen | | |
| | | |
| Carbon Dioxide | | 1.6742 |
| Nitrogen | 1 | 0.11244 |
| Methane Ethane | | 2.9834 |
| Propane | | 5.915 |
| sobutane | | 1.0224 |
| n-Butane | | 4.1742 |
| sopentane | | 1.3989 |
| n-Pentane | | 1.730 |
| 2-Methylpentane | 1 | 0.54179 |
| 3-Methylpentane | | 0.1927 |
| Heptane | | 0.51056 |
| Octane Nonane | | 0.085396 0.0059487 |
| Benzene | 1 | 0.07363 |
| Toluene | | 0.09415 |
| Ethylbenzene | | 0.0023744 |
| m-Xylene | | 0.0011862 |
| o-Xylene o-Xylene | | 0.007749 0.001575 |
| n-Hexane | | 0.5174 |
| 2,2,4-Trimethylpentane | | 0.037170 |
| Water | | |
| C10+ | | 3.84442E- |
| Mole Fraction | | % |
| Hydrogen Sulfide | | |
| Oxygen Carbon Dioxide | | 7.533 |
| Nitrogen | | 0.7948 |
| Methane | 1 | 14.64 |
| Ethane | | 19.64 |
| Propane | | 26.56 |
| sobutane | | 3.483 14.22 |
| n-Butane sopentane | | 3.839 |
| n-Pentane | | 4.750 |
| 2-Methylpentane | | 1.245 |
| 3-Methylpentane | | 0.4429 |
| Heptane | | 1.009 |
| Octane Nonane | | 0.1480- 0.009185 |
| Benzene | | 0.1866 |
| Toluene | | 0.2023 |
| Ethylbenzene | | 0.004429 |
| m-Xylene | | 0.002212 |
| o-Xylene | | 0.01445 |
| o-Xylene | | 0.002938 1.189 |
| n-Hexane 2,2,4-Trimethylpentane | | 0.06443 |
| Water | | |
| C10+ | | 3.43307E- |
| Mass Fraction | | % |
| Hydrogen Sulfide | | |
| Oxygen Carbon Dioxide | | 7.517 |
| Nitrogen | | 0.5049 |
| Methane | | 5.325 |
| Ethane | | 13.39 |
| Propane | | 26.56 4.591 |
| sobutane n-Butane | | 4.591 |
| sopentane | | 6.281 |
| n-Pentane | | 7.772 |
| 2-Methylpentane | | 2.432 |
| 3-Methylpentane | | 0.8655 |
| Heptane | | 2.292 0.3834 |
| Octane Nonane | | 0.02671 |
| Nonane Benzene | | 0.3306 |
| Toluene | | 0.4228 |
| Ethylbenzene | | 0.01066 |
| m-Xylene | | 0.005326 |
| p-Xylene | | 0.03479 |
| o-Xylene | | 0.007073 |
| n-Hexane 2,2,4-Trimethylpentane | | 2,323 0.1669 |
| | | |
| Water | | 0.1000 |

SWB HAP TPY
(assume 3.3% HAP)
based on oil flash
output stream HAP
concentration)
2.2

Oil Flash VOC TPY
71.5

Oil Flash HAP TPY
3.2

| Total VOC TPY | Total HAP TPY | |
|---------------|---------------|--|
| 73.6 | 3.3 | |

| Process Streams | | Oil Flash Emissions |
|-------------------------------|-------------------------|---------------------|
| Properties | Status: | Solved |
| Phase: Total | From Block: | Oil Storage Tanks |
| | To Block: | |
| Property | Units | |
| Temperature | °F | 60° |
| Pressure | psia | 14.6959* |
| Mole Fraction Vapor | % | 100 |
| Mole Fraction Light Liquid | % | C |
| Mole Fraction Heavy Liquid | % | 0 |
| Molecular Weight | lb/lbmol | 44.1006 |
| Mass Density | lb/ft^3 | 0.118142 |
| Molar Flow | lbmol/h | 0.504972 |
| Mass Flow | lb/h | 22.2696 |
| Vapor Volumetric Flow | ft^3/h | 188.499 |
| Liquid Volumetric Flow | gpm | 23.5012 |
| Std Vapor Volumetric Flow | MMSCFD | 0.00459910 |
| Std Liquid Volumetric Flow | sgpm | 0.0862504 |
| Compressibility | 171-00111 | 0.983666 |
| Specific Gravity | | 1.52267 |
| API Gravity | | |
| Enthalpy | Btu/h | -27816.5 |
| Mass Enthalpy | Btu/lb | -1249.08 |
| Mass Cp | Btu/(lb*°F) | 0.385757 |
| Ideal Gas CpCv Ratio | CONTROL CONTROL CONTROL | 1.13332 |
| Dynamic Viscosity | cP | 0.00856232 |
| Kinematic Viscosity | cSt | 4.52447 |
| Thermal Conductivity | Btu/(h*ft*°F) | 0.0104586 |
| Surface Tension | lbf/ft | |
| Net Ideal Gas Heating Value | Btu/ft^3 | 2124.59 |
| Net Liquid Heating Value | Btu/lb | 18138.8 |
| Gross Ideal Gas Heating Value | Btu/ft^3 | 2308.74 |
| Gross Liquid Heating Value | Btu/lb | 19723.5 |

| Process Streams | | Oil Flash Emissions |
|----------------------------|--------------------------|---------------------|
| Composition | Status: | Solved |
| Phase: Vapor | From Block: To Block: | Oll Storage Tanks |
| Mass Flow | | lb/h |
| Hydrogen Sulfide | | |
| Oxygen | | |
| Carbon Dioxide | | 1.6742 |
| Nitrogen | | 0.11244 |
| Methane | | 1.1860 |
| Ethane | | 2.9834 |
| Propane | | 5.915 |
| Isobutane | | 1.0224 |
| n-Butane | | 4.174 |
| Isopentane | | 1.398 |
| n-Pentane | | 1.730 |
| 2-Methylpentane | | 0.54179 |
| 3-Methylpentane | | 0.1927 |
| 3-Methylpentane Heptane | | 0.5105 |
| Heptane Octane | | 0.08539 |
| Nonane | | 0.005948 |
| | | 0.07363 |
| Benzene | | 0.07303 |
| Toluene | | 0.002374 |
| Ethylbenzene | | |
| m-Xylene | | 0.001186 |
| p-Xylene | | 0.007749 |
| o-Xylene | | 0.001575 |
| n-Hexane | | 0.5174 |
| 2,2,4-Trimethylpentane | | 0.03717 |
| Water | | |
| C10+ | | 3.84442E- |
| Mole Fraction | | % |
| Hydrogen Sulfide | | |
| Oxygen | | |
| Carbon Dioxide | | 7.533 |
| Nitrogen | | 0.7948 |
| Methane | | 14.64 |
| Ethane | | 19.64 |
| Propane | 1 | 26.56 |
| Isobutane | | 3.483 |
| n-Butane | 1 | 14.22 |
| Isopentane | | 3.839 |
| n-Pentane | | 4.750 |
| 2-Methylpentane | | 1.245 |
| 3-Methylpentane | 1 | 0.4429 |
| Heptane | | 1.009 |
| Octane | | 0.1480 |
| Nonane | | 0.009185 |
| Benzene | | 0.1866 |
| Toluene | | 0.2023 |
| Ethylbenzene | | 0.004429 |
| m-Xylene | | 0.002212 |
| p-Xylene | | 0.01445 |
| o-Xylene | | 0.002938 |
| n-Hexane | | 1.189 |
| 2,2,4-Trimethylpentane | | 0.06443 |
| Water | | |
| | | |

| Mass Fraction | % |
|------------------------|-------------|
| Hydrogen Sulfide | 0 |
| Oxygen | 0 |
| Carbon Dioxide | 7.51799 |
| Nitrogen | 0.504924 |
| Methane | 5.32594 |
| Ethane | 13.3971 |
| Propane | 26.5616 |
| Isobutane | 4.59106 |
| n-Butane | 18.7444 |
| Isopentane | 6.28184 |
| n-Pentane | 7.77200 |
| 2-Methylpentane | 2.43288 |
| 3-Methylpentane | 0.865572 |
| Heptane | 2.29265 |
| Octane | 0.383465 |
| Nonane | 0.0267122 |
| Benzene | 0.330642 |
| Toluene | 0.422809 |
| Ethylbenzene | 0.0106625 |
| m-Xylene | 0.00532689 |
| p-Xylene | 0.0347999 |
| o-Xylene | 0.00707363 |
| n-Hexane | 2.32359 |
| 2,2,4-Trimethylpentane | 0.166910 |
| Water | 0 |
| C10+ | 1.72631E-05 |

| Process Streams | | Oil Flash Emissions |
|-------------------------------|---------------|---------------------|
| Properties | Status: | Solved |
| Phase: Vapor | From Block: | Oil Storage Tanks |
| | To Block: | |
| Property | Units | |
| Temperature | °F T | 60 |
| Pressure | psia | 14.6959 |
| Mole Fraction Vapor | % | 100 |
| Mole Fraction Light Liquid | % | C |
| Mole Fraction Heavy Liquid | % | C |
| Molecular Weight | lb/lbmol | 44.1006 |
| Mass Density | lb/ft^3 | 0.118142 |
| Molar Flow | lbmol/h | 0.504972 |
| Mass Flow | lb/h | 22.2696 |
| Vapor Volumetric Flow | ft^3/h | 188.499 |
| Liquid Volumetric Flow | gpm | 23.5012 |
| Std Vapor Volumetric Flow | MMSCFD | 0.00459910 |
| Std Liquid Volumetric Flow | sgpm | 0.0862504 |
| Compressibility | | 0.983666 |
| Specific Gravity | | 1,52267 |
| API Gravity | | |
| Enthalpy | Btu/h | -27816.5 |
| Mass Enthalpy | Btu/lb | -1249.08 |
| Mass Cp | Btu/(lb*°F) | 0.385757 |
| Ideal Gas CpCv Ratio | | 1.13332 |
| Dynamic Viscosity | cP | 0.00856232 |
| Kinematic Viscosity | cSt | 4.52447 |
| Thermal Conductivity | Btu/(h*ft*°F) | 0.0104586 |
| Surface Tension | lbf/ft | |
| Net Ideal Gas Heating Value | Btu/ft^3 | 2124.59 |
| Net Liquid Heating Value | Btu/lb | 18138.8 |
| Gross Ideal Gas Heating Value | Btu/ft^3 | 2308.74 |
| Gross Liquid Heating Value | Btu/lb | 19723.5 |

Tank Indentification and Physical Characteristics Emissions Report - Summary Format **TANKS 4.0.9d**

| Fairway CS Condensate Tank | | Vertical Fixed Roof Tank | |
|----------------------------|--------|--------------------------|--------------|
| Identification | City: | Company: | Description: |
| User Identification: | State: | Type of Tank: | |

| Tank Dimensions | | | |
|--------------------------|-------------|------------|--|
| Shell Height (ft): | | 20.00 | |
| Diameter (ft): | | 12.00 | |
| Liquid Height (ft): | | 15.00 | |
| Avg. Liquid Height (ft): | | 14.00 | |
| Volume (gallons): | | 12,690.44 | |
| Turnovers: | | 72.48 | |
| Net Throughput(gal/yr): | | 919,800.00 | |
| Is Tank Heated (y/n): | z | | |
| | | | |
| Paint Characteristics | | | |
| Shell Color/Shade: | White/White | | |
| Shell Condition | Good | | |
| Roof Color/Shade: | White/White | | |
| Roof Condition: | Good | | |
| | | | |
| Roof Characteristics | | | |
| Type: | Cone | | |
| Height (ft) | | 0.50 | |
| Slone (#/#) (Cone Doof) | | 800 | |

| | | 0.50 | 0.08 |
|----------------------|-------|-------------|---------------------------|
| | Cone | | |
| Roof Characteristics | Type: | Height (ft) | Slope (ft/ft) (Cone Roof) |

| | -0.03 | 0.03 |
|------------------------|-------------------------|--------------------------|
| | | |
| Breather Vent Settings | Vacuum Settings (psig): | Pressure Settings (psig) |

Meterological Data used in Emissions Calculations: Cheyenne, Wyoming (Avg Atmospheric Pressure = 11.76 psia)

6/17/2015

TANKS 4.0.9d
Emissions Report - Summary Format
Liquid Contents of Storage Tank

Fairway CS Condensate Tank - Vertical Fixed Roof Tank

| Basis for Vapor Pressure | Calculations | Option 4: RVP=10, ASTM Slope=3 |
|--------------------------------------|-------------------|--------------------------------|
| | Weight | 92.00 |
| Vapor Mass | Fract. | |
| Liquid | Fract. | |
| Vapor Mol. | Weight. | 66,0000 |
| osia) | Max. | 4,5750 |
| oor Pressure (psia) | Min. | 3.5647 |
| Vapor | | 4.0445 |
| Liquid Bulk Temp | (deg F) | 45.62 |
| л. 3 F) | Max. | 53.62 |
| Daily Liquid Surf emperature (deg | Min. | 47.49 41.37 |
| Dail | Avg. | 1 |
| Daily Liquid Sur Temperature (deg | Month | A |
| | Mixture/Component | Gasoline (RVP 10) |

TANKS 4.0 Report

6/17/2015

TANKS 4.0.9d Emissions Report - Summary Format Individual Tank Emission Totals

Emissions Report for: Annual

Fairway CS Condensate Tank - Vertical Fixed Roof Tank

| | | Losses(lbs) | |
|-------------------|--------------|----------------|-----------------|
| Components | Working Loss | Breathing Loss | Total Emissions |
| Gasoline (RVP 10) | 3,393.96 | 922.17 | 4,316.13 |

TANKS 4.0.9d Emissions Report - Summary Format Tank Indentification and Physical Characteristics

| dethanol Tank | Roof Tank | 15.00 9.00 12.00 10.00 5,710.70 18.38 108,000.00 | | 0.50 |
|-------------------------------------------|-----------------------------------------------------|---------------------------------------------------------------------------------------------------------------------------------------------------------------------------|--------------------------------------------------------------------------------------------|---------------------------------------------------------------------------|
| Fairway CS - Methanol Tank | Vertical Fixed Roof Tank | Z | White/White Good White/White Good | Cone |
| Identification User Identification: City: | State: Company: Type of Tank: Description: | Tank Dimensions Shell Height (ft): Diameter (ft): Liquid Height (ft): Avg. Liquid Height (ft): Volume (gallons): Turnovers: Net Throughput(gal/yr): Is Tank Heated (y/n): | Paint Characteristics Shell Color/Shade: Shell Condition Roof Color/Shade: Roof Condition: | Roof Characteristics Type: Height (ft) Slope (ft/ft) (Cone Roof) |

Meterological Data used in Emissions Calculations: Cheyenne, Wyoming (Avg Atmospheric Pressure = 11.76 psia)

-0.03

Breather Vent Settings Vacuum Settings (psig): Pressure Settings (psig)

TANKS 4.0.9d
Emissions Report - Summary Format
Liquid Contents of Storage Tank

Fairway CS - Methanol Tank - Vertical Fixed Roof Tank

| | Vapor Liquid | F) Temp Vapor Pressure (psia) Mol. Mass Mass | Max, (deg F) Avg. Min. Max, Weight. Fract. | All 47.49 41.37 53.62 45.62 0.9614 0.7814 1.1760 32.0400 32.04 Option 2: A=7.897, B=1474,08, C=229.13 |
|--------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------|--------------|----------------------------------------------|--------------------------------------------|-------------------------------------------------------------------------------------------------------|
| Academican and an academic of the second participate of the second participates of the second particip | | | Mixture/Component | Methyl alcohol |

TANKS 4.0.9d Emissions Report - Summary Format Individual Tank Emission Totals

Emissions Report for: Annual

Fairway CS - Methanol Tank - Vertical Fixed Roof Tank

| | | Losses(lbs) | |
|----------------|--------------|----------------|-----------------|
| Components | Working Loss | Breathing Loss | Total Emissions |
| Methyl alcohol | 79.21 | 42.63 | 121.84 |

TANKS 4.0 Report

6/9/2015

GRI-GLYCalc VERSION 4.0 - SUMMARY OF INPUT VALUES

Case Name: Fairway CS

File Name: C:\Users\msmith6\Documents\my qly calc stuff\Fairway CS\Fairway CS update.ddf

Date: June 17, 2015

DESCRIPTION:

Description: 20 MMCFD dehy two (2) Kimray 21015PV pumps

(7.0 gpm)

Annual Hours of Operation: 8760.0 hours/yr

WET GAS:

Temperature: 100.00 deg. F
Pressure: 1000.00 psig
Wet Gas Water Content: Saturated

| Component | Conc. (vol %) |
|------------------------|---------------|
| Carbon Dioxide | 2.6062 |
| Nitrogen | 0.9044 |
| Methane | 60.5243 |
| Ethane | 12.5469 |
| Propane | 12.6560 |
| Isobutane | 1.3642 |
| n-Butane | 4.9501 |
| Isopentane | 1.0322 |
| n-Pentane | 1.2482 |
| Cyclopentane | 0.0942 |
| n-Hexane | 0.4230 |
| Cyclohexane | 0.2358 |
| Other Hexanes | 0.4817 |
| Heptanes | 0.6081 |
| Methylcyclohexane | 0.1090 |
| 2,2,4-Trimethylpentane | 0.0002 |
| Benzene | 0.1382 |
| Toluene | 0.0386 |
| Ethylbenzene | 0.0020 |
| Xylenes | 0.0045 |
| C8+ Heavies | 0.0340 |

DRY GAS:

Flow Rate: 20.0 MMSCF/day Water Content: 7.0 lbs. H2O/MMSCF

LEAN GLYCOL:

Glycol Type: TEG

Water Content: 1.5 wt% H20 Flow Rate: 7.0 gpm

PUMP:

Glycol Pump Type: Gas Injection

Gas Injection Pump Volume Ratio: 0.080 acfm gas/gpm glycol

FLASH TANK:

Flash Control: Combustion device

Flash Control Efficiency: 98.00 %
Temperature: 80.0 deg. F
Pressure: 60.0 psig

REGENERATOR OVERHEADS CONTROL DEVICE:

Control Device: Condenser

Temperature: 100.0 deg. F Pressure: 12.0 psia

Control Device: Combustion Device

Destruction Efficiency: 98.0 %
Excess Oxygen: 0.0 %
Ambient Air Temperature: 50.0 deg. F

GRI-GLYCalc VERSION 4.0 - EMISSIONS SUMMARY

CONTROLLED REGENERATOR EMISSIONS

| Component | lbs/hr | lbs/day | tons/yr |
|------------------------------------------------------------------------------------------|---------|---------|---------|
| Methane | 0.0138 | 0.332 | 0.0605 |
| Ethane | 0.0250 | 0.601 | 0.1097 |
| Propane | 0.0820 | 1.968 | 0.3591 |
| Isobutane | 0.0181 | 0.435 | 0.0794 |
| n-Butane | 0.0864 | 2.073 | 0.3784 |
| Isopentane | 0.0202 | 0.485 | 0.0885 |
| n-Pentane | 0.0275 | 0.661 | 0.1206 |
| Cyclopentane | 0.0089 | 0.214 | 0.0391 |
| n-Hexane | 0.0121 | 0.291 | 0.0532 |
| Cyclohexane | 0.0218 | 0.523 | 0.0954 |
| Other Hexanes Heptanes Methylcyclohexane 2,2,4-Trimethylpentane Benzene | 0.0135 | 0.324 | 0.0592 |
| | 0.0142 | 0.342 | 0.0624 |
| | 0.0064 | 0.154 | 0.0280 |
| | <0.0001 | <0.001 | <0.0001 |
| | 0.1000 | 2.399 | 0.4378 |
| Toluene | 0.0133 | 0.318 | 0.0581 |
| Ethylbenzene | 0.0003 | 0.007 | 0.0013 |
| Xylenes | 0.0006 | 0.014 | 0.0026 |
| C8+ Heavies | <0.0001 | <0.001 | <0.0001 |
| Total Emissions | 0.4642 | 11.141 | 2.0331 |
| Total Hydrocarbon Emissions Total VOC Emissions Total HAP Emissions Total BTEX Emissions | 0.4642 | 11.141 | 2.0331 |
| | 0.4253 | 10.208 | 1.8630 |
| | 0.1263 | 3.030 | 0.5530 |
| | 0.1141 | 2.739 | 0.4998 |

UNCONTROLLED REGENERATOR EMISSIONS

| Component | lbs/hr | lbs/day | tons/yr |
|-------------------------------------------------------------------------|---------|---------|---------|
| Methane | 0.6930 | 16.631 | 3.0352 |
| Ethane | 1.2713 | 30.511 | 5.5682 |
| Propane | 4.4065 | 105.755 | 19.3003 |
| Isobutane | 1.0537 | 25.289 | 4.6152 |
| n-Butane | 5.4716 | 131.319 | 23.9658 |
| Isopentane | 1.6358 | 39.258 | 7.1646 |
| n-Pentane | 2.6057 | 62.536 | 11.4128 |
| Cyclopentane | 0.9526 | 22.862 | 4.1724 |
| n-Hexane | 1.8897 | 45.352 | 8.2768 |
| Cyclohexane | 4.5525 | 109.261 | 19.9401 |
| Other Hexanes Heptanes Methylcyclohexane 2,2,4-Trimethylpentane Benzene | 1.6227 | 38.945 | 7.1074 |
| | 5.7496 | 137.991 | 25.1834 |
| | 2.4588 | 59.012 | 10.7697 |
| | 0.0011 | 0.026 | 0.0048 |
| | 22.2445 | 533.869 | 97.4311 |
| Toluene | 8.1474 | 195.538 | 35.6857 |
| Ethylbenzene | 0.5049 | 12.118 | 2.2115 |
| Xylenes | 1.5122 | 36.292 | 6.6233 |
| C8+ Heavies | 0.8767 | 21.041 | 3.8399 |

| | | | Page: 2 |
|-----------------------------------|--------------------|--------------------|----------------------|
| Total Emissions | 67.6502 | 1623.606 | 296.3080 |
| Total Hydrocarbon Emissions | 67.6502 | 1623.606 | 296.3080 |
| Total VOC Emissions | 65.6860 | 1576.464 | 287.7046 |
| Total HAP Emissions | 34.2998 32.4090 | 823.195 777.816 | 150.2331 141.9515 |
| Total BTEX Emissions | 32.4090 | ///.816 | 141.9515 |
| FLASH GAS EMISSIONS | | | |
| Component | lbs/hr | lbs/day | tons/yr |
| Methane | 2.0310 | 48.745 | 8.8960 |
| Ethane | 0.8701 | 20.882 | 3.8110 |
| Propane | 1.2840 | 30.816 | 5.6238 |
| Isobutane | 0.1787 | 4.290 | 0.7829 |
| n-Butane | 0.6618 | 15.883 | 2.8987 |
| Isopentane | 0.1566 | 3.758 4.569 | 0.6859 0.8338 |
| n-Pentane Cyclopentane | 0.1904 0.0170 | 0.407 | 0.0743 |
| n-Hexane | 0.0665 | 1.597 | 0.2914 |
| Cyclohexane | 0.0385 | 0.923 | 0.1685 |
| Other Hexanes | 0.0789 | 1.893 | 0.3455 |
| Heptanes | 0.0848 | 2.035 | 0.3714 |
| Methylcyclohexane | 0.0146 | 0.351 | 0.0641 |
| 2,2,4-Trimethylpentane Benzene | <0.0001 0.0216 | 0.001 0.519 | 0.0002 0.0947 |
| | | | |
| Toluene Ethylbenzene | 0.0044 | 0.106 | 0.0193 |
| Xylenes | 0.0003 | 0.007 | 0.0012 |
| C8+ Heavies | 0.0015 | 0.036 | 0.0066 |
| Total Emissions | 5.7009 | 136.821 | 24.9698 |
| Total Hydrocarbon Emissions | 5.7009 | 136.821 | 24.9698 |
| Total VOC Emissions | 2.7997 | 67.193 | 12.2628 |
| Total HAP Emissions | 0.0930 | 2.232 | 0.4073 |
| Total BTEX Emissions | 0.0264 | 0.634 | 0.1158 |
| LASH TANK OFF GAS | | | |
| Component | lbs/hr | lbs/day | tons/yr |
| Methane | 101.5525 | 2437.259 | 444.7997 |
| Ethane | 43.5042 | 1044.101 | 190.5483 |
| Propane | 64.1990 | 1540.776 | 281.1917 |
| Isobutane n-Butane | 8.9369 33.0901 | 214.486 794.163 | 39.1436 144.9348 |
| Isopentane | 7.8298 | 187.914 | 34.2944 |
| n-Pentane | 9.5188 | 228.450 | 41.6921 |
| Cyclopentane | 0.8481 | 20.354 | 3.7147 |
| n-Hexane | 3.3265 | 79.837 | 14.5702 |
| Cyclohexane | 1.9230 | 46.152 | 8.4228 |
| Other Hexanes | 3.9438 | 94.652 | 17.2740 |
| Heptanes | 4.2398 | 101.756 | 18.5705 |
| Methylcyclohexane | 0.7319 | 17.566 0.041 | 3.2058 0.0079 |
| 2,2,4-Trimethylpentane Benzene | 0.0017 1.0808 | 25.939 | 4.7338 |
| Denzene | 1.0000 | 20.505 | , 55 |
| Toluene | 0.2205 | 5.291 | 0.9657 |
| Ethylbenzene | 0.0069 | 0.165 | 0.0300 |
| | | | |

| | C8 | Xylenes 3+ Heavies | 0.0137 0.0750 | 0.328 | Page: 3 0.0599 0.3285 |
|-------|-----------------------------------------------------|------------------------|------------------------------------------|-------------------------------------------|--------------------------------------------|
| | Total | Emissions | 285.0429 | 6841.030 | 1248.4880 |
| Total | Hydrocarbon Total VOC Total HAP Total BTEX | Emissions Emissions | 285.0429 139.9863 4.6500 1.3218 | 6841.030 3359.671 111.600 31.723 | 1248.4880 613.1399 20.3671 5.7894 |

GRI-GLYCalc VERSION 4.0 - STREAM REPORT

Case Name: Fairway CS

File Name: C:\Users\msmith6\Documents\my gly calc stuff\Fairway CS\Fairway CS update.ddf

Date: June 17, 2015

FLASH TANK OFF GAS STREAM

Temperature: 80.00 deg. F Pressure: 74.70 psia Flow Rate: 4.16e+003 scfh

| Flow Rate: 4.16e+003 scfh | | |
|--------------------------------------------|---------------------------------------------------------------|-------------------------------------|
| Component | Conc. (vol%) | Loading (lb/hr) |
| Carbon Dioxide Nitrogen Methane | 3.95e-002 4.46e+000 8.90e-001 5.77e+001 1.32e+001 | 2.15e+001 2.74e+000 1.02e+002 |
| Isobutane n-Butane Isopentane | 1.33e+001 1.40e+000 5.19e+000 9.89e-001 1.20e+000 | 8.94e+000 3.31e+001 7.83e+000 |
| Cyclohexane Other Hexanes | 3.52e-001 2.08e-001 | 3.33e+000 1.92e+000 3.94e+000 |
| | 1.37e-004 1.26e-001 2.18e-002 | 1.71e-003 1.08e+000 2.20e-001 |
| Xylenes C8+ Heavies Total Components | | |



INSTALLATION, OPERATION AND MAINTENANCE MANUAL

FOR
EOG RESOURCES
C/O KAHUNA VENTURES
West Minster, Colorado USA

SFVP-1042 Flare Tip & Model 850 Pilots, -B System FL-411

Document No 140663-M02-0001, Rev 0



CERTIFIED FINAL

OA: Auch Model

ENG: Hart WAS



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1.0 PROJECT DESCRIPTION

1.1 Project Summary

Flare Industries (hereafter to be called FI) was contracted by EOG RESOURCES c/o KAHUNA VENTURES to engineer, design, fabricate, and supply (1) SFVP-1042 Flare system with Model 850 Pilots. This system was designed by FI to meet the conditions and engineering criteria as specified by EOG RESOURCES and to match previous FI project 10-0246-B. Critical commercial information relating to the project is summarized below.

| Flare Industries Job Number | 140663-B |
|-----------------------------|----------------------|
| Customer Purchase Order | 210431 |
| Customer Name | EOG Resources |
| Customer Location | Hereford, CO |
| Job Location | Hereford, CO |
| Date Shipped | November, 19th, 2014 |



1.2 Scope of Supply

The following table provides an outline of the major equipment provided by FII:

| | | | | or equipment provided by FII: |
|------|-----|----------------------------------------------|----------------|---------------------------------------------------------------------------------------------------------------------------------------------------------------------------|
| Item | Qty | Description | Material | Notes |
| 1 | 2 | 54' Freestanding Flare Stack (60' OAH) | CS | 10" Inner Gas Riser; 42" Outer Air Riser 10" Waste Gas Inlet Baseplate Assembly |
| 2 | 2 | 6' Flare Tip | 316SS CS | Dynamic Purge Seal10" Gas Connection42" Plate Flange Connection |
| 3 | 6 | Model 850 Pilot | 310SS 316SS | Dual Element Type-K thermocouples Direct Spark Ignition Continuous Pilot Relight Function Retractable for easy maintenance |
| 4 | 2 | High Volume/ High Pressure Blower | | Vane Axial Blower50HP480VAC, 3 Phase, 60 Hz |
| 5 | 2 | AC-AL-TC Control System | | NEMA 4X enclosure Automatic Continuous System Ignition Self-supporting Control Stand |

1.3 Process Conditions

The flare system was designed according to the following process specifications as defined by the customer:

| Condition | |
|-----------------------------|------------------------------------------|
| Maximum Inlet Flow Rate: | 20 MMSCFD |
| Smokeless Flow Rate: | 0 to 20 MMSCFD |
| Molecular Weight: | 23.8 |
| Flare Gas BTU Value: | 1,297 BTU/SCF |
| Inlet Temperature: | 80ºF |
| Inlet Pressure Required: | 4.45 psig |
| Max Heat Radiation @ Grade: | 1,454 BTU/ft ² /hr (including |
| | solar) |



1.4 Site Conditions

The following site conditions were used to complete the engineering design of the flare system:

| Design Wind Speed | 90 mph (Structural) 20 mph (Radiation) | |
|-------------------|-------------------------------------------|--|
| Seismic Zone | UBC Zone 0 | |
| Elevation | 2000 ft | |
| Humidity | High | |

1.5 Utility Requirements

Utility requirements of the system are as follows:

| Pilot Fuel Gas | 65 SCFH of Natural Gas @ 8-10 PSIG (per pilot) |
|----------------|------------------------------------------------------------------------|
| Purge Gas | 83 SCFH |
| Electrical | 1 Phase / 60 Hz / 120VAC (Controls) 3Phase / 60Hz / 480VAC (Blower) |



2.0 ASSEMBLY, INSTALLATION, AND COMMISSIONING PROCEDURES

The following sections outline the procedures required to successfully install the flare system. The intent of these procedures is to provide guidance and general steps to complete the installation. These procedures are not intended to be a substitute for experienced installation personnel. Field assembly and erection of the flare is outside the scope of work to be provided by Flare Industries, Inc., and is the sole responsibility of others. It is understood that the field contractor retained by the customer is familiar with the assembly and erection of tall towers.

The following guidelines provide approximate on-site requirements for personnel and equipment:

| Item | Function | Duratio n | Requirements |
|-------------------------------------|----------------------------------------------|--------------|-------------------------------------------------------|
| Crane | Lift flare stack | As Rqd. | Lifting slingsSpreader bar |
| Tailing Crane | Control base of flare stack during erection | As Rqd. | Necessary rigging for tailing operations |
| Electrician and one assistant | Install controls and electronic pilots | As Rqd. | |

2.1 Flare Stack Assembly and Preparation

This section provides guidance for the preparation of the flare stack prior to erection. All steps described within this section are performed with the flare in the horizontal position. It is the responsibility of the field crew to verify and perform the preparation procedure as required and in accordance with the proper codes.

- 2.1.1 Inspect the flare tip, flare riser, and pilot track for any damage that may have occurred during shipment. Also, be sure the flare tip and flare riser are free of any obstructions that may inhibit flow. If any damage is found, contact Flare Industries, immediately (contact information located in section 7.3.)
- 2.1.2 With the stack in the horizontal position, weld the Inner Gas Tip to the top of the inner gas riser section.
- 2.1.3 Bolt the Outer Tip assembly to the flanged connection on the top of the flare stack after installing the supplied gasket.
- 2.1.4 The flare is ready for erection.



2.2 Flare Stack Erection Procedure

This section describes the general procedure required to erect the flare stack. Special care must be taken during the erection procedure to prevent injury and damage. Only field contractors with experience and familiarity with tall tower erection should attempt to install the flare stack. The following steps should serve only as guidance, not the definitive source for the erection activities.

The following is a list of major equipment that is required to complete the procedures described within this section:

- Survey equipment including transit
- Lifting crane
- Tailing crane
- 2.2.1 Secure lifting slings to each of the two lifting trunnions on the flare stack.
- 2.2.2 Secure a tailing line to the end of the stack with a shackle through one of the bolt holes in the base plate.
- 2.2.3 Raise the tip and stack assembly in the horizontal position to approximate elevation 10'. From this height, lift the stack into the vertical position.
- 2.2.4 Raise and swing the vertical stack over the foundation and align it correctly over the anchor bolts. Remove tailing line connection from the base plate assembly.
- 2.2.5 Carefully lower the flare stack onto the foundation anchor bolts.
- 2.2.6 Secure the flare stack to the foundation using the anchor nuts and the provided plate washers.
- 2.2.7 Remove the lifting crane connection.
- 2.2.8 Attach pilot tracks to the flare riser and tip.
- 2.2.9 Remove the Model 850 electronic pilots from their crate and inspect for any damage that may have occurred during shipment. If any damage is found, contact Flare Industries immediately.
- 2.2.10 Insert the pilot wheels into the end of the track nearest the base of the flare and roll the pilot a few feet along the pilot track.
 - NOTE: Ensure care is taken to prevent catching or damaging the pilot harness as the pilot is deployed.
- 2.2.11 Remove the Pilot Gas Manifold from the crate, and mount to the provided unistrut mounting bracket using the included Unistrut Pipe Clamp.



- 2.2.12 After checking the pilot, remove the $\frac{1}{4}$ " diameter winch cable and winch from the shipping crate.
- 2.2.13 Mount the winch onto its mounting plate using the supplied hardware.
- 2.2.14 Attach one end of the ¼" winch cable to the winch spool and reel several feet of cable onto the spool.
- 2.2.15 Run the loose end of the winch cable through the pulley, located on the flare tip, and back to the winch plate. The winch cable should pass over the pulley and away from the flare stack so that the loose end is on the outer edge of the pulley.
- 2.2.16 Attach the loose end to the pilot with the provided cable clamps.
- 2.2.17 Attach the blower support assembly to the base of the flare stack using the provided hardware.
- 2.2.18 Attach blower to the blower duct on the flare stack assembly using the provided hardware.
- 2.2.19 Connect the customer waste gas service line to the waste gas inlet nozzle (N1) provided for this purpose.
- 2.2.20 Connect the pilot gas line to the provided pilot gas nozzle (C2).
- 2.2.21 Following the erection, check for any damage that may have occurred during the erection procedure.

2.3 System Controls Installation Procedure

This section will guide the installation crew through the general procedure used to install the system controls. The installation should adhere to local electrical code and be conducted by a licensed electrician. Failure to properly ground equipment will result in equipment damage and may injure personnel. It is the responsibility of the customer to provide the appropriate cables and wiring where necessary. The following steps should serve only as guidance, not the definitive source of reference.

For piping and electrical connections, please reference drawings E38CX0-A-800, E38CX0-A-801, E38CX0-A-802, E38CX0-A-803, E38CX0-A-804, E38CX0-A-805, E38CX0-A-806, E38CX0-A-807, E38CX0-A-808, E38CX0-A-809, E38CX0-A-810, E38CX0-A-811, E38CX0-A-812, E38CX0-A-813, E38CX0-A-900, E38CX0-A-901 & E38CX0-A-902.

2.3.1 Remove the AC-AL-TC Control System from its packaging and inspect the equipment for any damage that may have occurred during shipment. If any damage is found, contact Flare Industries immediately (contact information located in section 7.3.)



- 2.3.2 Locate and position the AC-AL-TC Control Stand at the desired location for installation.
- 2.3.3 Secure the AC-AL-TC Control Stand as required.
- 2.3.4 Following the installation, check for any damage that may have occurred during the process.
- 2.3.5 Connect the customer electrical service and customer alarm connections to the ignition controls box.
- 2.3.6 Install Type-K thermocouple wires, inside minimum ½" galvanized conduit, between the AC-AL-TC controls enclosure and the flare stack.
- 2.3.7 Install ignition power connection cable between the AC-AL-TC controls enclosure and the flare stack.
- 2.3.8 Verify all electrical connections are tight, as there may have been some loosening and/or settling during shipment.



3.0 SAFETY CONSIDERATIONS

GENERAL COMMENTS FOR SAFETY DURING FLARE OPERATION

CAUTION! Safety during flare operation requires that there is not an air / gas mixture in the flare system at any time. Purge gas, which can consist of either inert gas (preferred), fuel gas, or waste gas, should be used in such quantities as to avoid the entry of air into the flare system. A purge of the flare should occur prior to the release of waste gas into the system and before the ignition system is turned on. Explosion hazards can exist during the operation of a flare system **only** if the ignition system has been initiated and before the flare is purged. Therefore, the ignition system must not be operated until the system is thoroughly purged and the flare system is absolutely gas tight.

3.1 Pre-Start-Up Checklist

The following items should be checked before starting the flare:

- Verify that all electrical devices are connected to the proper power sources.
- All system lines should be dry and free of dirt and foreign matter.
- Check that all drain and vent valves are closed and that all drain and vent plugs are tightly secured.
- Check all control valves for proper function.
- Purge the flare for 10 volumes of the flare and flare header (20-30 minutes minimum).
- To provide smokeless operation of the Air Assist Flare, the Blower should always be in operation whenever the flare is operating.

3.2 System Purge

There is danger of severe explosion in the flare system if the flare is ignited before the flare system has been purged. Ensure that a system purge from the beginning of the system, all the way to the flare, occurs using a volume of non-condensable gas equal to ten times the volume of the flare system. The flare system includes all piping from relief valves toward the flare and riser to the elevation of the flare at the point of combustion.

Suitable purge gases include natural gas, propane, nitrogen, inert gas, carbon dioxide or butane, if temperature level is 32°F or above. Steam as purge volume is not recommended for two reasons. The first is that the steam is at an elevated temperature and the steam content of the flare will shrink as the steam cools and condenses to draw air back into the flare system. The second is that as the steam condenses, water will be present in the flare system partially blocking the system, which presents a freezing hazard. In addition, the condensation accelerates corrosion.

Installation, Operation and Maintenance Manual 140663-M01-0001, Revision 0 12/23/2014



The flare should be ignited only after the "SYSTEM PURGE" is complete as outlined above and preferably as the purge gas is being admitted. If the purge gas is combustible, the burning of the purge gas at the flare will be proof of ignition.

Additionally, this flare system is designed to provide smokeless operation at a full flow status. Both to ensure smokeless operation and to provide a complete system purge, the blower must be started and run for at least one minute prior to placing the flare system in operation.



4.0 OPERATING SUMMARY

The operating summary outlines the critical information related to the AC-AL-TC control system. The following sections will help the system operator become familiar with the controls, initial settings, and general operation of the system. System purge must be completed prior to any ignition or waste gas combustion.

4.1 Controls Summary

The AC-AL-TC control system was designed by FI to provide reliable control and monitoring of the flare system. By design, the control system will operate and monitor the flare system with minimal user input. The following is a list of the major components used to control the flare system:

- Type-K thermocouple Collects pilot temperature readings
- Temperature controller Monitors pilot temperatures
- Timer Controls ignition sequence timing
- Ignition Transformer Generates high-energy spark to ignite pilots
- Model 850 Pilots Ignite waste gas flow

Before any ignition sequences begin, the flare should be checked and fully purged as described in section 3.0. The blower must be started prior to initiating start-up of the flare system, to complete the purge of the flare system.

Startup of the flare begins by turning ON the Main power. The Power On and System Failure Indicators will illuminate. As soon as the system is energized, the ignition transformer will generate a high-energy spark for the Model 850 Pilot. When pilot fuel gas is supplied to the Model 850 Pilot, the high-energy spark will ignite the fuel gas and light the pilots.

Once the pilot is ignited, the temperature controller and Type-K thermocouples are used to monitor the status of the pilots. Upon reaching the minimum pilot temperature set point (250°F.), SYSTEM FAILURE indicators will go out. In the event of system failure, the temperature at the pilot nozzle will begin to decrease. When pilot temperature falls below the temperature controller set point (250°F), the SYSTEM FAILURE light will illuminate and activate the customer alarm. The indicator and customer alarm will remain activated until ignition is successful and the pilot temperature reaches 250°F.



4.2 Customer Contacts

Customer contacts are used to communicate data between the flare's control system and the existing customer controls. These contacts typically communicate critical information such as pilot failure notification, liquid level status, or various service pressures. The following customer contacts have been provided:

| Interlock Description | Point of Connection |
|-----------------------------|---------------------|
| Ignition Failure – Pilot #1 | TBA 190220 B to C |
| Ignition Failure – Pilot #2 | TBA 190221 B to C |
| Ignition Failure – Pilot #3 | TBA 190222 B to C |

4.3 Initial Settings

All system controls have been properly adjusted before shipment and arrive ready for operation. The following settings are to be used for information only and should only be used for modification in the event of necessary adjustment.

| Tag# | Component | Set Point |
|----------|-----------------------------------|-----------|
| 1TC90001 | Temperature controller (Pilot #1) | 250°F |
| 1TC90002 | Temperature controller (Pilot #2) | 250°F |
| 1TC90003 | Temperature controller (Pilot #3) | 250°F |

4.4 Schedule of Alarms

| Alarm | Associated Component | Cause | Effect | |
|----------------|----------------------------|-------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------|---------------------------------------------------------------------------------------------------|--|
| SYSTEM FAILURE | Temperature Controller | Indicates that the temperature controller has failed to sense the lit pilot for the period of time determined by the timer setting. | Customer alarm contacts energized IGNITION FAILURE LIGHT illuminates | |



4.5 Schedule of Operators and Indicators

This section provides a description of the operators and indicators located on the main control panel. One should become familiar with the meaning and function of each component prior to any attempt to operate the system.

| Item | Operator or Indicator | Tag # | Function | | | | | |
|-------|--------------------------|----------|----------------------------------------------------------------------------------------------------------------------------------------------|--|--|--|--|--|
| | Switches and Pushbuttons | | | | | | | |
| 1 | MAIN POWER OFF/ON | 1SS90001 | Controls main power for entire control system Must be in the ON position to operate system | | | | | |
| Note: | | | When the MAIN POWER OFF/ON switch is turned to the ON position, ignition sequence (sparking) begins immediately. | | | | | |
| | | Indi | cators | | | | | |
| 1 | POWER ON | 1LT90201 | Indicates the system is energized | | | | | |
| 2 | SYSTEM FAILURE | 1LT90202 | Indicates that pilot #1 is out and the system is not attempting to re-light the pilot | | | | | |
| 3 | SYSTEM FAILURE | 1LT90203 | Indicates that pilot #2 is out and the system is not attempting to re-light the pilot | | | | | |
| 4 | SYSTEM FAILURE | 1LT90204 | Indicates that pilot #3 is out and the system is not attempting to re-light the pilot | | | | | |

4.6 System Operation

This section describes the automatic operation of the ignition control system. While operating, the system controls will monitor the Model 850 Pilot temperature. If pilot temperature drops below 250°F the System Failure light illuminates and generates a system failure alarm while the pilot continues to spark.



- 4.6.1 Fully purge the flare system according to section 3.2.
- 4.6.2 Start the Blower. Blower operation as the flare is started up will assist in the completion of the purge process of the flare and ensure that as waste gas is admitted into the flare, the flare will maintain smokeless operation.

NOTE: In some cases, igniting the pilot may be difficult with the blower running. In the event that it is impossible to get the pilot to light while the blower is running, complete a one (1) minute purge of the air riser using the blower. Secure the blower. Start the pilot and then immediately re-initiate blower operation.

- 4.6.3 Open the valve controlling the pilot fuel line.
- 4.6.4 Turn the MAIN POWER switch (1SS90001) to the ON position. Once the system is energized, the pilot will automatically begin the ignition sequence.
- 4.6.5 Within several minutes, the SYSTEM FAILURE indicators should go out, indicating the pilots have ignited. The time delay is a result of the time required for the pilot thermocouple to reach the minimum temperature set point (250°F). Keep in mind that the time delay may vary depending on ambient conditions. If the pilot does not ignite, refer to section 6.0 for troubleshooting.
- 4.6.6 Once operating, the system is ready to accept waste gas flow.

4.7 System Shutdown

The system should only be shut down if the flare is intended for intermittent use. Once the system has been shut down, any ignition operation and system monitoring will end.

- 4.7.1 Verify that waste gas flow has ceased and that any corresponding waste gas control valves are fully closed.
- 4.7.2 Close the valves controlling the pilot fuel gas. This will extinguish the Model 850 Pilots.
- 4.7.3 Turn the MAIN POWER OFF/ON switch to the OFF position. The POWER ON indicator should go out, indicating the system has been shut down.
- 4.7.4 Stop the blower.



5.0 SYSTEM MAINTENANCE

The following sections summarize the required maintenance of the flare system. Diligence to the maintenance is required to ensure the system remains in optimum operating condition. Failure to maintain the system as required could lead to damage or malfunction.

5.1 Model 850 Pilot

| Maintenance Number | Action | Monthly | Quarterly | Semi- Annually | Annually | |
|-----------------------|--------------------------------------------------------------------------------------|---------|-----------|-------------------|----------|--|
| Inspect entire | nspect entire flare, base assembly, and guywire package for structural integrity and | | | | | |
| | any extreme wind event or seis | | | | | |
| IM-1 | Verify the pilot is operating by visual check at control panel and flare tip | ✓ | | | | |
| IQ-1 | Verify electronic ignition is operating by manually igniting all pilots | | ✓ | | | |
| IS-1 | Remove pilot strainer and clear debris | | | ✓ | | |
| IS-2 | Inspect pilot head for flame damage or excessive corrosion | | | ✓ | | |



5.2 AC-AL-TC Control System

| Maintenance Number | Action | Monthly | Quarterly | Semi- Annually | Annually | | |
|-----------------------------------------------------------------|---------------------------------------------------------------------------------------|----------|-----------|-------------------|----------|--|--|
| | Since some components are susceptible to damage by electrostatic discharge, check the | | | | | | |
| control system for proper operation following lightning storms. | | | | | | | |
| EM-1 | Check control switches to verify each operates freely, without binding | ✓ | | | | | |
| EM-2 | Check all indicators to verify that each is functioning appropriately | ✓ | | | | | |
| EQ-1 | Inspect each enclosure for leaks and ensure that all properly seal | | ✓ | | | | |
| EQ-2 | Confirm that all customer contacts are in working order | | ✓ | | | | |
| EA-1 | Check that all electrical connections are tight | | | | ✓ | | |
| EA-2 | Inspect system wiring for deterioration, discoloration, corrosion fraying | | | | ✓ | | |
| EA-3 | Inspect control system for proper grounding connection | | | | ✓ | | |



5.3 Flare Stack and Tip

| Maintenance Number | Action | Monthly | Quarterly | Semi- Annually | Annually | |
|---------------------------------------------------------------------------------------|-----------------------------------------------------------------------------------|--------------|-----------|-------------------|----------|--|
| Inspect entire flare, base assembly, and guywire package for structural integrity and | | | | | | |
| damage after | any extreme wind event or seis | mic activity | | | | |
| SQ-1 | Verify all process connections are properly connected and in operating conditions | | ✓ | | | |
| SS-1 | Examine anchor bolts and base support plates assembly for corrosion | | | ✓ | | |
| SS-2 | Check foundation for heat damage or excessive cracking due to service loads | | | ✓ | | |
| SA-1 | Inspect flare riser for corrosion and repair as necessary | | | | ✓ | |
| SA-2 | Check flare tip for flame damage and corrosion | | | | ✓ | |
| SA-3 | Inspect flare tip flange bolts and verify each bolt's torque | | | | ✓ | |



6.0 TROUBLESHOOTING

The following sections provide troubleshooting to help solve any potential problems that may arise during the operation of the flare system. If required, contact Flare Industries, Inc. for technical assistance.

6.1 Model 850 Pilot

| Problem | roblem Cause Solut | |
|-----------------------------------------------------------------------------------|-------------------------------------------------------------|--------------------------------------------------------------|
| Pilot will not light | System power is not on | Energize system |
| | Ignition transformer has failed | Replace transformer |
| | Lack of pilot fuel gas | Verify that all fuel gas valves are open |
| | Fuel gas lines may be blocked | Clean strainers on pilot and customer fuel gas lines |
| | Fuel gas lines may contain condensation | • Drain condensation from fuel gas lines |
| | Insufficient fuel gas pressure | Verify fuel gas is at min. 8 psig |
| | 10 | Increase fuel gas pressure |
| | Inspirator orifice is | Contact FII for replacement |
| | incorrectly sized | orifice |
| Pilot will not stay lit | Fuel gas is not on | Turn on fuel gas |
| photocolymerchicler(1,254,000,000) 8,000,000 (0,000,000,000,000,000,000,000, | Fuel gas pressure is too low | Set fuel gas pressure to 8 psig |
| | Fuel is contaminated | Upgrade fuel supply |
| | Fuel gas does not have BTU | Upgrade fuel supply |
| | value high enough to sustain ignition | |
| | Pilot nozzle is damaged | Replace pilot nozzle |



6.2 Ignition Control System

| Problem | Cause | Solution | |
|--------------------------------------------------------------------------|-------------------------------------|------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------|--|
| | Associated control relay is damaged | Replace appropriate control relay | |
| Pilot is ignited but the controls system does not acknowledge the status | Pilot thermocouple is damaged | At the thermocouple junction box, switch the pilot thermocouple connections to the second thermocouple element Replacement thermocouple is required | |
| | Temperature controller is faulty | Replace temperature controller | |
| | System wiring is damaged | Check all wiring and connections | |



7.0 RECOMMENDED SPARE PARTS

The following sections include lists of recommended spare parts for the flare system. When ordering spare parts, please indicate the FII part number and the FII project number. This information will help expedite your orders and ensure you receive exactly what you require.

7.1 Model 850 Pilot

| Item | FII Part # | Description | For S.U. and Comm. | For 2 Years Operation |
|------|----------------|-------------------------------------------------|-----------------------|--------------------------|
| 1 | TRAIGN10K01 | Ignition Transformer Pri. 120VAC, Sec 10KVDC | 0 | 1 |
| 2 | PLTSPARKPLUG13 | Model 850 Pilot Spark Plug | 1 | 2 |
| 3 | TEMTC116DK01 | Thermocouple, Type KK, Dual Ele. | 1 | 1 |
| 4 | PLTINSP03-SS | Model 850 Pilot Inspirator | 0 | 1 |
| 5 | STR005020201 | Model 850 Pilot Strainer, SS | 0 | 1 |
| 6 | TEMTCNHX-K-MF | Ceramic Thermocouple Connector | 2 | 4 |

7.2 Ignition Control System

| Item | FII Part # | Description | For S.U. and Comm. | For 2 Years Operation |
|------|------------------|------------------------|-----------------------|--------------------------|
| 1 | ELETIMER00 | Timer (Omicron) | 0 | 1 |
| 2 | RELSS40A06 | Control Relay | 0 | 1 |
| 3 | RELGEN2P120A1501 | General Relay, 120VAC | 0 | 1 |
| 4 | FUS0030GGM301 | Fuse, 3Amp-250V, Glass | 2 | 3 |
| 5 | FUS0010GGM101 | Fuse, 1Amp-250V, Glass | 2 | 3 |
| 6 | TEMTICE5CN04 | Temperature Controller | 1 | 2 |



7.3 Contact Information

INTERNATIONAL HEADQUARTERS

Flare Industries, an Aereon Company 16310 Bratton Lane Building 3, Suite 350 Austin, Texas 78728

TOLL-FREE PHONE: (800) 475-9473 FAX: (512) 836-3025 WEB: www.aereon.com

NEW EQUIPMENT SALES

PHONE: (512) 836-9473 EMAIL: sales@aereon.com

SPARE PARTS

PHONE: (512) 836-9473 EXT 145 EMAIL: spareparts@aereon.com

SERVICE & TECHNICAL ASSISTANCE

PHONE: (512) 836-9473 EXT 145 EMAIL: service@aereon.com

SHIPPING DEPARTMENT HOURS

Monday-Friday: 8:00AM-3:00PM CST (U.S.) Saturday-Sunday: CLOSED

CONTACT FLARE INDUSTRIES LOGISTICS COORDINATOR FOR APPOINTMENT

(512) 836-9473

OFFICE HOURS

Monday-Friday: 8:30AM-4:30PM CST (U.S.) Saturday-Sunday: CLOSED



8.0 PROJECT DRAWINGS

| Document # | Description |
|--------------|----------------------------------------------------|
| 140663-B-P01 | Piping & Instrumentation Diagram |
| 140663-B-G01 | General Arrangement, SFVP-1042 Air Flare System |
| 140663-B-G05 | General Arrangement, AC-AL-TC Control Stand |
| | |
| E38CX0-A-700 | Drawing Directory & Symbol Legend |
| E38CX0-A-701 | Wiring & General Notes |
| E38CX0-A-800 | 1CP800 – Flare Control Panel Layout |
| E38CX0-A-801 | 1CP800 – Flare Control Panel BOM |
| E38CX0-A-802 | 1CP800 – Flare Control Panel Operator Detail |
| E38CX0-A-803 | 1CP803 - Ignition XFMR Control Panel Layout |
| E38CX0-A-804 | 1CP803 – Ignition XFMR Control Panel BOM |
| E38CX0-A-805 | 1CP803 – Ignition XFMR Operator Detail |
| E38CX0-A-806 | 1CP806 - Ignition XFMR Control Panel Layout |
| E38CX0-A-807 | 1CP806 – Ignition XFMR Control Panel BOM |
| E38CX0-A-808 | 1CP806 – Ignition XFMR Operator Detail |
| E38CX0-A-809 | 1CP809 - Ignition XFMR Control Panel Layout |
| E38CX0-A-810 | 1CP809 – Ignition XFMR Control Panel BOM |
| E38CX0-A-811 | 1CP809 – Ignition XFMR Operator Detail |
| E38CX0-A-812 | 1JB812 & 1JB806A-C – Terminal Jbox General Layout |
| E38CX0-A-813 | 1JB812 & 1JB806A-C – Terminal Jbox Terminal Detail |
| E38CX0-A-900 | Ladder Logic Diagram |
| E38CX0-A-901 | Ladder Logic Diagram |
| E38CX0-A-902 | Ladder Logic Diagram |



9.0 WARRANTY INFORMATION

If within 12 months after the date of notice of availability for shipment, or one year after startup, whichever occurs first, any Goods furnished by Seller prove to be defective in material or workmanship, and Seller is so notified in writing, upon examination by Seller, Seller will, at Seller's discretion, either repair the Goods or supply identical or substantially similar replacement Goods, F.O.B. manufacturing facility. Any repaired or replacement Goods will be warranted against defects in material or workmanship for the unexpired portion of the warranty applicable to the particular Goods. Goods not manufactured by Seller are subject only to warranties of Seller's vendors and Seller hereby assigns to Buyer all rights in such vendors warranties, provided however. Seller shall furnish to the Buyer reasonable assistance in enforcing such rights. Seller will not be responsible for costs of making access for, or of export/import, shipment, removal or installation of any items needed to repair or replace any defective Goods. Inexpensive items requiring repairs or replacement and routine maintenance-related or consumable items shall be outside the scope of these limited warranties. With regard to warranty-related remedial work, the Seller will not be responsible for materials or workmanship of others or shipment, labor and other related expenses for any work performed by others in the repair or replacement of defective Goods, without Seller's prior written consent. Seller's performance guarantees, if any, shall be deemed to be met by a satisfactory demonstration of the performance guarantees during a performance test, which shall be the responsibility of the Buyer, pursuant to mutually agreed-upon test procedures. If the performance test is not completed within 45 days after notice of availability for shipment, the performance test shall be deemed to be satisfactorily performed for any and all purposes.

These limited warranties will be voided if: (a) the Goods were not stored, installed, maintained or operated in accordance with accepted U.S. industrial practice and any specific instructions provided by Seller; (b) the Goods were subjected to any accident, misapplication, environmental contaminant, corrosion, abrasion, abuse or misuse; (c) Buyer used, repaired, or modified the Goods after discovery of the defect without Seller's prior written consent to continue use; or (d) Buyer fails to permit Seller to examine the Goods and operating data or fails to furnish routine operating data sufficient to determine the nature of the defect claimed.

THERE ARE NO OTHER WARRANTIES, EXPRESS OR IMPLIED EXCEPT, AS EXPRESSLY PROVIDED HEREIN; SELLER EXTENDS NO IMPLIED WARRANTY OF MERCHANTABILITY OR FITNESS FOR PARTICULAR PURPOSE. NO WARRANTY, EITHER EXPRESS OR IMPLED, IS GIVEN AS TO THE CAPACITY, EFFICIENCY OR PERFORMANCE OF THE GOODS, EXCEPT AS MAY BE EXPRESSLY AGREED TO BY THE PARTIES IN WRITING.

NSR Application A0001327 Fairway Compressor Station and Water Transfer Facility F026209 July 20, 2015

Air Quality Division Application for NSR Permit

NSR Application

Date application received: 07/20/2015 Is this a legacy NSR Application? No

This information should be filled out for each New Source Review (NSR) application. An NSR permit is required for all air contaminant sources (emissions units) installed or modified after January 1, 1974. See the application instructions for additional information.

| Emission Unit application reason summary : | Construction | Synthetic Minor |
|--------------------------------------------|----------------|------------------|
| | x Modification | Temporary Permit |
| | Reconstruction | Other |

Facility Type: Sage Grouse:

Purpose of Application

Please summarize the reason this permit is being applied for.

modify the Fairway Compressor Station to reflect the as built configuration, include new equipment, include 500 hours of flaring due to routine maintenance, and include new equipment associated with the Water Transfer Facility

Has the facility changed location or is it a new/greenfield facility? No Does production at this facility contain H2S? No

Federal Rules Applicability - Facility Level

Prevention of Significant Deterioration (PSD)

Not affected

These rules are found under WAQSR Chapter 6, Section 4.

Non-Attainment New Source Review
These rules are found under WAQSR Chapter 6, Section

Not affected

- Trade Secret Information - One or more Emissions Units in this application contains trade secret information.

No

 Permit Application Contact - Newly created contacts and application contact changes will be saved when the application is saved.

| (303) 262-9946 | | Curtis_Rice@eogresources.com |
|------------------------------|------------------------------------|------------------------------|
| Street Address | City/Township, State | Zip Code |
| 600 17th Street, Suite 1000N | Denver, CO | 80202 |
| Name | Title | Company |
| Curtis Rice | Senior Environmental Specialist | EOG Resources, Inc. |

Modeling Section

Ambient Air Quality Impact Analysis: WAQSR Chapter 6, Section 2(c)(ii) requires that permit applicants demonstrate that a proposed facility will not prevent the attainment or maintenance of any ambient air quality standard.

Has the applicant contacted AQD to determine if modeling is required? No ls a modeling analysis part of this application? No ls the proposed project subject to Prevention of Significant Deterioration (PSD) No requirements?

- Application Attachments

| Required Attachment | Public Document Id | Attachment Type | Description |
|------------------------|-----------------------|-------------------------------------|-----------------------|
| × | 6810 | Emissions Calculations | emission calculations |
| X | 6811 | Cover Letter/Project Description | Cover Letter |

- Notes

| | - | |
|--------------|------|------|
| User Name | Date | Noto |
| USCI IVAILIE | Date | Note |
| | | |

AQD EU ID: BVC001

AQD EU description:

Company EU ID: BVC1

Company EU Description: compressor

blowdown - routed

to flare

- Source Installation or Modification Schedule – Select reason(s) for this emissions unit being included in this application (must be completed regardless of date of installation or modification):

Modification

When will you begin to modify the air contaminant source? 07/20/2015

- Emission Unit Type Specific Information

Emission Unit Type: Blow-down/Venting/Well Completion

- Potential Operating Schedule - Provide the operating schedule for this emissions unit

Hours/day: 24 Hours/year: 8760

Emissions Information "Potential to emit" means the maximum capacity of a source to emit any air pollutant under its physical and operational design. Any physical or operational limitation on the capacity of a source to emit an air pollutant, including air pollution control equipment and restrictions on hours of operation or on the type or amount of material combusted, stored or processed, shall be treated as part of its design if the limitation is enforceable by the EPA and the Division. This term does not alter or affect the use of this term for any other purposes under the Act, or the term "capacity factor" as used in Title IV of the Act or the regulations promulgated thereunder.

Basis for Determination Options:

- Manufacturer Data
- Test results for this source
- Similar source test results
- GRICalc
- Tanks Program
- AP-42
- Other. If this is selected, attach a document with a description of the method used.

Criteria Pollutants:

| Pollutant | Pre- | Efficiency | Standards | Potential to | Potential to | Basis for |
|-----------------------------------------------------------------|---------------------------------------------------|-----------------------------|-----------|-------------------------|--------------------------|--------------------|
| | Controlled Potential Emissions (tons/yr) | Potential to Emit (PTE)* | Units* | Emit (PTE) (lbs/hr)* | Emit (PTE) (tons/yr)* | Determinatio n* |
| Particulate emissions (PE/PM) (formerly particulate matter, PM) | 0 | 0 | | 0 | 0 | |
| PM # 10 microns in diameter (PE/PM10) | 0 | 0 | | 0 | 0 | |
| PM # 2.5 microns in diameter (PE/PM2.5) | 0 | 0 | | 0 | 0 | |
| Sulfur dioxide (SO2) | 0 | 0 | | 0 | 0 | |

| Nitrogen oxides (NOx) | 0 | 0 | 0 | 0 | |
|------------------------------------------|-----|---|-----|---|-------|
| Carbon monoxide (CO) | 0 | 0 | 0 | 0 | |
| Volatile organic compounds (VOC) | 1.6 | 0 | 0 | 0 | AP-42 |
| Lead (Pb) | 0 | 0 | 0 | 0 | |
| Total Hazardous Air Pollutants (HAPs) | 0.1 | 0 | 0 | 0 | AP-42 |
| Fluoride (F) | 0 | 0 | 0 | 0 | |
| Hydrogen Sulfide (H2S) | 0 | 0 | 0 | 0 | |
| Mercury (Hg) | 0 | 0 | 0 | 0 | |
| Total Reduced Sulfur (TRS) | 0 | 0 | . 0 | 0 | |
| Sulfuric Acid Mist (SAM) | 0 | 0 | 0 | 0 | |

| Pollutant | Pollutant Category | Pre- Controlled | Efficiency Potential to | | | Potential to Emit (PTE) | Basis for Determinati |
|-----------|-----------------------|-------------------------------------|----------------------------|-------|-----------|-------------------------|--------------------------|
| | | Potential Emissions (tons/yr) | Emit (PTE)* | Units | (lbs/hr)* | (tons/yr)* | on* |

Greenhouse Gases (GHGs):

| Pollutant | Pollutant Category | Pre- Controlled Potential Emissions | Efficiency Potential to Emit (PTE)* | Standards Units* | Potential to Emit (PTE) (lbs/hr)* | Basis for Determinati on* |
|-----------|-----------------------|----------------------------------------------|-------------------------------------------|---------------------|-----------------------------------------|---------------------------------|
| | | (tons/yr) | , | | | |

^{*} Provide your calculations as an attachment and explain how all process variables and emissions factors were selected. Note the emission factor(s) employed and document origin. Example: AP-42, Table 4.4-3 (8/97); stack test, Method 5, 4/96; mass balance based on MSDS; etc.

- Best Available Control Technology (BACT)

Was a BACT Analysis completed for this unit? No

Lowest Achievable Emission Rate (LAER)

Was a LAER Analysis completed for this unit? No

- Federal and State Rule Applicability

New Source Performance Standards (NSPS)
New Source Performance Standards are listed under 40
CFR 60 - Standards of Performance for New Stationary
Sources.

Not affected

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 61)

National Emissions Standards for Hazardous Air Pollutants (NESHAP Part 61) are listed under 40 CFR 61. (These include asbestos, benzene, beryllium, mercury, and vinyl chloride).

Not affected

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63)

Not affected

^{**} AQD Calculated - See 'Help' for more information.

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63) standards are listed under 40 CFR 63.

Not Affected

Prevention of Significant Deterioration (PSD)
These rules are found under WAQSR Chapter 6, Section 4.

Not Affected

Non-Attainment New Source Review
These rules are found under WAQSR Chapter 6, Section

| Required Attachment | Public Document | Attachment Type | Description |
|------------------------|-----------------|-----------------|-------------|
| Attachment | Iu | | |

AQD EU ID: BVC002

AQD EU description:

Company EU ID: BVC2

Company EU Description: pigging - routed

to flare

- Source Installation or Modification Schedule – Select reason(s) for this emissions unit being included in this application (must be completed regardless of date of installation or modification):

Modification

When will you begin to modify the air contaminant source? 07/20/2015

- Emission Unit Type Specific Information

Emission Unit Type: Blow-down/Venting/Well Completion

- Potential Operating Schedule - Provide the operating schedule for this emissions unit

Hours/day: 24 Hours/year: 8760

Emissions Information "Potential to emit" means the maximum capacity of a source to emit any air pollutant under its physical and operational design. Any physical or operational limitation on the capacity of a source to emit an air pollutant, including air pollution control equipment and restrictions on hours of operation or on the type or amount of material combusted, stored or processed, shall be treated as part of its design if the limitation is enforceable by the EPA and the Division. This term does not alter or affect the use of this term for any other purposes under the Act, or the term "capacity factor" as used in Title IV of the Act or the regulations promulgated thereunder.

Basis for Determination Options:

- Manufacturer Data
- Test results for this source
- Similar source test results
- GRICalc
- Tanks Program
- AP-42
- Other. If this is selected, attach a document with a description of the method used.

Criteria Pollutants:

| Pollutant | Pre- | Efficiency | Standards | Potential to | Potential to | Basis for |
|-----------------------------------------------------------------|---------------------------------------------------|-----------------------------|-----------|-------------------------|--------------------------|--------------------|
| | Controlled Potential Emissions (tons/yr) | Potential to Emit (PTE)* | Units* | Emit (PTE) (Ibs/hr)* | Emit (PTE) (tons/yr)* | Determinatio n* |
| Particulate emissions (PE/PM) (formerly particulate matter, PM) | 0 | 0 | | 0 | 0 | |
| PM # 10 microns in diameter (PE/PM10) | 0 | 0 | | 0 | 0 | |
| PM # 2.5 microns in diameter (PE/PM2.5) | 0 | 0 | | 0 | 0 | |
| Sulfur dioxide (SO2) | 0 | 0 | | 0 | 0 | |
| Nitrogen oxides (NOx) | 0 | 0 | | 0 | 0 | |

| Carbon monoxide (CO) | 0 | 0 | 0 | 0 | |
|------------------------------------------|------|---|---|---|-------|
| Volatile organic compounds (VOC) | 84.7 | 0 | 0 | 0 | AP-42 |
| Lead (Pb) | 0 | 0 | 0 | 0 | |
| Total Hazardous Air Pollutants (HAPs) | 3.4 | 0 | 0 | 0 | AP-42 |
| Fluoride (F) | 0 | 0 | 0 | 0 | |
| Hydrogen Sulfide (H2S) | 0 | 0 | 0 | 0 | |
| Mercury (Hg) | 0 | 0 | 0 | 0 | |
| Total Reduced Sulfur (TRS) | 0 | 0 | 0 | 0 | |
| Sulfuric Acid Mist (SAM) | 0 | 0 | 0 | 0 | |

| Pollutant | Pollutant | Pre- | Efficiency | Standards | | Potential to | |
|-----------|-----------|---------------------------------------------------|-----------------------------|-----------|-----------|--------------|--------------------|
| | Category | Controlled Potential Emissions (tons/yr) | Potential to Emit (PTE)* | Units* | (lbs/hr)* | (tons/yr)* | Determinati on* |

Greenhouse Gases (GHGs):

| Pollutant | Pollutant | Pre- | Efficiency | Standards | Potential to | | |
|-----------|-----------|---------------------------------------------------|-----------------------------|-----------|-------------------------|------------|--------------------|
| | Category | Controlled Potential Emissions (tons/yr) | Potential to Emit (PTE)* | | Emit (PTE) (Ibs/hr)* | (tons/yr)* | Determinati on* |

^{*} Provide your calculations as an attachment and explain how all process variables and emissions factors were selected.

Note the emission factor(s) employed and document origin. Example: AP-42, Table 4.4-3 (8/97); stack test, Method 5, 4/96; mass balance based on MSDS; etc.

Best Available Control Technology (BACT)

Was a BACT Analysis completed for this unit? No

Lowest Achievable Emission Rate (LAER)

Was a LAER Analysis completed for this unit? No

- Federal and State Rule Applicability

New Source Performance Standards (NSPS)

New Source Performance Standards are listed under 40 CFR 60 - Standards of Performance for New Stationary Sources.

Not affected

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 61)

National Emissions Standards for Hazardous Air Pollutants (NESHAP Part 61) are listed under 40 CFR 61. (These include asbestos, benzene, beryllium, mercury, and vinyl chloride).

Not affected

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63)

National Emission Standards for Hazardous Air Pollutants

Not affected

^{**} AQD Calculated - See 'Help' for more information.

(NESHAP Part 63) standards are listed under 40 CFR 63.

Prevention of Significant Deterioration (PSD)
These rules are found under WAQSR Chapter 6, Section 4.

Not Affected

Not Affected

Non-Attainment New Source Review

These rules are found under WAQSR Chapter 6, Section 13.

| Required Attachment | Public Document Id | Attachment Type | Description |
|------------------------|-----------------------|-----------------|-------------|
|------------------------|-----------------------|-----------------|-------------|

AQD EU ID: DHY001

AQD EU description:

Company EU ID: DHY1

Company EU Description: 20 MMCFD TEG

dehydration unit

w/reboiler overheads

condenser, glycol flash separator, two (2) Kimray Model 21015PV glycol circulation

pumps, and 0.6 MMBtu/hr reboiler

heater

Source Installation or Modification Schedule - Select reason(s) for this emissions unit being included in this application (must be completed regardless of date of installation or modification):

Modification

When will you begin to modify the air contaminant source? 07/20/2015

Emission Unit Type Specific Information

Emission Unit Type: Dehydration Unit

Temperature of Wet Gas (F): 100

Water Content of Dry Gas 7.00

(lbs H2O/MMscf):

Pressure of Wet Gas (psig): 1,000.00

Manufacturer Name of Glycol Kimray

Circulation Pump:

Water Content of Wet Gas

(lbs H2O/MMscf):

Model Name and Number of 21015PV

Glycol Circulation Pump:

Flow Rate of Dry Gas 20.00

(MMscfd):

Type of Glycol Circulation Gas Pump:

Pump Volume Ratio 0.08

(acfm/gpm):

Actual LEAN Glycol 3.5000

Circulation Rate (gallons/minute):

Maximum LEAN Glycol 3.5000

Circulation Rate (gallons/minute):

Source of Motive Gas for field gas

Pump:

Additional Gas Stripping: No

Include Glycol Flash Yes Tank/Separator:

Flash Tank Off Gas Stream 4,160.00 (scf/hr):

Operating Temperature (F): 80

Where are Flash vapors compressor inlet

Operating Pressure (psig): 60.00

Routed?

Is Vessel Heated: No

Potential Operating Schedule - Provide the operating schedule for this emissions unit

Hours/day: 24 Hours/year: 8760

Emissions Information "Potential to emit" means the maximum capacity of a source to emit any air pollutant under its physical and operational design. Any physical or operational limitation on the capacity of a source to emit an air pollutant, including air pollution control equipment and restrictions on hours of operation or on the type or amount of material combusted, stored or processed, shall be treated as part of its design if the limitation is enforceable by the EPA and the Division. This term does not alter or affect the use of this term for any other purposes under the Act, or the term "capacity factor" as used in Title IV of the Act or the regulations promulgated thereunder.

Basis for Determination Options:

- Manufacturer Data
- Test results for this source
- Similar source test results
- GRICalc
- Tanks Program
- AP-42
- Other. If this is selected, attach a document with a description of the method used.

Criteria Pollutants:

| Pollutant | Pre- | Efficiency | Standards | Potential to | Potential to | Basis for |
|-----------------------------------------------------------------|---------------------------------------------------|-----------------------------|-----------|-------------------------|--------------------------|--------------------|
| | Controlled Potential Emissions (tons/yr) | Potential to Emit (PTE)* | Units* | Emit (PTE) (lbs/hr)* | Emit (PTE) (tons/yr)* | Determinatio n* |
| Particulate emissions (PE/PM) (formerly particulate matter, PM) | 0 | 0 | | 0 | 0 | |
| PM # 10 microns in diameter (PE/PM10) | 0 | 0 | | 0 | 0 | |
| PM # 2.5 microns in diameter (PE/PM2.5) | 0 | 0 | | 0 | 0 | |
| Sulfur dioxide (SO2) | 0 | 0 | | 0 | 0 | |
| Nitrogen oxides (NOx) | 0 | 0 | | 0 | 0 | |
| Carbon monoxide (CO) | 0 | 0 | | 0 | 0 | |
| Volatile organic compounds (VOC) | 900.8 | 0 | | 3.22 | 14.1 | GRI GlyCalc |
| Lead (Pb) | 0 | 0 | | 0 | 0 | |
| Total Hazardous Air Pollutants (HAPs) | 170.6 | 0 | | 0.23 | 1 | GRI GlyCalc |
| Fluoride (F) | 0 | 0 | | 0 | 0 | |
| Hydrogen Sulfide (H2S) | 0 | 0 | | 0 | 0 | |
| Mercury (Hg) | 0 | 0 | | 0 | 0 | |
| Total Reduced Sulfur (TRS) | 0 | 0 | | 0 | 0 | |
| Sulfuric Acid Mist (SAM) | 0 | 0 | | 0 | 0 | |

Hazardous Air Pollutants (HAPs) and Toxic Air Contaminants:

| Poll | utant | Pollutant | Pre- | Efficiency | Standards | Potential to | | |
|------|-------|-----------|---------------------------------------------------|-----------------------------|-----------|-------------------------|--------------------------|--------------------|
| | | Category | Controlled Potential Emissions (tons/yr) | Potential to Emit (PTE)* | Units* | Emit (PTE) (Ibs/hr)* | Emit (PTE) (tons/yr)* | Determinati on* |

Greenhouse Gases (GHGs):

| Pollutant | Pollutant | Pre- | Efficiency Standards | Potential to | Potential to | Basis for |
|-----------|-----------|------|----------------------|--------------|--------------|-----------|
| | | | , | | | |

| Category | Emissions | Potential to Emit (PTE)* | Units* | Emit (PTE) (lbs/hr)* | Emit (PTE) (tons/yr)* | Determinati on* |
|----------|-----------|-----------------------------|--------|-------------------------|--------------------------|--------------------|
| | (tons/yr) | L | | | | |

^{*} Provide your calculations as an attachment and explain how all process variables and emissions factors were selected. Note the emission factor(s) employed and document origin. Example: AP-42, Table 4.4-3 (8/97); stack test, Method 5, 4/96; mass balance based on MSDS; etc.

- Best Available Control Technology (BACT)

Was a BACT Analysis completed for this unit? No

Lowest Achievable Emission Rate (LAER)

Was a LAER Analysis completed for this unit? No

Federal and State Rule Applicability

New Source Performance Standards (NSPS)
New Source Performance Standards are listed under 40
CFR 60 - Standards of Performance for New Stationary
Sources.

Not affected

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 61)

National Emissions Standards for Hazardous Air Pollutants (NESHAP Part 61) are listed under 40 CFR 61. (These include asbestos, benzene, beryllium, mercury, and vinyl chloride).

Not affected

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63)

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63) standards are listed under 40 CFR 63.

Subject to subpart

Part 63 NESHAP Subpart

HH - Oil and Natural Gas Production Facilities

Prevention of Significant Deterioration (PSD)
These rules are found under WAQSR Chapter 6, Section 4.

Not Affected

Non-Attainment New Source Review
These rules are found under WAQSR Chapter 6, Section

Not Affected

| Required Public Docu | ment Attachment Type | Description |
|----------------------|----------------------|-------------|
|----------------------|----------------------|-------------|

^{**} AQD Calculated - See 'Help' for more information.

AQD EU ID: FLR001

AQD EU description:

Company EU ID: FL1

Company EU Description: Flare to control

Flare to control dehydration unit

and for

emergency/upset/ma

intenance activities

- Source Installation or Modification Schedule – Select reason(s) for this emissions unit being included in this application (must be completed regardless of date of installation or modification):

Modification

When will you begin to modify the air contaminant source? 07/20/2015

- Emission Unit Type Specific Information

Emission Unit Type: Flare

Emergency Flare Only: No

Ignition Device Type: Pilot

Smokeless Design: Yes

Btu Content (Btu/scf): 1,565.00

Assist Gas Utilized: No

Waste Gas Volume: 101,395.00

Units: scf/day

Installation Date: 01/27/2015

Continuously Monitored: Yes

Describe Continuous continuous pilots monitored through Cygnet

Monitoring:

- Potential Operating Schedule - Provide the operating schedule for this emissions unit

Hours/day: 24 Hours/year: 8760

Emissions Information "Potential to emit" means the maximum capacity of a source to emit any air pollutant under its physical and operational design. Any physical or operational limitation on the capacity of a source to emit an air pollutant, including air pollution control equipment and restrictions on hours of operation or on the type or amount of material combusted, stored or processed, shall be treated as part of its design if the limitation is enforceable by the EPA and the Division. This term does not alter or affect the use of this term for any other purposes under the Act, or the term "capacity factor" as used in Title IV of the Act or the regulations promulgated thereunder.

Basis for Determination Options:

- Manufacturer Data
- Test results for this source
- Similar source test results
- GRICalc
- Tanks Program
- AP-42
- Other. If this is selected, attach a document with a description of the method used.

Criteria Pollutants:

| Pollutant | Pre- | Efficiency Standards | Potential to | | |
|-----------|------------|----------------------|--------------|------------|--------------|
| | Controlled | | Emit (PTE) | Emit (PTE) | Determinatio |

| | Potential Emissions (tons/yr) | Potential to Emit (PTE)* | Units* | (lbs/hr)* | (tons/yr)* | n* |
|-----------------------------------------------------------------|-------------------------------------|-----------------------------|--------|-----------|------------|-------|
| Particulate emissions (PE/PM) (formerly particulate matter, PM) | 0 | 0 | | 0 | 0 | |
| PM # 10 microns in diameter (PE/PM10) | 0 | 0 | | 0 | 0 | |
| PM # 2.5 microns in diameter (PE/PM2.5) | 0 | 0 | | 0 | 0 | |
| Sulfur dioxide (SO2) | 0 | 0 | | 0 | 0 | |
| Nitrogen oxides (NOx) | 0 | 0 | | 6.27 | 27.5 | AP-42 |
| Carbon monoxide (CO) | 0 | 0 | | 1.55 | 6.8 | AP-42 |
| Volatile organic compounds (VOC) | 0 | 0 | | 0 | 0 | |
| Lead (Pb) | 0 | 0 | | 0 | 0 | |
| Total Hazardous Air Pollutants (HAPs) | 0 | 0 | | 0 | 0 | |
| Fluoride (F) | 0 | 0 | | 0 | 0 | |
| Hydrogen Sulfide (H2S) | 0 | 0 | | 0 | 0 | |
| Mercury (Hg) | 0 | 0 | | 0 | 0 | |
| Total Reduced Sulfur (TRS) | 0 | 0 | | 0 | 0 | |
| Sulfuric Acid Mist (SAM) | 0 | 0 | | 0 | 0 | |

| Pollutant | Pollutant Category | Pre- Controlled Potential | Efficiency Potential to Emit (PTE)* | Potential to Emit (PTE) (lbs/hr)* | Potential to Emit (PTE) (tons/yr)* | Basis for Determinati on* | |
|-----------|-----------------------|---------------------------------|-------------------------------------|---------------------------------------------|------------------------------------------|---------------------------------|--|
| | | Emissions (tons/yr) | Lillit (FTL) | 13.000.5 | | | |

Greenhouse Gases (GHGs):

| Pollutant | Pollutant | Pre- | Efficiency | Standards | Potential to | | |
|-----------|-----------|---------------------------------------------------|-----------------------------|-----------|-------------------------|--------------------------|--------------------|
| | Category | Controlled Potential Emissions (tons/yr) | Potential to Emit (PTE)* | Units* | Emit (PTE) (Ibs/hr)* | Emit (PTE) (tons/yr)* | Determinati on* |

^{*} Provide your calculations as an attachment and explain how all process variables and emissions factors were selected.

Note the emission factor(s) employed and document origin. Example: AP-42, Table 4.4-3 (8/97); stack test, Method 5, 4/96; mass balance based on MSDS; etc.

Best Available Control Technology (BACT)

Was a BACT Analysis completed for this unit? No

- Lowest Achievable Emission Rate (LAER)

Was a LAER Analysis completed for this unit? No

- Federal and State Rule Applicability

^{**} AQD Calculated - See 'Help' for more information.

New Source Performance Standards (NSPS)

New Source Performance Standards are listed under 40 CFR 60 - Standards of Performance for New Stationary Sources.

Not affected

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 61) National Emissions Standards for Hazardous Air Pollutants (NESHAP Part 61) are listed under 40 CFR 61. (These include asbestos, benzene, beryllium, mercury, and vinyl chloride).

Not affected

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63)

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63) standards are listed under 40 CFR 63.

Not affected

Prevention of Significant Deterioration (PSD)
These rules are found under WAQSR Chapter 6, Section 4.

Not Affected

Non-Attainment New Source Review

These rules are found under WAQSR Chapter 6, Section

Not Affected

| Required Attachment | Public Document | Attachment Type | Description |
|------------------------|-----------------|-----------------|-------------|
| Attachment | Id | Actaonment Type | Description |

AQD EU ID: FLR002

AQD EU description:

Ignition Device Type: Pilot

Smokeless Design: Yes

Units: scf/hr

Company EU ID: FL2

Company EU Description: 48" x 12' Cimarron

standard enclosed combustion device

- Source Installation or Modification Schedule – Select reason(s) for this emissions unit being included in this application (must be completed regardless of date of installation or modification):

Modification

When will you begin to modify the air contaminant source? 07/20/2015

- Emission Unit Type Specific Information

Emission Unit Type: Flare

Emergency Flare Only: No

Dt. Contact (Dt. /orf) : 0.00

Btu Content (Btu/scf): 2,308.00

Assist Gas Utilized: No

Waste Gas Volume: 191.60

Installation Date: 01/27/2015

Continuously Monitored: Yes

Describe Continuous continuous pilot flame monitored through Cygnet

Monitoring:

- Potential Operating Schedule - Provide the operating schedule for this emissions unit

Hours/day: 24 Hours/year: 8760

Emissions Information "Potential to emit" means the maximum capacity of a source to emit any air pollutant under its physical and operational design. Any physical or operational limitation on the capacity of a source to emit an air pollutant, including air pollution control equipment and restrictions on hours of operation or on the type or amount of material combusted, stored or processed, shall be treated as part of its design if the limitation is enforceable by the EPA and the Division. This term does not alter or affect the use of this term for any other purposes under the Act, or the term "capacity factor" as used in Title IV of the Act or the regulations promulgated thereunder.

Basis for Determination Options:

- Manufacturer Data
- Test results for this source
- Similar source test results
- GRICalc
- Tanks Program
- AP-42
- Other. If this is selected, attach a document with a description of the method used.

Criteria Pollutants:

| Pollutant | Pre- | Efficiency Standards | | Potential to | Potential to | Basis for |
|-----------|---------------------------------------------------|-----------------------------|--------|-------------------------|--------------------------|--------------------|
| | Controlled Potential Emissions (tons/yr) | Potential to Emit (PTE)* | Units* | Emit (PTE) (Ibs/hr)* | Emit (PTE) (tons/yr)* | Determinatio n* |

| Particulate emissions (PE/PM) (formerly particulate matter, PM) | 0 | 0 | 0 | 0 | |
|-----------------------------------------------------------------|---|---|------|-----|-------|
| PM # 10 microns in diameter (PE/PM10) | 0 | 0 | 0 | 0 | |
| PM # 2.5 microns in diameter (PE/PM2.5) | 0 | 0 | 0 | 0 | |
| Sulfur dioxide (SO2) | 0 | 0 | 0 | 0 | |
| Nitrogen oxides (NOx) | 0 | 0 | 0.07 | 0.3 | AP-42 |
| Carbon monoxide (CO) | 0 | 0 | 0.02 | 0.1 | AP-42 |
| Volatile organic compounds (VOC) | 0 | 0 | 0 | 0 | |
| Lead (Pb) | 0 | 0 | 0 | 0 | |
| Total Hazardous Air Pollutants (HAPs) | 0 | 0 | 0 | 0 | |
| Fluoride (F) | 0 | 0 | 0 | 0 | |
| Hydrogen Sulfide (H2S) | 0 | 0 | 0 | 0 | |
| Mercury (Hg) | 0 | 0 | 0 | 0 | |
| Total Reduced Sulfur (TRS) | 0 | 0 | 0 | 0 | |
| Sulfuric Acid Mist (SAM) | 0 | 0 | 0 | 0 | |

| Pollutant | . onditarit | Pre- | Efficiency | Efficiency Standards | | | |
|-----------|-------------|---------------------------------------------------|-----------------------------|----------------------|-----------|------------|--------------------|
| | Category | Controlled Potential Emissions (tons/yr) | Potential to Emit (PTE)* | | (lbs/hr)* | (tons/yr)* | Determinati on* |

Greenhouse Gases (GHGs):

| Р | ollutant | Pollutant | Pre- Efficiency St | | Standards | Potential to | | |
|---|----------|-----------|-------------------------------------|-----------------------------|-----------|--------------|--------------------------|-----|
| | | Category | Potential Emissions (tons/yr) | Potential to Emit (PTE)* | Units* | (lbs/hr)* | Emit (PTE) (tons/yr)* | on* |

^{*} Provide your calculations as an attachment and explain how all process variables and emissions factors were selected. Note the emission factor(s) employed and document origin. Example: AP-42, Table 4.4-3 (8/97); stack test, Method 5, 4/96; mass balance based on MSDS; etc.

- Best Available Control Technology (BACT)

Was a BACT Analysis completed for this unit? No

- Lowest Achievable Emission Rate (LAER)

Was a LAER Analysis completed for this unit? No

Federal and State Rule Applicability

New Source Performance Standards (NSPS)
New Source Performance Standards are listed under 40
CFR 60 - Standards of Performance for New Stationary
Sources.

Not affected

^{**} AQD Calculated - See 'Help' for more information.

National Emission Standards for Hazardous Air

Not affected

Pollutants (NESHAP Part 61)
National Emissions Standards for Hazardous Air Pollutants (NESHAP Part 61) are listed under 40 CFR 61. (These include asbestos, benzene, beryllium, mercury, and vinyl chloride).

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63)

Not affected

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63) standards are listed under 40 CFR 63.

Not Affected

Prevention of Significant Deterioration (PSD)
These rules are found under WAQSR Chapter 6, Section 4.

Not Affected

Non-Attainment New Source Review These rules are found under WAQSR Chapter 6, Section 13.

| Required Attachment | Public Document Id | Attachment Type | Description |
|------------------------|-----------------------|-----------------|-------------|
|------------------------|-----------------------|-----------------|-------------|

AQD EU ID: FLR003

AQD EU description:

Company EU ID: FL3

Company EU Description: 48" x 12' Cimarron

standard enclosed combustion device

- Source Installation or Modification Schedule – Select reason(s) for this emissions unit being included in this application (must be completed regardless of date of installation or modification):

Modification

When will you begin to modify the air contaminant source?

07/20/2015

- Emission Unit Type Specific Information

Emission Unit Type: Flare

Emergency Flare Only: No Ignition Device Type: Pilot
Btu Content (Btu/scf): 1,565.00 Smokeless Design: Yes

Assist Gas Utilized: No

Waste Gas Volume: 504.00 Units: scf/day

Installation Date: 07/20/2015

Continuously Monitored: Yes

Describe Continuous continuous pilot flame monitored through Cygnet

Monitoring:

- Potential Operating Schedule - Provide the operating schedule for this emissions unit

Hours/day: 24 Hours/year: 8760

- Emissions Information "Potential to emit" means the maximum capacity of a source to emit any air pollutant under its physical and operational design. Any physical or operational limitation on the capacity of a source to emit an air pollutant, including air pollution control equipment and restrictions on hours of operation or on the type or amount of material combusted, stored or processed, shall be treated as part of its design if the limitation is enforceable by the EPA and the Division. This term does not alter or affect the use of this term for any other purposes under the Act, or the term "capacity factor" as used in Title IV of the Act or the regulations promulgated thereunder.

Basis for Determination Options:

- Manufacturer Data
- Test results for this source
- Similar source test results
- GRICalc
- Tanks Program
- AP-42
- Other. If this is selected, attach a document with a description of the method used.

Criteria Pollutants:

| Potential Potential to Units* (lbs/hr)* (tons/yr)* n* | Pollutant | Pre- | Efficiency | Standards | Potential to | Potential to | Basis for |
|-------------------------------------------------------|-----------|-----------|------------|-----------|-------------------------|--------------------------|--------------------|
| (tons/yr) | | Emissions | | Units* | Emit (PTE) (Ibs/hr)* | Emit (PTE) (tons/yr)* | Determinatio n* |

| Particulate emissions (PE/PM) (formerly particulate matter, PM) | 0 | 0 | 0 | 0 | |
|-----------------------------------------------------------------|---|---|-------|------|-------|
| PM # 10 microns in diameter (PE/PM10) | 0 | 0 | 0 | 0 | |
| PM # 2.5 microns in diameter (PE/PM2.5) | 0 | 0 | 0 | 0 | |
| Sulfur dioxide (SO2) | 0 | 0 | 0 | 0 | |
| Nitrogen oxides (NOx) | 0 | 0 | 0.005 | 0.02 | AP-42 |
| Carbon monoxide (CO) | 0 | 0 | 0.002 | 0.01 | AP-42 |
| Volatile organic compounds (VOC) | 0 | 0 | 0 | 0 | |
| Lead (Pb) | 0 | 0 | 0 | 0 | |
| Total Hazardous Air Pollutants (HAPs) | 0 | 0 | 0 | 0 | |
| Fluoride (F) | 0 | 0 | 0 | 0 | |
| Hydrogen Sulfide (H2S) | 0 | 0 | 0 | 0 | |
| Mercury (Hg) | 0 | 0 | 0 | 0 | |
| Total Reduced Sulfur (TRS) | 0 | 0 | 0 | 0 | |
| Sulfuric Acid Mist (SAM) | 0 | 0 | 0 | 0 | |

| Pollutant | Pollutant | Pre- | Efficiency | Standards | Potential to | | |
|-----------|-----------|---------------------------------------------------|-----------------------------|-----------|-------------------------|--------------------------|--------------------|
| | Category | Controlled Potential Emissions (tons/yr) | Potential to Emit (PTE)* | Units* | Emit (PTE) (lbs/hr)* | Emit (PTE) (tons/yr)* | Determinati on* |

Greenhouse Gases (GHGs):

| | Pollutant | Pollutant Category | Pre- Controlled Potential Emissions (tons/yr) | Efficiency Potential to Emit (PTE)* | | Potential to Emit (PTE) (lbs/hr)* | Potential to Emit (PTE) (tons/yr)* | Basis for Determinati on* | |
|--|-----------|-----------------------|-----------------------------------------------------------|-------------------------------------------|--|-----------------------------------------|------------------------------------------|---------------------------------|--|
|--|-----------|-----------------------|-----------------------------------------------------------|-------------------------------------------|--|-----------------------------------------|------------------------------------------|---------------------------------|--|

^{*} Provide your calculations as an attachment and explain how all process variables and emissions factors were selected. Note the emission factor(s) employed and document origin. Example: AP-42, Table 4.4-3 (8/97); stack test, Method 5, 4/96; mass balance based on MSDS; etc.

- Best Available Control Technology (BACT)

Was a BACT Analysis completed for this unit? No

- Lowest Achievable Emission Rate (LAER)

Was a LAER Analysis completed for this unit? No

Federal and State Rule Applicability

New Source Performance Standards (NSPS)
New Source Performance Standards are listed under 40
CFR 60 - Standards of Performance for New Stationary
Sources.

Not affected

^{**} AQD Calculated - See 'Help' for more information.

National Emission Standards for Hazardous Air

Pollutants (NESHAP Part 61)
National Emissions Standards for Hazardous Air Pollutants
(NESHAP Part 61) are listed under 40 CFR 61. (These include asbestos, benzene, beryllium, mercury, and vinyl chloride).

Not affected

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63)

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63) standards are listed under 40 CFR 63. Not affected

Prevention of Significant Deterioration (PSD)
These rules are found under WAQSR Chapter 6, Section 4.

Not Affected

Non-Attainment New Source Review

These rules are found under WAQSR Chapter 6, Section 13.

Not Affected

| | T | | |
|------------|-----------------|-----------------|-------------|
| Required | Public Document | Attachment Type | Description |
| Attachment | ld | | |

AQD EU ID: FUG001

AQD EU description:

Company EU ID: FUG1

Company EU Description: process fugitives

Source Installation or Modification Schedule - Select reason(s) for this emissions unit being included in this application (must be completed regardless of date of installation or modification):

Modification

When will you begin to modify the air contaminant source? 07/20/2015

Emission Unit Type Specific Information

Emission Unit Type: Fugitive

Type of Fugitive Emission: Fugitive Leaks at O&G

| Equipment and Service Type | Number of Each Equipment Type | Leak Rate (ppm) | Percent VOC |
|-------------------------------|----------------------------------|-----------------|-------------|
| Connector; Gas | 50 | 10,000.00 | 46.300 |
| Flange; Gas | 250 | 10,000.00 | 46.300 |
| Open Ended Line; Gas | 5 | 10,000.00 | 46.300 |
| Other; Gas | 10 | 10,000.00 | 46.300 |
| Valve; Gas | 20 | 10,000.00 | 46.300 |
| Connector; Light Oil | 50 | 10,000.00 | 73.200 |
| Flange; Light Oil | 250 | 10,000.00 | 73.200 |
| Open Ended Line; Light Oil | 5 | 10,000.00 | 73.200 |
| Other; Light Oil | 10 | 10,000.00 | 73.200 |
| Valve; Light Oil | 10 | 10,000.00 | 73.200 |
| Flange; Water/Light Oil | 250 | 10,000.00 | 73.200 |
| Other; Water/Light Oil | 10 | 10,000.00 | 73.200 |
| Valve; Water/Light Oil | 10 | 10,000.00 | 73.200 |

Potential Operating Schedule - Provide the operating schedule for this emissions unit

Hours/day:

Hours/year:

Emissions Information "Potential to emit" means the maximum capacity of a source to emit any air pollutant under its physical and operational design. Any physical or operational limitation on the capacity of a source to emit an air pollutant, including air pollution control equipment and restrictions on hours of operation or on the type or amount of material combusted, stored or processed, shall be treated as part of its design if the limitation is enforceable by the EPA and the Division. This term does not alter or affect the use of this term for any other purposes under the Act, or the term "capacity factor" as used in Title IV of the Act or the regulations promulgated thereunder.

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Basis for Determination Options:

- Manufacturer Data
- Test results for this source

- Similar source test results
- GRICalc
- Tanks Program
- AP-42
- Other. If this is selected, attach a document with a description of the method used.

Criteria Pollutants:

| Pollutant | Pre- | Efficiency | Standards | Potential to | Potential to | Basis for |
|-----------------------------------------------------------------|---------------------------------------------------|-----------------------------|-----------|-------------------------|--------------------------|--------------------|
| | Controlled Potential Emissions (tons/yr) | Potential to Emit (PTE)* | Units* | Emit (PTE) (lbs/hr)* | Emit (PTE) (tons/yr)* | Determinatio n* |
| Particulate emissions (PE/PM) (formerly particulate matter, PM) | 0 | 0 | | 0 | 0 | |
| PM # 10 microns in diameter (PE/PM10) | 0 | 0 | | 0 | 0 | |
| PM # 2.5 microns in diameter (PE/PM2.5) | 0 | 0 | | 0 | 0 | |
| Sulfur dioxide (SO2) | 0 | 0 | | 0 | 0 | |
| Nitrogen oxides (NOx) | 0 | 0 | | 0 | 0 | |
| Carbon monoxide (CO) | 0 | 0 | | 0 | 0 | |
| Volatile organic compounds (VOC) | 3 | 0 | | 0 | 0 | AP-42 |
| Lead (Pb) | 0 | 0 | | 0 | 0 | |
| Total Hazardous Air Pollutants (HAPs) | 0.1 | 0 | | 0 | 0 | AP-42 |
| Fluoride (F) | 0 | 0 | | 0 | 0 | |
| Hydrogen Sulfide (H2S) | 0 | 0 | | 0 | 0 | |
| Mercury (Hg) | 0 | 0 | | 0 | 0 | |
| Total Reduced Sulfur (TRS) | 0 | 0 | | 0 | 0 | |
| Sulfuric Acid Mist (SAM) | 0 | 0 | | 0 | 0 | |

Hazardous Air Pollutants (HAPs) and Toxic Air Contaminants:

| Pollutant | Pollutant Category | Pre- Controlled Potential Emissions (tons/yr) | , | Units* | Potential to Emit (PTE) (lbs/hr)* | Potential to Emit (PTE) (tons/yr)* | |
|-----------|-----------------------|-----------------------------------------------------------|---|--------|-----------------------------------------|------------------------------------------|--|
|-----------|-----------------------|-----------------------------------------------------------|---|--------|-----------------------------------------|------------------------------------------|--|

Greenhouse Gases (GHGs):

| Pollutant | Pollutant Category | Pre- Controlled Potential | Efficiency Potential to Emit (PTE)* | Units* | Potential to Emit (PTE) (tons/yr)* | |
|-----------|-----------------------|---------------------------------|-------------------------------------------|--------|------------------------------------------|--|
| | | Emissions (tons/yr) | Emit (PTE) | | | |

^{*} Provide your calculations as an attachment and explain how all process variables and emissions factors were selected. Note the emission factor(s) employed and document origin. Example: AP-42, Table 4.4-3 (8/97); stack test, Method 5, 4/96; mass balance based on MSDS; etc.

^{**} AQD Calculated - See 'Help' for more information.

- Best Available Control Technology (BACT)

Was a BACT Analysis completed for this unit? No

Lowest Achievable Emission Rate (LAER)

Was a LAER Analysis completed for this unit? No

Federal and State Rule Applicability

New Source Performance Standards (NSPS)
New Source Performance Standards are listed under 40
CFR 60 - Standards of Performance for New Stationary
Sources.

Not affected

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 61)

National Emissions Standards for Hazardous Air Pollutants (NESHAP Part 61) are listed under 40 CFR 61. (These include asbestos, benzene, beryllium, mercury, and vinyl chloride).

Not affected

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63)

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63) standards are listed under 40 CFR 63.

Not affected

Prevention of Significant Deterioration (PSD)

These rules are found under WAQSR Chapter 6, Section 4.

Not Affected

Non-Attainment New Source Review
These rules are found under WAQSR Chapter 6, Section

Not Affected

| Required Public Document Attachment Type Description Attachment Id | | | Attachment Type | Description |
|--------------------------------------------------------------------|--|--|-----------------|-------------|
|--------------------------------------------------------------------|--|--|-----------------|-------------|

AQD EU ID: HET001

AQD EU description:

Company EU ID: HET1

Company EU Description: tank heater

- Source Installation or Modification Schedule – Select reason(s) for this emissions unit being included in this application (must be completed regardless of date of installation or modification):

Modification

When will you begin to modify the air contaminant source? 07/20/2015

Emission Unit Type Specific Information

Emission Unit Type: Heater/Chiller

Fuel Sulfur Content: 0.00 Units: ppm

- Potential Operating Schedule - Provide the operating schedule for this emissions unit

Hours/day: 24 Hours/year: 8760

- Emissions Information "Potential to emit" means the maximum capacity of a source to emit any air pollutant under its physical and operational design. Any physical or operational limitation on the capacity of a source to emit an air pollutant, including air pollution control equipment and restrictions on hours of operation or on the type or amount of material combusted, stored or processed, shall be treated as part of its design if the limitation is enforceable by the EPA and the Division. This term does not alter or affect the use of this term for any other purposes under the Act, or the term "capacity factor" as used in Title IV of the Act or the regulations promulgated thereunder.
 - Basis for Determination Options:
 - Manufacturer Data
 - Test results for this source
 - Similar source test results
 - GRICalc
 - Tanks Program
 - AP-42
 - Other. If this is selected, attach a document with a description of the method used.

Criteria Pollutants :

| Pollutant | Pre- | Efficiency | Standards | Potential to | Potential to | Basis for |
|-----------------------------------------------------------------|---------------------------------------------------|-----------------------------|-----------|-------------------------|--------------------------|--------------------|
| | Controlled Potential Emissions (tons/yr) | Potential to Emit (PTE)* | Units* | Emit (PTE) (lbs/hr)* | Emit (PTE) (tons/yr)* | Determinatio n* |
| Particulate emissions (PE/PM) (formerly particulate matter, PM) | 0 | 0 | | 0 | 0 | |
| PM # 10 microns in diameter (PE/PM10) | 0 | 0 | | 0 | 0 | |
| PM # 2.5 microns in diameter (PE/PM2.5) | 0 | 0 | | 0 | 0 | |
| Sulfur dioxide (SO2) | 0 | 0 | | 0 | 0 | |
| Nitrogen oxides (NOx) | 0 | 0 | | 0.075 | 0.33 | AP-42 |

| Carbon monoxide (CO) | 0 | 0 | 0. | . 063 | 0.28 | AP-42 |
|------------------------------------------|---|---|----|-------|------|-------|
| Volatile organic compounds (VOC) | 0 | 0 | 0 | | 0 | |
| Lead (Pb) | 0 | 0 | 0 | | 0 | |
| Total Hazardous Air Pollutants (HAPs) | 0 | 0 | 0 | | 0 | |
| Fluoride (F) | 0 | 0 | 0 | | 0 | |
| Hydrogen Sulfide (H2S) | 0 | 0 | 0 | | 0 | |
| Mercury (Hg) | 0 | 0 | 0 | | 0 | |
| Total Reduced Sulfur (TRS) | 0 | 0 | 0 | | 0 | |
| Sulfuric Acid Mist (SAM) | 0 | 0 | 0 | | 0 | |

| Pollutant | Pollutant | | Efficiency | Standards | Potential to | | |
|-----------|-----------|---------------------------------------------------|-----------------------------|-----------|--------------|------------|--------------------|
| , | Category | Controlled Potential Emissions (tons/yr) | Potential to Emit (PTE)* | Units* | (lbs/hr)* | (tons/yr)* | Determinati on* |

Greenhouse Gases (GHGs):

| Pollutant | Pollutant Category | Pre- Controlled Potential Emissions | Efficiency Potential to Emit (PTE)* | | Potential to Emit (PTE) (tons/yr)* | |
|-----------|-----------------------|----------------------------------------------|-------------------------------------------|--|------------------------------------------|--|
| | | (tons/yr) | | | | |

^{*} Provide your calculations as an attachment and explain how all process variables and emissions factors were selected. Note the emission factor(s) employed and document origin. Example: AP-42, Table 4.4-3 (8/97); stack test, Method 5, 4/96; mass balance based on MSDS; etc.

Best Available Control Technology (BACT)

Was a BACT Analysis completed for this unit? No

Lowest Achievable Emission Rate (LAER)

Was a LAER Analysis completed for this unit? No

- Federal and State Rule Applicability

Sources.

New Source Performance Standards (NSPS)
New Source Performance Standards are listed under 40
CFR 60 - Standards of Performance for New Stationary

Not affected

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 61)

Not affected

National Emissions Standards for Hazardous Air Pollutants (NESHAP Part 61) are listed under 40 CFR 61. (These include asbestos, benzene, beryllium, mercury, and vinyl chloride).

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63)

Not affected

National Emission Standards for Hazardous Air Pollutants

^{**} AQD Calculated - See 'Help' for more information.

(NESHAP Part 63) standards are listed under 40 CFR 63.

Prevention of Significant Deterioration (PSD)
These rules are found under WAQSR Chapter 6, Section 4.

Not Affected

Not Affected

Non-Attainment New Source Review

These rules are found under WAQSR Chapter 6, Section 13.

| Required Attachment | Public Document Id | Attachment Type | Description |
|------------------------|-----------------------|-----------------|-------------|
|------------------------|-----------------------|-----------------|-------------|

AQD EU ID: HET002

AQD EU description:

Company EU ID: HET2

Company EU Description: tank heater

- Source Installation or Modification Schedule – Select reason(s) for this emissions unit being included in this application (must be completed regardless of date of installation or modification):

Modification

When will you begin to modify the air contaminant source? 07/20/2015

Emission Unit Type Specific Information

Emission Unit Type: Heater/Chiller

Fuel Sulfur Content: 0.00 Units: ppm

- Potential Operating Schedule - Provide the operating schedule for this emissions unit

Hours/day: 24 Hours/year: 8760

- Emissions Information "Potential to emit" means the maximum capacity of a source to emit any air pollutant under its physical and operational design. Any physical or operational limitation on the capacity of a source to emit an air pollutant, including air pollution control equipment and restrictions on hours of operation or on the type or amount of material combusted, stored or processed, shall be treated as part of its design if the limitation is enforceable by the EPA and the Division. This term does not alter or affect the use of this term for any other purposes under the Act, or the term "capacity factor" as used in Title IV of the Act or the regulations promulgated thereunder.

Basis for Determination Options:

- Manufacturer Data
- Test results for this source
- Similar source test results
- GRICalc
- Tanks Program
- AP-42
- Other. If this is selected, attach a document with a description of the method used.

Criteria Pollutants:

| Pollutant | Pre- | Efficiency | Standards | Potential to | Potential to | Basis for | |
|-----------------------------------------------------------------|---------------------------------------------------|-----------------------------|-----------|-------------------------|--------------------------|--------------------|--|
| | Controlled Potential Emissions (tons/yr) | Potential to Emit (PTE)* | Units* | Emit (PTE) (Ibs/hr)* | Emit (PTE) (tons/yr)* | Determinatio n* | |
| Particulate emissions (PE/PM) (formerly particulate matter, PM) | 0 | 0 | | 0 | 0 | | |
| PM # 10 microns in diameter (PE/PM10) | 0 | 0 | | 0 | 0 | | |
| PM # 2.5 microns in diameter (PE/PM2.5) | 0 | 0 | | 0 | 0 | | |
| Sulfur dioxide (SO2) | 0 | 0 | | 0 | 0 | | |
| Nitrogen oxides (NOx) | 0 | 0 | | 0.075 | 0.33 | AP-42 | |

| Carbon monoxide (CO) | 0 | 0 | 0.063 | 0.28 | AP-42 |
|------------------------------------------|---|---|-------|------|-------|
| Volatile organic compounds (VOC) | 0 | 0 | 0 | 0 | |
| Lead (Pb) | 0 | 0 | 0 | 0 | |
| Total Hazardous Air Pollutants (HAPs) | 0 | 0 | 0 | 0 | |
| Fluoride (F) | 0 | 0 | 0 | 0 | |
| Hydrogen Sulfide (H2S) | 0 | 0 | 0 | 0 | |
| Mercury (Hg) | 0 | 0 | 0 | 0 | |
| Total Reduced Sulfur (TRS) | 0 | 0 | 0 | 0 | |
| Sulfuric Acid Mist (SAM) | 0 | 0 | 0 | 0 | |

| Pollutant | Pollutant | Pre- | Efficiency Standards | | | Potential to | |
|-----------|-----------|-------------------------------------|-----------------------------|--|-------------------------|--------------------------|--------------------|
| | Category | Potential Emissions (tons/yr) | Potential to Emit (PTE)* | | Emit (PTE) (Ibs/hr)* | Emit (PTE) (tons/yr)* | Determinati on* |

Greenhouse Gases (GHGs):

| Pollutant | Pollutant Pre- | | Efficiency | Standards | | Potential to | |
|-----------|----------------|---------------------------------------------------|-----------------------------|-----------|-------------------------|--------------------------|--------------------|
| | Category | Controlled Potential Emissions (tons/yr) | Potential to Emit (PTE)* | Units* | Emit (PTE) (Ibs/hr)* | Emit (PTE) (tons/yr)* | Determinati on* |

^{*} Provide your calculations as an attachment and explain how all process variables and emissions factors were selected. Note the emission factor(s) employed and document origin. Example: AP-42, Table 4.4-3 (8/97); stack test, Method 5, 4/96; mass balance based on MSDS; etc.

Best Available Control Technology (BACT)

Was a BACT Analysis completed for this unit? No

Lowest Achievable Emission Rate (LAER)

Was a LAER Analysis completed for this unit? No

Federal and State Rule Applicability

Sources.

New Source Performance Standards (NSPS) New Source Performance Standards are listed under 40 CFR 60 - Standards of Performance for New Stationary Not affected

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 61)

National Emissions Standards for Hazardous Air Pollutants (NESHAP Part 61) are listed under 40 CFR 61. (These include asbestos, benzene, beryllium, mercury, and vinyl chloride).

Not affected

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63)

Not affected

National Emission Standards for Hazardous Air Pollutants

^{**} AQD Calculated - See 'Help' for more information.

(NESHAP Part 63) standards are listed under 40 CFR 63.

Prevention of Significant Deterioration (PSD)
These rules are found under WAQSR Chapter 6, Section 4.

Not Affected

Not Affected

Non-Attainment New Source Review These rules are found under WAQSR Chapter 6, Section 13.

| Required F Attachment | Public Document Id | Attachment Type | Description |
|--------------------------|--------------------|-----------------|-------------|
|--------------------------|--------------------|-----------------|-------------|

AQD EU ID: HET003

AQD EU description:

Company EU ID: HET3

Company EU Description: tank heater

- Source Installation or Modification Schedule – Select reason(s) for this emissions unit being included in this application (must be completed regardless of date of installation or modification):

Modification

When will you begin to modify the air contaminant source? 07/20/2015

- Emission Unit Type Specific Information

Emission Unit Type: Heater/Chiller

Fuel Sulfur Content: 0.00 Units: ppm

- Potential Operating Schedule - Provide the operating schedule for this emissions unit

Hours/day: 24 Hours/year: 8760

- Emissions Information "Potential to emit" means the maximum capacity of a source to emit any air pollutant under its physical and operational design. Any physical or operational limitation on the capacity of a source to emit an air pollutant, including air pollution control equipment and restrictions on hours of operation or on the type or amount of material combusted, stored or processed, shall be treated as part of its design if the limitation is enforceable by the EPA and the Division. This term does not alter or affect the use of this term for any other purposes under the Act, or the term "capacity factor" as used in Title IV of the Act or the regulations promulgated thereunder.

Basis for Determination Options:

- Manufacturer Data
- Test results for this source
- Similar source test results
- GRICalc
- Tanks Program
- AP-42
- Other. If this is selected, attach a document with a description of the method used.

Criteria Pollutants :

| Pollutant | Pre- | Efficiency | Standards | Potential to | Potential to | Basis for |
|-----------------------------------------------------------------|---------------------------------------------------|-----------------------------|-----------|-------------------------|--------------------------|--------------------|
| | Controlled Potential Emissions (tons/yr) | Potential to Emit (PTE)* | Units* | Emit (PTE) (Ibs/hr)* | Emit (PTE) (tons/yr)* | Determinatio n* |
| Particulate emissions (PE/PM) (formerly particulate matter, PM) | 0 | 0 | | 0 | 0 | |
| PM # 10 microns in diameter (PE/PM10) | 0 | 0 | | 0 | 0 | |
| PM # 2.5 microns in diameter (PE/PM2.5) | 0 | 0 | | 0 | 0 | |
| Sulfur dioxide (SO2) | 0 | 0 | | 0 | 0 | |
| Nitrogen oxides (NOx) | 0 | 0 | | 0.075 | 0.33 | AP-42 |

| | 1 | | | | |
|------------------------------------------|---|---|-------|------|-------|
| Carbon monoxide (CO) | 0 | 0 | 0.063 | 0.28 | AP-42 |
| Volatile organic compounds (VOC) | 0 | 0 | 0 | 0 | |
| Lead (Pb) | 0 | 0 | 0 | 0 | |
| Total Hazardous Air Pollutants (HAPs) | 0 | 0 | 0 | 0 | |
| Fluoride (F) | 0 | 0 | 0 | 0 | |
| Hydrogen Sulfide (H2S) | 0 | 0 | 0 | 0 | |
| Mercury (Hg) | 0 | 0 | 0 | 0 | |
| Total Reduced Sulfur (TRS) | 0 | 0 | 0 | 0 | |
| Sulfuric Acid Mist (SAM) | 0 | 0 | 0 | 0 | |

| Pollutant | Pollutant | Pre- | Efficiency | Standards | | Potential to | |
|-----------|-----------|---------------------------------------------------|-----------------------------|-----------|-----------|--------------|--------------------|
| | Category | Controlled Potential Emissions (tons/yr) | Potential to Emit (PTE)* | Units* | (lbs/hr)* | (tons/yr)* | Determinati on* |

Greenhouse Gases (GHGs):

| Pollutant | Pollutant | Pre- | Efficiency S | Standards | | Potential to | |
|-----------|-----------|---------------------------------------------------|-----------------------------|-----------|-------------------------|--------------------------|--------------------|
| | Category | Controlled Potential Emissions (tons/yr) | Potential to Emit (PTE)* | Units* | Emit (PTE) (Ibs/hr)* | Emit (PTE) (tons/yr)* | Determinati on* |

^{*} Provide your calculations as an attachment and explain how all process variables and emissions factors were selected. Note the emission factor(s) employed and document origin. Example: AP-42, Table 4.4-3 (8/97); stack test, Method 5, 4/96; mass balance based on MSDS; etc.

Best Available Control Technology (BACT)

Was a BACT Analysis completed for this unit? No

Lowest Achievable Emission Rate (LAER)

Was a LAER Analysis completed for this unit? No

Federal and State Rule Applicability

New Source Performance Standards (NSPS)

New Source Performance Standards are listed under 40 CFR 60 - Standards of Performance for New Stationary

Not affected

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 61)

National Emissions Standards for Hazardous Air Pollutants (NESHAP Part 61) are listed under 40 CFR 61. (These include asbestos, benzene, beryllium, mercury, and vinyl chloride).

Not affected

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63)

National Emission Standards for Hazardous Air Pollutants

Not affected

^{**} AQD Calculated - See 'Help' for more information.

(NESHAP Part 63) standards are listed under 40 CFR 63.

Prevention of Significant Deterioration (PSD)
These rules are found under WAQSR Chapter 6, Section 4.

Not Affected

Non-Attainment New Source Review
These rules are found under WAQSR Chapter 6, Section 13.

Not Affected

| Required Public Document Id | Attachment Type | Description |
|-----------------------------|-----------------|-------------|
|-----------------------------|-----------------|-------------|

AQD EU ID: HET004

AQD EU description:

Company EU ID: HET4

Company EU Description: line heater

- Source Installation or Modification Schedule – Select reason(s) for this emissions unit being included in this application (must be completed regardless of date of installation or modification):

Modification

When will you begin to modify the air contaminant source? 07/20/2015

- Emission Unit Type Specific Information

Emission Unit Type: Heater/Chiller

Fuel Sulfur Content: 0.00 Units: ppm

- Potential Operating Schedule - Provide the operating schedule for this emissions unit

Hours/day: 24 Hours/year: 8760

Emissions Information "Potential to emit" means the maximum capacity of a source to emit any air pollutant under its physical and operational design. Any physical or operational limitation on the capacity of a source to emit an air pollutant, including air pollution control equipment and restrictions on hours of operation or on the type or amount of material combusted, stored or processed, shall be treated as part of its design if the limitation is enforceable by the EPA and the Division. This term does not alter or affect the use of this term for any other purposes under the Act, or the term "capacity factor" as used in Title IV of the Act or the regulations promulgated thereunder.

Basis for Determination Options:

- Manufacturer Data
- Test results for this source
- Similar source test results
- GRICalc
- Tanks Program
- AP-42
- Other. If this is selected, attach a document with a description of the method used.

Criteria Pollutants:

| Pollutant | Pre- | Efficiency | Standards | Potential to | Potential to | Basis for |
|-----------------------------------------------------------------|---------------------------------------------------|-----------------------------|-----------|-------------------------|--------------------------|--------------------|
| | Controlled Potential Emissions (tons/yr) | Potential to Emit (PTE)* | Units* | Emit (PTE) (lbs/hr)* | Emit (PTE) (tons/yr)* | Determinatio n* |
| Particulate emissions (PE/PM) (formerly particulate matter, PM) | 0 | 0 | | 0 | 0 | |
| PM # 10 microns in diameter (PE/PM10) | 0 | 0 | | 0 | 0 | |
| PM # 2.5 microns in diameter (PE/PM2.5) | 0 | 0 | | 0 | 0 | |
| Sulfur dioxide (SO2) | 0 | 0 | | 0 | 0 | |
| Nitrogen oxides (NOx) | 0 | 0 | | 0.038 | 0.17 | AP-42 |

| Carbon monoxide (CO) | 0 | 0 | 0.032 | 0.14 | AP-42 |
|------------------------------------------|---|---|-------|------|-------|
| Volatile organic compounds (VOC) | 0 | 0 | 0 | 0 | |
| Lead (Pb) | 0 | 0 | 0 | 0 | |
| Total Hazardous Air Pollutants (HAPs) | 0 | 0 | 0 | 0 | |
| Fluoride (F) | 0 | 0 | 0 | 0 | |
| Hydrogen Sulfide (H2S) | 0 | 0 | 0 | 0 | |
| Mercury (Hg) | 0 | 0 | 0 | 0 | |
| Total Reduced Sulfur (TRS) | 0 | 0 | 0 | 0 | |
| Sulfuric Acid Mist (SAM) | 0 | 0 | 0 | 0 | |

| Pollutant | Pollutant | Pre- | Efficiency | Standards | | Potential to | |
|-----------|-----------|-------------------------------------|-----------------------------|-----------|-------------------------|--------------------------|--------------------|
| | Category | Potential Emissions (tons/yr) | Potential to Emit (PTE)* | | Emit (PTE) (Ibs/hr)* | Emit (PTE) (tons/yr)* | Determinati on* |

Greenhouse Gases (GHGs):

| Pollutant | Pollutant | Pre- | Efficiency | Standards | | Potential to | |
|-----------|-----------|---------------------------------------------------|-----------------------------|-----------|-----------|--------------|--------------------|
| | Category | Controlled Potential Emissions (tons/yr) | Potential to Emit (PTE)* | Units* | (lbs/hr)* | (tons/yr)* | Determinati on* |

^{*} Provide your calculations as an attachment and explain how all process variables and emissions factors were selected. Note the emission factor(s) employed and document origin. Example: AP-42, Table 4.4-3 (8/97); stack test, Method 5, 4/96; mass balance based on MSDS; etc.

Best Available Control Technology (BACT)

Was a BACT Analysis completed for this unit? No

Lowest Achievable Emission Rate (LAER)

Was a LAER Analysis completed for this unit? No

Federal and State Rule Applicability

New Source Performance Standards (NSPS)

New Source Performance Standards are listed under 40 CFR 60 - Standards of Performance for New Stationary Sources.

Not affected

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 61)

National Emissions Standards for Hazardous Air Pollutants (NESHAP Part 61) are listed under 40 CFR 61. (These include asbestos, benzene, beryllium, mercury, and vinyl chloride).

Not affected

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63)

National Emission Standards for Hazardous Air Pollutants

Not affected

^{**} AQD Calculated - See 'Help' for more information.

(NESHAP Part 63) standards are listed under 40 CFR 63.

Prevention of Significant Deterioration (PSD)
These rules are found under WAQSR Chapter 6, Section 4.

Not Affected

Non-Attainment New Source Review
These rules are found under WAQSR Chapter 6, Section 13.

Not Affected

| Required Attachment | Public Document Id | Attachment Type | Description |
|------------------------|-----------------------|-----------------|-------------|
| 711140111110111 | 10 | | |

AQD EU ID: HET005

AQD EU description:

Company EU ID: HET5

Company EU Description: reboiler heater

- Source Installation or Modification Schedule – Select reason(s) for this emissions unit being included in this application (must be completed regardless of date of installation or modification):

Modification

When will you begin to modify the air contaminant source? 07/20/2015

Emission Unit Type Specific Information

Emission Unit Type: Heater/Chiller

Fuel Sulfur Content: 0.00 Units: ppm

- Potential Operating Schedule - Provide the operating schedule for this emissions unit

Hours/day: 24 Hours/year: 8760

- Emissions Information "Potential to emit" means the maximum capacity of a source to emit any air pollutant under its physical and operational design. Any physical or operational limitation on the capacity of a source to emit an air pollutant, including air pollution control equipment and restrictions on hours of operation or on the type or amount of material combusted, stored or processed, shall be treated as part of its design if the limitation is enforceable by the EPA and the Division. This term does not alter or affect the use of this term for any other purposes under the Act, or the term "capacity factor" as used in Title IV of the Act or the regulations promulgated thereunder.

Basis for Determination Options:

- Manufacturer Data
- Test results for this source
- Similar source test results
- GRICalc
- Tanks Program
- AP-42
- Other. If this is selected, attach a document with a description of the method used.

| Pollutant | Pre- | Efficiency | Standards | Potential to | Potential to | Basis for |
|-----------------------------------------------------------------|---------------------------------------------------|-----------------------------|-----------|-------------------------|--------------------------|--------------------|
| | Controlled Potential Emissions (tons/yr) | Potential to Emit (PTE)* | Units* | Emit (PTE) (Ibs/hr)* | Emit (PTE) (tons/yr)* | Determinatio n* |
| Particulate emissions (PE/PM) (formerly particulate matter, PM) | 0 | 0 | | 0 | 0 | |
| PM # 10 microns in diameter (PE/PM10) | 0 | 0 | | 0 | 0 | |
| PM # 2.5 microns in diameter (PE/PM2.5) | 0 | 0 | | 0 | 0 | |
| Sulfur dioxide (SO2) | 0 | 0 | | 0 | 0 | |
| Nitrogen oxides (NOx) | 0 | 0 | | 0.09 | 0.4 | AP-42 |

| Carbon monoxide (CO) | 0 | 0 | 0.076 | 0.33 | AP-42 |
|------------------------------------------|---|---|-------|------|-------|
| Volatile organic compounds (VOC) | 0 | 0 | 0 | 0 | |
| Lead (Pb) | 0 | 0 | 0 | 0 | |
| Total Hazardous Air Pollutants (HAPs) | 0 | 0 | 0 | 0 | |
| Fluoride (F) | 0 | 0 | 0 | 0 | |
| Hydrogen Sulfide (H2S) | 0 | 0 | 0 | 0 | |
| Mercury (Hg) | 0 | 0 | 0 | 0 | |
| Total Reduced Sulfur (TRS) | 0 | 0 | 0 | 0 | |
| Sulfuric Acid Mist (SAM) | 0 | 0 | 0 | 0 | |

| Pollut | | | | Standards | | Potential to | |
|--------|-------|--------------------------------------------------------|--------------|-----------|-----------|--------------------------|--------------------|
| | Cateo | gory Controlled Potential Emissions (tons/yr) | Potential to | | (lbs/hr)* | Emit (PTE) (tons/yr)* | Determinati on* |

Greenhouse Gases (GHGs):

| Pollutant | Pollutant | Pre- | Efficiency | Standards | | Potential to | |
|-----------|-----------|---------------------------------------------------|-----------------------------|-----------|-------------------------|--------------------------|--------------------|
| | Category | Controlled Potential Emissions (tons/yr) | Potential to Emit (PTE)* | Units* | Emit (PTE) (Ibs/hr)* | emit (PTE) (tons/yr)* | Determinati on* |

^{*} Provide your calculations as an attachment and explain how all process variables and emissions factors were selected.

Note the emission factor(s) employed and document origin. Example: AP-42, Table 4.4-3 (8/97); stack test, Method 5, 4/96; mass balance based on MSDS; etc.

Best Available Control Technology (BACT)

Was a BACT Analysis completed for this unit? No

Lowest Achievable Emission Rate (LAER)

Was a LAER Analysis completed for this unit? No

- Federal and State Rule Applicability

New Source Performance Standards (NSPS)
New Source Performance Standards are listed under 40
CFR 60 - Standards of Performance for New Stationary

Sources.

Not affected

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 61)

National Emissions Standards for Hazardous Air Pollutants (NESHAP Part 61) are listed under 40 CFR 61. (These include asbestos, benzene, beryllium, mercury, and vinyl chloride).

Not affected

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63)

National Emission Standards for Hazardous Air Pollutants

Not affected

^{**} AQD Calculated - See 'Help' for more information.

(NESHAP Part 63) standards are listed under 40 CFR 63.

Prevention of Significant Deterioration (PSD)
These rules are found under WAQSR Chapter 6, Section 4.

Not Affected

Non-Attainment New Source Review
These rules are found under WAQSR Chapter 6, Section 13.

Not Affected

| Required Public Document Attachment Type Attachment | Description |
|-----------------------------------------------------|-------------|
|-----------------------------------------------------|-------------|

AQD EU ID: LUD001

AQD EU description:

Company EU ID: TLO1

Company EU Description: truck loading from

condensate tanks

- Source Installation or Modification Schedule – Select reason(s) for this emissions unit being included in this application (must be completed regardless of date of installation or modification):

Modification

When will you begin to modify the air contaminant source? 07/20/2015

- Emission Unit Type Specific Information

Emission Unit Type: Loading/Unloading/Dump

Maximum Hourly Throughput 3

Units: barrels/hr

Detailed Description of condensate tank truck loadout (60 bbls/day) Loading/Unloading/Dump

Source:

*Provide detailed calculations documenting the potential emissions and emission factors used to calculate emissions from this source.

- Potential Operating Schedule - Provide the operating schedule for this emissions unit

Hours/day: 24 Hours/year: 8760

Emissions Information "Potential to emit" means the maximum capacity of a source to emit any air pollutant under its physical and operational design. Any physical or operational limitation on the capacity of a source to emit an air pollutant, including air pollution control equipment and restrictions on hours of operation or on the type or amount of material combusted, stored or processed, shall be treated as part of its design if the limitation is enforceable by the EPA and the Division. This term does not alter or affect the use of this term for any other purposes under the Act, or the term "capacity factor" as used in Title IV of the Act or the regulations promulgated thereunder.

Basis for Determination Options:

- Manufacturer Data
- Test results for this source
- Similar source test results
- GRICalc
- Tanks Program
- AP-42
- Other. If this is selected, attach a document with a description of the method used.

| Pollutant | Pre- | Efficiency | Standards | | | Basis for |
|-----------------------------------------------------------------|---------------------------------------------------|-----------------------------|-----------|-------------------------|--------------------------|--------------------|
| | Controlled Potential Emissions (tons/yr) | Potential to Emit (PTE)* | Units* | Emit (PTE) (Ibs/hr)* | Emit (PTE) (tons/yr)* | Determinatio n* |
| Particulate emissions (PE/PM) (formerly particulate matter, PM) | 0 | 0 | | 0 | 0 | |

| | (=) | | | | |
|------------------------------------------|-----|---|---|---|-------|
| PM # 10 microns in diameter (PE/PM10) | 0 | 0 | 0 | 0 | |
| PM # 2.5 microns in diameter (PE/PM2.5) | 0 | 0 | 0 | 0 | |
| Sulfur dioxide (SO2) | 0 | 0 | 0 | 0 | |
| Nitrogen oxides (NOx) | 0 | 0 | 0 | 0 | |
| Carbon monoxide (CO) | 0 | 0 | 0 | 0 | |
| Volatile organic compounds (VOC) | 1.3 | 0 | 0 | 0 | AP-42 |
| Lead (Pb) | 0 | 0 | 0 | 0 | |
| Total Hazardous Air Pollutants (HAPs) | 0.1 | 0 | 0 | 0 | AP-42 |
| Fluoride (F) | 0 | 0 | 0 | 0 | |
| Hydrogen Sulfide (H2S) | 0 | 0 | 0 | 0 | |
| Mercury (Hg) | 0 | 0 | 0 | 0 | |
| Total Reduced Sulfur (TRS) | 0 | 0 | 0 | 0 | |
| Sulfuric Acid Mist (SAM) | 0 | 0 | 0 | 0 | |

| Pollutant | Pollutant | Pre- | Efficiency | Standards | Potential to | | |
|-----------|-----------|---------------------------------------------------|-----------------------------|-----------|-------------------------|------------|--------------------|
| | Category | Controlled Potential Emissions (tons/yr) | Potential to Emit (PTE)* | Units* | Emit (PTE) (Ibs/hr)* | (tons/yr)* | Determinati on* |

Greenhouse Gases (GHGs):

| Pollutant | Pollutant | Pre- | Efficiency | Standards | | Potential to | |
|-----------|-----------|---------------------------------------------------|-----------------------------|-----------|-----------|--------------|--------------------|
| | Category | Controlled Potential Emissions (tons/yr) | Potential to Emit (PTE)* | Units* | (lbs/hr)* | (tons/yr)* | Determinati on* |

^{*} Provide your calculations as an attachment and explain how all process variables and emissions factors were selected. Note the emission factor(s) employed and document origin. Example: AP-42, Table 4.4-3 (8/97); stack test, Method 5, 4/96; mass balance based on MSDS; etc.

Best Available Control Technology (BACT)

Was a BACT Analysis completed for this unit? No

Lowest Achievable Emission Rate (LAER)

Was a LAER Analysis completed for this unit? No

- Federal and State Rule Applicability

New Source Performance Standards (NSPS)
New Source Performance Standards are listed under 40
CFR 60 - Standards of Performance for New Stationary
Sources.

Not affected

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 61)

National Emissions Standards for Hazardous Air Pollutants

Not affected

^{**} AQD Calculated - See 'Help' for more information.

(NESHAP Part 61) are listed under 40 CFR 61. (These include asbestos, benzene, beryllium, mercury, and vinyl chloride).

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63)

Not affected

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63) standards are listed under 40 CFR 63.

Prevention of Significant Deterioration (PSD)

Not Affected

These rules are found under WAQSR Chapter 6, Section 4.

Non-Attainment New Source Review

These rules are found under WAQSR Chapter 6, Section

Not Affected

| Required Attachment | Public Document Id | Attachment Type | Description |
|------------------------|-----------------------|-----------------|-------------|
|------------------------|-----------------------|-----------------|-------------|

AQD EU ID: TNK001

AQD EU description:

Company EU ID: T1

Company EU Description: 400-bbl condensate

storage tank

- Source Installation or Modification Schedule – Select reason(s) for this emissions unit being included in this application (must be completed regardless of date of installation or modification):

Modification

When will you begin to modify the air contaminant source? 07/20/2015

Emission Unit Type Specific Information

Emission Unit Type: Storage Tank/Silo

Maximum Hourly Throughput 2,5000

.

Units: barrels/hr

Is Tank Heated: Yes

Operating Pressure (psig): 0.01

Vapor Pressure of Material 6.00

Stored (psig):

- Potential Operating Schedule - Provide the operating schedule for this emissions unit

Hours/day: 24 Hours/year: 8760

Emissions Information "Potential to emit" means the maximum capacity of a source to emit any air pollutant under its physical and operational design. Any physical or operational limitation on the capacity of a source to emit an air pollutant, including air pollution control equipment and restrictions on hours of operation or on the type or amount of material combusted, stored or processed, shall be treated as part of its design if the limitation is enforceable by the EPA and the Division. This term does not alter or affect the use of this term for any other purposes under the Act, or the term "capacity factor" as used in Title IV of the Act or the regulations promulgated thereunder.

Basis for Determination Options:

- Manufacturer Data
- Test results for this source
- Similar source test results
- GRICalc
- Tanks Program
- AP-42
- Other. If this is selected, attach a document with a description of the method used.

| Pollutant | Pre- | Efficiency Standards | | Potential to | Potential to | Basis for |
|-----------------------------------------------------------------|---------------------------------------------------|-----------------------------|--------|-------------------------|--------------------------|--------------------|
| | Controlled Potential Emissions (tons/yr) | Potential to Emit (PTE)* | Units* | Emit (PTE) (Ibs/hr)* | Emit (PTE) (tons/yr)* | Determinatio n* |
| Particulate emissions (PE/PM) (formerly particulate matter, PM) | 0 | 0 | | 0 | 0 | |
| PM # 10 microns in | 0 | 0 | | 0 | 0 | |

| diameter (PE/PM10) | | | | | |
|------------------------------------------|------|---|-------|------|------------------|
| PM # 2.5 microns in diameter (PE/PM2.5) | 0 | 0 | 0 | 0 | |
| Sulfur dioxide (SO2) | 0 | 0 | 0 | 0 | |
| Nitrogen oxides (NOx) | 0 | 0 | 0 | 0 | |
| Carbon monoxide (CO) | 0 | 0 | 0 | 0 | |
| Volatile organic compounds (VOC) | 36.8 | 0 | 0.17 | 0.7 | Tanks Program |
| Lead (Pb) | 0 | 0 | 0 | 0 | |
| Total Hazardous Air Pollutants (HAPs) | 1.65 | 0 | 0.008 | 0.03 | Tanks Program |
| Fluoride (F) | 0 | 0 | 0 | 0 | |
| Hydrogen Sulfide (H2S) | 0 | 0 | 0 | 0 | |
| Mercury (Hg) | 0 | 0 | 0 | 0 | |
| Total Reduced Sulfur (TRS) | 0 | 0 | 0 | 0 | |
| Sulfuric Acid Mist (SAM) | 0 | 0 | 0 | 0 | |

| Pollutant | Pollutant | Pre- | Efficiency | Standards | Potential to | | |
|-----------|-----------|-------------------------------------|-----------------------------|-----------|-------------------------|--------------------------|--------------------|
| | Category | Potential Emissions (tons/yr) | Potential to Emit (PTE)* | Units* | Emit (PTE) (Ibs/hr)* | Emit (PTE) (tons/yr)* | Determinati on* |

Greenhouse Gases (GHGs):

| Pollutant | Pollutant | Pre- | Efficiency | Standards | | Potential to | |
|-----------|-----------|---------------------------------------------------|-----------------------------|-----------|-------------------------|--------------------------|--------------------|
| | Category | Controlled Potential Emissions (tons/yr) | Potential to Emit (PTE)* | Units* | Emit (PTE) (Ibs/hr)* | Emit (PTE) (tons/yr)* | Determinati on* |

^{*} Provide your calculations as an attachment and explain how all process variables and emissions factors were selected. Note the emission factor(s) employed and document origin. Example: AP-42, Table 4.4-3 (8/97); stack test, Method 5, 4/96; mass balance based on MSDS; etc.

Best Available Control Technology (BACT)

Was a BACT Analysis completed for this unit? No

- Lowest Achievable Emission Rate (LAER)

Was a LAER Analysis completed for this unit? No

- Federal and State Rule Applicability

New Source Performance Standards (NSPS) New Source Performance Standards are listed under 40 CFR 60 - Standards of Performance for New Stationary

Subject to subpart

NSPS Subpart

OCOO - Crude Oil and Natural Gas Production, Transmission and Distribution

Sources.

^{**} AQD Calculated - See 'Help' for more information.

National Emission Standards for Hazardous Air

Pollutants (NESHAP Part 61)
National Emissions Standards for Hazardous Air Pollutants
(NESHAP Part 61) are listed under 40 CFR 61. (These include asbestos, benzene, beryllium, mercury, and vinyl chloride).

Not affected

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63)

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63) standards are listed under 40 CFR 63. Not affected

Prevention of Significant Deterioration (PSD)
These rules are found under WAQSR Chapter 6, Section 4.

Not Affected

Non-Attainment New Source Review

These rules are found under WAQSR Chapter 6, Section 13.

Not Affected

| Required F Attachment | Public Document Id | Attachment Type | Description |
|--------------------------|-----------------------|-----------------|-------------|
|--------------------------|-----------------------|-----------------|-------------|

AQD EU ID: TNK002

AQD EU description:

Company EU ID: T2

Company EU Description: 400-bbl condensate

storage tank

Source Installation or Modification Schedule – Select reason(s) for this emissions unit being included in this application (must be completed regardless of date of installation or modification):

Modification

When will you begin to modify the air contaminant source? 07/20/2015

- Emission Unit Type Specific Information

Emission Unit Type: Storage Tank/Silo

Maximum Hourly Throughput 2.5000

.

Units: barrels/hr

Is Tank Heated: Yes

Operating Pressure (psig): 0.01

Vapor Pressure of Material 6.00

Stored (psig):

- Potential Operating Schedule - Provide the operating schedule for this emissions unit

Hours/day: 24 Hours/year: 8760

- Emissions Information "Potential to emit" means the maximum capacity of a source to emit any air pollutant under its physical and operational design. Any physical or operational limitation on the capacity of a source to emit an air pollutant, including air pollution control equipment and restrictions on hours of operation or on the type or amount of material combusted, stored or processed, shall be treated as part of its design if the limitation is enforceable by the EPA and the Division. This term does not alter or affect the use of this term for any other purposes under the Act, or the term "capacity factor" as used in Title IV of the Act or the regulations promulgated thereunder.

Basis for Determination Options:

- Manufacturer Data
- Test results for this source
- Similar source test results
- GRICalc
- Tanks Program
- AP-42
- Other. If this is selected, attach a document with a description of the method used.

| Pollutant | Pre- | Efficiency | Standards | Potential to | Potential to | Basis for |
|-----------------------------------------------------------------|---------------------------------------------------|-----------------------------|-----------|-------------------------|--------------------------|--------------------|
| | Controlled Potential Emissions (tons/yr) | Potential to Emit (PTE)* | Units* | Emit (PTE) (Ibs/hr)* | Emit (PTE) (tons/yr)* | Determinatio n* |
| Particulate emissions (PE/PM) (formerly particulate matter, PM) | 0 | 0 | | 0 | 0 | |
| PM # 10 microns in | 0 | 0 | | 0 | 0 | |

| diameter (PE/PM10) | | | | | |
|------------------------------------------|------|---|-------|------|------------------|
| PM # 2.5 microns in diameter (PE/PM2.5) | 0 | 0 | 0 | 0 | |
| Sulfur dioxide (SO2) | 0 | 0 | 0 | 0 | |
| Nitrogen oxides (NOx) | 0 | 0 | 0 | 0 | |
| Carbon monoxide (CO) | 0 | 0 | 0 | 0 | |
| Volatile organic compounds (VOC) | 36.8 | 0 | 0.17 | 0.7 | Tanks Program |
| Lead (Pb) | 0 | 0 | 0 | 0 | |
| Total Hazardous Air Pollutants (HAPs) | 1.65 | 0 | 0.008 | 0.03 | Tanks Program |
| Fluoride (F) | 0 | 0 | 0 | 0 | |
| Hydrogen Sulfide (H2S) | 0 | 0 | 0 | 0 | |
| Mercury (Hg) | 0 | 0 | 0 | 0 | |
| Total Reduced Sulfur (TRS) | 0 | 0 | 0 | 0 | |
| Sulfuric Acid Mist (SAM) | 0 | 0 | 0 | 0 | |

| ٠, | | | | | | | | |
|----|-----------|-----------|---------------------------------------------------|-----------------------------|-----------|-------------------------|--------------|--------------------|
| | Pollutant | Pollutant | Pre- Efficiency Standa | | Standards | | Potential to | |
| | | Category | Controlled Potential Emissions (tons/yr) | Potential to Emit (PTE)* | Units* | Emit (PTE) (lbs/hr)* | (tons/yr)* | Determinati on* |

Greenhouse Gases (GHGs):

| Pollutant | Pollutant Category | Pre- Controlled Potential | Efficiency Potential to Emit (PTE)* | Units* | Potential to Emit (PTE) (lbs/hr)* | Potential to Emit (PTE) (tons/yr)* | |
|-----------|-----------------------|---------------------------------|-------------------------------------|--------|-----------------------------------------|------------------------------------------|----|
| | | Emissions (tons/yr) | Emit (PTE)* | | (IDS/III) | (tons/yr) | on |

^{*} Provide your calculations as an attachment and explain how all process variables and emissions factors were selected. Note the emission factor(s) employed and document origin. Example: AP-42, Table 4.4-3 (8/97); stack test, Method 5, 4/96; mass balance based on MSDS; etc.

Best Available Control Technology (BACT)

Was a BACT Analysis completed for this unit? No

- Lowest Achievable Emission Rate (LAER)

Was a LAER Analysis completed for this unit? No

- Federal and State Rule Applicability

New Source Performance Standards (NSPS) New Source Performance Standards are listed under 40 CFR 60 - Standards of Performance for New Stationary Sources. Subject to subpart

| NSPS Subpart | | | | | | | | | | |
|--------------|---|-------|-----|-----|---------|-----|-------------|--------------|-----|--------------|
| 0000 | - | Crude | Oil | and | Natural | Gas | Production, | Transmission | and | Distribution |

^{**} AQD Calculated - See 'Help' for more information.

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 61)

Not affected

National Emissions Standards for Hazardous Air Pollutants (NESHAP Part 61) are listed under 40 CFR 61. (These include asbestos, benzene, beryllium, mercury, and vinyl

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63)

Not affected

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63) standards are listed under 40 CFR 63.

Prevention of Significant Deterioration (PSD)
These rules are found under WAQSR Chapter 6, Section 4.

Not Affected

Not Affected

Non-Attainment New Source Review These rules are found under WAQSR Chapter 6, Section

| Required Publ Attachment | ic Document Id | Attachment Type | Description |
|-----------------------------|-------------------|-----------------|-------------|
|-----------------------------|-------------------|-----------------|-------------|

AQD EU ID: TNK003

AQD EU description:

Company EU ID: T3

Company EU Description: 400-bbl water

storage tank

- Source Installation or Modification Schedule – Select reason(s) for this emissions unit being included in this application (must be completed regardless of date of installation or modification):

Modification

When will you begin to modify the air contaminant source? 07/20/2015

- Emission Unit Type Specific Information

Emission Unit Type: Storage Tank/Silo

Maximum Hourly Throughput 2.5000

.

Units: barrels/hr

Is Tank Heated: Yes

Operating Pressure (psig): 0.01

Vapor Pressure of Material 0.01

Stored (psig):

- Potential Operating Schedule - Provide the operating schedule for this emissions unit

Hours/day: 24 Hours/year: 8760

Emissions Information "Potential to emit" means the maximum capacity of a source to emit any air pollutant under its physical and operational design. Any physical or operational limitation on the capacity of a source to emit an air pollutant, including air pollution control equipment and restrictions on hours of operation or on the type or amount of material combusted, stored or processed, shall be treated as part of its design if the limitation is enforceable by the EPA and the Division. This term does not alter or affect the use of this term for any other purposes under the Act, or the term "capacity factor" as used in Title IV of the Act or the regulations promulgated thereunder.

Basis for Determination Options:

- Manufacturer Data
- Test results for this source
- Similar source test results
- GRICalc
- Tanks Program
- AP-42
- Other. If this is selected, attach a document with a description of the method used.

| Pollutant | Pre- | Efficiency | Standards | Potential to | Potential to | Basis for | |
|-----------------------------------------------------------------|---------------------------------------------------|-----------------------------|-----------|-------------------------|--------------------------|--------------------|--|
| | Controlled Potential Emissions (tons/yr) | Potential to Emit (PTE)* | Units* | Emit (PTE) (Ibs/hr)* | Emit (PTE) (tons/yr)* | Determinatio n* | |
| Particulate emissions (PE/PM) (formerly particulate matter, PM) | 0 | 0 | | 0 | 0 | | |
| PM # 10 microns in | 0 | 0 | | 0 | 0 | | |

| diameter (PE/PM10) | | | | | |
|------------------------------------------|---|---|---|-----|--|
| PM # 2.5 microns in diameter (PE/PM2.5) | 0 | 0 | 0 | 0 | |
| Sulfur dioxide (SO2) | 0 | 0 | 0 | 0 | |
| Nitrogen oxides (NOx) | 0 | 0 | 0 | 0 | |
| Carbon monoxide (CO) | 0 | 0 | 0 | 0 | |
| Volatile organic compounds (VOC) | 0 | 0 | 0 | 0 | |
| Lead (Pb) | 0 | 0 | 0 | 0 | |
| Total Hazardous Air Pollutants (HAPs) | 0 | 0 | 0 | 0 | |
| Fluoride (F) | 0 | 0 | 0 | 0 | |
| Hydrogen Sulfide (H2S) | 0 | 0 | 0 | 0 , | |
| Mercury (Hg) | 0 | 0 | 0 | 0 | |
| Total Reduced Sulfur (TRS) | 0 | 0 | 0 | 0 | |
| Sulfuric Acid Mist (SAM) | 0 | 0 | 0 | 0 | |

| Pollutant | Pollutant | Pre- | | Standards | | Potential to | |
|-----------|-----------|---------------------------------------------------|-----------------------------|-----------|-------------------------|--------------|--------------------|
| | Category | Controlled Potential Emissions (tons/yr) | Potential to Emit (PTE)* | Units* | Emit (PTE) (Ibs/hr)* | (tons/yr)* | Determinati on* |

Greenhouse Gases (GHGs):

| Pollutant | Pollutant | Pre- | Efficiency | Standards | Potential to | | |
|-----------|-----------|---------------------------------------------------|-----------------------------|-----------|-------------------------|--------------------------|--------------------|
| | Category | Controlled Potential Emissions (tons/yr) | Potential to Emit (PTE)* | Units* | Emit (PTE) (lbs/hr)* | Emit (PTE) (tons/yr)* | Determinati on* |

^{*} Provide your calculations as an attachment and explain how all process variables and emissions factors were selected.

Note the emission factor(s) employed and document origin. Example: AP-42, Table 4.4-3 (8/97); stack test, Method 5, 4/96; mass balance based on MSDS; etc.

Best Available Control Technology (BACT)

Was a BACT Analysis completed for this unit? No

- Lowest Achievable Emission Rate (LAER)

Was a LAER Analysis completed for this unit? No

Federal and State Rule Applicability

New Source Performance Standards (NSPS) New Source Performance Standards are listed under 40 CFR 60 - Standards of Performance for New Stationary Sources.

Subject to subpart

| NSPS Subpart | | | | | | | | | | | |
|--------------|---|-------|-----|-----|---------|-----|-------------|--------------|-----|--------------|--|
| 0000 | _ | Crude | Oil | and | Natural | Gas | Production, | Transmission | and | Distribution | |

^{**} AQD Calculated - See 'Help' for more information.

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 61)

National Emissions Standards for Hazardous Air Pollutants (NESHAP Part 61) are listed under 40 CFR 61. (These include asbestos, benzene, beryllium, mercury, and vinyl

Not affected

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63)

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63) standards are listed under 40 CFR 63.

Not affected

Prevention of Significant Deterioration (PSD)
These rules are found under WAQSR Chapter 6, Section 4.

Not Affected

Non-Attainment New Source Review

These rules are found under WAQSR Chapter 6, Section

Not Affected

| Required Attachment | Public Document Id | Attachment Type | Description |
|------------------------|-----------------------|-----------------|-------------|
|------------------------|-----------------------|-----------------|-------------|

AQD EU ID: TNK004

AQD EU description:

Company EU ID: T4

Company EU Description: 6000 gallon

methanol storage

tank

- Source Installation or Modification Schedule – Select reason(s) for this emissions unit being included in this application (must be completed regardless of date of installation or modification):

Modification

When will you begin to modify the air contaminant source? 07/20/2015

- Emission Unit Type Specific Information

Emission Unit Type: Storage Tank/Silo

Maximum Hourly Throughput 6.2000

Units: gallons/hr

Is Tank Heated: No

Operating Pressure (psig): 0.01

Vapor Pressure of Material 1.89

Stored (psig):

- Potential Operating Schedule - Provide the operating schedule for this emissions unit

Hours/day: 24 Hours/year: 8760

- Emissions Information "Potential to emit" means the maximum capacity of a source to emit any air pollutant under its physical and operational design. Any physical or operational limitation on the capacity of a source to emit an air pollutant, including air pollution control equipment and restrictions on hours of operation or on the type or amount of material combusted, stored or processed, shall be treated as part of its design if the limitation is enforceable by the EPA and the Division. This term does not alter or affect the use of this term for any other purposes under the Act, or the term "capacity factor" as used in Title IV of the Act or the regulations promulgated thereunder.

Basis for Determination Options:

- Manufacturer Data
- Test results for this source
- Similar source test results
- GRICalc
- Tanks Program
- AP-42
- Other. If this is selected, attach a document with a description of the method used.

| Pollutant | Pre- | | | Potential to | Potential to | Basis for |
|-----------------------------------------------------------------|---------------------------------------------------|-----------------------------|--------|-------------------------|--------------------------|--------------------|
| | Controlled Potential Emissions (tons/yr) | Potential to Emit (PTE)* | Units* | Emit (PTE) (Ibs/hr)* | Emit (PTE) (tons/yr)* | Determinatio n* |
| Particulate emissions (PE/PM) (formerly particulate matter, PM) | 0 | 0 | | 0 | 0 | |
| | | | | | | |

| PM # 10 microns in diameter (PE/PM10) | 0 | 0 | 0 | 0 | |
|------------------------------------------|------|---|---|---|------------------|
| PM # 2.5 microns in diameter (PE/PM2.5) | 0 | 0 | 0 | 0 | |
| Sulfur dioxide (SO2) | 0 | 0 | 0 | 0 | |
| Nitrogen oxides (NOx) | 0 | 0 | 0 | 0 | |
| Carbon monoxide (CO) | 0 | 0 | 0 | 0 | |
| Volatile organic compounds (VOC) | 0.05 | 0 | 0 | 0 | Tanks Program |
| Lead (Pb) | 0 | 0 | 0 | 0 | |
| Total Hazardous Air Pollutants (HAPs) | 0 | 0 | 0 | 0 | |
| Fluoride (F) | 0 | 0 | 0 | 0 | |
| Hydrogen Sulfide (H2S) | 0 | 0 | 0 | 0 | |
| Mercury (Hg) | 0 | 0 | 0 | 0 | |
| Total Reduced Sulfur (TRS) | 0 | 0 | 0 | 0 | |
| Sulfuric Acid Mist (SAM) | 0 | 0 | 0 | 0 | |

| Pollutant | Pollutant Category | Pre- Controlled Potential Emissions (tons/yr) | | Standards Units* | | Potential to Emit (PTE) (tons/yr)* | |
|-----------|-----------------------|-----------------------------------------------------------|--|---------------------|--|------------------------------------------|--|
|-----------|-----------------------|-----------------------------------------------------------|--|---------------------|--|------------------------------------------|--|

Greenhouse Gases (GHGs):

| Pollutant | Pollutant | Pre- | Efficiency | Standards | | Potential to | |
|-----------|-----------|---------------------------------------------------|-----------------------------|-----------|-----------|--------------|--------------------|
| | Category | Controlled Potential Emissions (tons/yr) | Potential to Emit (PTE)* | Units* | (lbs/hr)* | (tons/yr)* | Determinati on* |

^{*} Provide your calculations as an attachment and explain how all process variables and emissions factors were selected.

Note the emission factor(s) employed and document origin. Example: AP-42, Table 4.4-3 (8/97); stack test, Method 5, 4/96; mass balance based on MSDS; etc.

Best Available Control Technology (BACT)

Was a BACT Analysis completed for this unit? No

Lowest Achievable Emission Rate (LAER)

Was a LAER Analysis completed for this unit? No

- Federal and State Rule Applicability

New Source Performance Standards (NSPS) New Source Performance Standards are listed under 40 CFR 60 - Standards of Performance for New Stationary Sources. Not affected

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 61)

National Emissions Standards for Hazardous Air Pollutants

Not affected

^{**} AQD Calculated - See 'Help' for more information.

(NESHAP Part 61) are listed under 40 CFR 61. (These include asbestos, benzene, beryllium, mercury, and vinyl chloride).

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63) National Emission Standards for Hazardous Air Pollutants

Not affected

(NESHAP Part 63) standards are listed under 40 CFR 63.

Prevention of Significant Deterioration (PSD)

Not Affected

These rules are found under WAQSR Chapter 6, Section 4.

Non-Attainment New Source Review

Not Affected

These rules are found under WAQSR Chapter 6, Section 13.

| Required Attachment | Public Document Id | Attachment Type | Description |
|------------------------|-----------------------|-----------------|-------------|
| | | | |

AQD EU ID: TNK005

AQD EU description:

Company EU ID: T5

Company EU Description: 6000 gallon

methanol storage

tank

- Source Installation or Modification Schedule – Select reason(s) for this emissions unit being included in this application (must be completed regardless of date of installation or modification):

Modification

When will you begin to modify the air contaminant source? 07/20/2015

- Emission Unit Type Specific Information

Emission Unit Type: Storage Tank/Silo

Maximum Hourly Throughput 6.2000

Units: gallons/hr

Is Tank Heated: No

Operating Pressure (psig): 0.01

Vapor Pressure of Material 1.89

Stored (psig):

Potential Operating Schedule – Provide the operating schedule for this emissions unit

Hours/day: 24 Hours/year: 8760

Emissions Information "Potential to emit" means the maximum capacity of a source to emit any air pollutant under its physical and operational design. Any physical or operational limitation on the capacity of a source to emit an air pollutant, including air pollution control equipment and restrictions on hours of operation or on the type or amount of material combusted, stored or processed, shall be treated as part of its design if the limitation is enforceable by the EPA and the Division. This term does not alter or affect the use of this term for any other purposes under the Act, or the term "capacity factor" as used in Title IV of the Act or the regulations promulgated thereunder.

Basis for Determination Options:

- Manufacturer Data
- Test results for this source
- Similar source test results
- GRICalc
- Tanks Program
- AP-42
- Other. If this is selected, attach a document with a description of the method used.

| Pollutant | Pre- | Efficiency Standards | | Potential to | Potential to | Basis for |
|-----------------------------------------------------------------|---------------------------------------------------|-----------------------------|--------|-------------------------|--------------------------|--------------------|
| | Controlled Potential Emissions (tons/yr) | Potential to Emit (PTE)* | Units* | Emit (PTE) (lbs/hr)* | Emit (PTE) (tons/yr)* | Determinatio n* |
| Particulate emissions (PE/PM) (formerly particulate matter, PM) | 0 | 0 | | 0 | 0 | |

| PM # 10 microns in diameter (PE/PM10) | 0 | 0 | 0 | 0 | |
|------------------------------------------|------|---|---|---|------------------|
| PM # 2.5 microns in diameter (PE/PM2.5) | 0 | 0 | 0 | 0 | |
| Sulfur dioxide (SO2) | 0 | 0 | 0 | 0 | |
| Nitrogen oxides (NOx) | 0 | 0 | 0 | 0 | |
| Carbon monoxide (CO) | 0 | 0 | 0 | 0 | |
| Volatile organic compounds (VOC) | 0.05 | 0 | 0 | 0 | Tanks Program |
| Lead (Pb) | 0 | 0 | 0 | 0 | |
| Total Hazardous Air Pollutants (HAPs) | 0 | 0 | 0 | 0 | |
| Fluoride (F) | 0 | 0 | 0 | 0 | |
| Hydrogen Sulfide (H2S) | 0 | 0 | 0 | 0 | |
| Mercury (Hg) | 0 | 0 | 0 | 0 | |
| Total Reduced Sulfur (TRS) | 0 | 0 | 0 | 0 | |
| Sulfuric Acid Mist (SAM) | 0 | 0 | 0 | 0 | |

| Pollutant | Pollutant | Pre- | Efficiency | Standards | Potential to | | |
|-----------|-----------|---------------------------------------------------|-----------------------------|-----------|-------------------------|--------------------------|--------------------|
| | Category | Controlled Potential Emissions (tons/yr) | Potential to Emit (PTE)* | Units* | Emit (PTE) (lbs/hr)* | Emit (PTE) (tons/yr)* | Determinati on* |

Greenhouse Gases (GHGs):

| Pollutant | Pollutant | Pre- | Efficiency | Standards | Potential to | | |
|-----------|-----------|-------------------------------------|-----------------------------|-----------|-------------------------|--------------------------|--------------------|
| | Category | Potential Emissions (tons/yr) | Potential to Emit (PTE)* | Units* | Emit (PTE) (lbs/hr)* | Emit (PTE) (tons/yr)* | Determinati on* |

^{*} Provide your calculations as an attachment and explain how all process variables and emissions factors were selected. Note the emission factor(s) employed and document origin. Example: AP-42, Table 4.4-3 (8/97); stack test, Method 5, 4/96; mass balance based on MSDS; etc.

- Best Available Control Technology (BACT)

Was a BACT Analysis completed for this unit? No

- Lowest Achievable Emission Rate (LAER)

Was a LAER Analysis completed for this unit? No

Federal and State Rule Applicability

New Source Performance Standards (NSPS)
New Source Performance Standards are listed under 40
CFR 60 - Standards of Performance for New Stationary
Sources.

Not affected

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 61)

National Emissions Standards for Hazardous Air Pollutants

Not affected

^{**} AQD Calculated - See 'Help' for more information.

(NESHAP Part 61) are listed under 40 CFR 61. (These include asbestos, benzene, beryllium, mercury, and vinyl chloride).

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63)

Not affected

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63) standards are listed under 40 CFR 63.

Prevention of Significant Deterioration (PSD)

Not Affected

These rules are found under WAQSR Chapter 6, Section 4.

Non-Attainment New Source Review
These rules are found under WAQSR Chapter 6, Section

Not Affected

| Required Pu | ıblic Document Id | Attachment Type | Description |
|-------------|----------------------|-----------------|-------------|
|-------------|----------------------|-----------------|-------------|

AQD EU ID: TNK006

AQD EU description:

Company EU ID: T6

Company EU Description: 500-bbl water

storage tank

Source Installation or Modification Schedule – Select reason(s) for this emissions unit being included in this application (must be completed regardless of date of installation or modification):

Modification

When will you begin to modify the air contaminant source? 07/20/2015

- Emission Unit Type Specific Information

Emission Unit Type: Storage Tank/Silo

Maximum Hourly Throughput 166.6700

Units: barrels/hr

Is Tank Heated: No

Operating Pressure (psig): 0.01

Vapor Pressure of Material 0.01

Stored (psig):

- Potential Operating Schedule - Provide the operating schedule for this emissions unit

Hours/day: 24 Hours/year: 8760

Emissions Information "Potential to emit" means the maximum capacity of a source to emit any air pollutant under its physical and operational design. Any physical or operational limitation on the capacity of a source to emit an air pollutant, including air pollution control equipment and restrictions on hours of operation or on the type or amount of material combusted, stored or processed, shall be treated as part of its design if the limitation is enforceable by the EPA and the Division. This term does not alter or affect the use of this term for any other purposes under the Act, or the term "capacity factor" as used in Title IV of the Act or the regulations promulgated thereunder.

Basis for Determination Options:

- Manufacturer Data
- Test results for this source
- Similar source test results
- GRICalc
- Tanks Program
- AP-42
- Other. If this is selected, attach a document with a description of the method used.

| Pollutant | Pre- | Efficiency | Standards | Potential to | Potential to | Basis for |
|-----------------------------------------------------------------|---------------------------------------------------|-----------------------------|-----------|-------------------------|--------------------------|--------------------|
| | Controlled Potential Emissions (tons/yr) | Potential to Emit (PTE)* | Units* | Emit (PTE) (Ibs/hr)* | Emit (PTE) (tons/yr)* | Determinatio n* |
| Particulate emissions (PE/PM) (formerly particulate matter, PM) | 0 | 0 | | 0 | 0 | |
| PM # 10 microns in | 0 | 0 | | 0 | 0 | |

| | | | () | | Manager programming and research control of the programming and the second |
|------------------------------------------|------|---|----|---|----------------------------------------------------------------------------|
| diameter (PE/PM10) | | | | | |
| PM # 2.5 microns in diameter (PE/PM2.5) | 0 | 0 | 0 | 0 | |
| Sulfur dioxide (SO2) | 0 | 0 | 0 | 0 | |
| Nitrogen oxides (NOx) | 0 | 0 | 0 | 0 | |
| Carbon monoxide (CO) | 0 | 0 | 0 | 0 | |
| Volatile organic compounds (VOC) | 0.62 | 0 | 0 | 0 | AP-42 |
| Lead (Pb) | 0 | 0 | 0 | 0 | |
| Total Hazardous Air Pollutants (HAPs) | 0.02 | 0 | 0 | 0 | AP-42 |
| Fluoride (F) | 0 | 0 | 0 | 0 | |
| Hydrogen Sulfide (H2S) | 0 | 0 | 0 | 0 | |
| Mercury (Hg) | 0 | 0 | 0 | 0 | |
| Total Reduced Sulfur (TRS) | 0 | 0 | 0 | 0 | |
| Sulfuric Acid Mist (SAM) | 0 | 0 | 0 | 0 | |

| | Pollutant Category Controlled Potential Emissions (tons/yr) | Efficiency Standards Potential to Emit (PTE)* | Potential to Emit (PTE) (lbs/hr)* | Potential to Emit (PTE) (tons/yr)* | Basis for Determinati on* |
|--|-------------------------------------------------------------|-----------------------------------------------|-----------------------------------------|------------------------------------------|---------------------------------|
|--|-------------------------------------------------------------|-----------------------------------------------|-----------------------------------------|------------------------------------------|---------------------------------|

Greenhouse Gases (GHGs):

| Pollutant | Pollutant | Pre- | Efficiency | Standards | Potential to | | |
|-----------|-----------|------|-----------------------------|-----------|--------------|------------|--------------------|
| | Category | | Potential to Emit (PTE)* | Units* | (lbs/hr)* | (tons/yr)* | Determinati on* |

^{*} Provide your calculations as an attachment and explain how all process variables and emissions factors were selected. Note the emission factor(s) employed and document origin. Example: AP-42, Table 4.4-3 (8/97); stack test, Method 5, 4/96; mass balance based on MSDS; etc.

- Best Available Control Technology (BACT)

Was a BACT Analysis completed for this unit? No

- Lowest Achievable Emission Rate (LAER)

Was a LAER Analysis completed for this unit? No

- Federal and State Rule Applicability

New Source Performance Standards (NSPS) New Source Performance Standards are listed under 40 CFR 60 - Standards of Performance for New Stationary Sources. Subject to subpart

| NSPS Subpart | | | | | | | | | | |
|--------------|---|-------|-----|-----|---------|-----|-------------|--------------|-----|--------------|
| 0000 | - | Crude | Oil | and | Natural | Gas | Production, | Transmission | and | Distribution |

^{**} AQD Calculated - See 'Help' for more information.

National Emission Standards for Hazardous Air

Not affected

Pollutants (NESHAP Part 61)
National Emissions Standards for Hazardous Air Pollutants (NESHAP Part 61) are listed under 40 CFR 61. (These include asbestos, benzene, beryllium, mercury, and vinyl chloride).

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63)

Not affected

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63) standards are listed under 40 CFR 63.

Prevention of Significant Deterioration (PSD)

Not Affected

These rules are found under WAQSR Chapter 6, Section 4.

Not Affected

Non-Attainment New Source Review These rules are found under WAQSR Chapter 6, Section 13.

| Required Attachment | Public Document | Attachment Type | Description | |
|------------------------|-----------------|-----------------|-------------|--|
|------------------------|-----------------|-----------------|-------------|--|

AQD EU ID: TNK007

AQD EU description:

Company EU ID: T7

Company EU Description: 500-bbl water

storage tank

Source Installation or Modification Schedule – Select reason(s) for this emissions unit being included in this application (must be completed regardless of date of installation or modification):

Modification

When will you begin to modify the air contaminant source? 07/20/2015

- Emission Unit Type Specific Information

Emission Unit Type: Storage Tank/Silo

Maximum Hourly Throughput 166.6700

Units: barrels/hr

Is Tank Heated: No

Operating Pressure (psig): 0.01

Vapor Pressure of Material 0.01

Stored (psig):

- Potential Operating Schedule - Provide the operating schedule for this emissions unit

Hours/day: 24 Hours/year: 8760

Emissions Information "Potential to emit" means the maximum capacity of a source to emit any air pollutant under its physical and operational design. Any physical or operational limitation on the capacity of a source to emit an air pollutant, including air pollution control equipment and restrictions on hours of operation or on the type or amount of material combusted, stored or processed, shall be treated as part of its design if the limitation is enforceable by the EPA and the Division. This term does not alter or affect the use of this term for any other purposes under the Act, or the term "capacity factor" as used in Title IV of the Act or the regulations promulgated thereunder.

Basis for Determination Options:

- Manufacturer Data
- Test results for this source
- Similar source test results
- GRICalc
- Tanks Program
- AP-42
- Other. If this is selected, attach a document with a description of the method used.

| Pollutant | Pre- | Efficiency | Standards | Potential to | Potential to | Basis for |
|-----------------------------------------------------------------|---------------------------------------------------|-----------------------------|-----------|-------------------------|--------------------------|--------------------|
| | Controlled Potential Emissions (tons/yr) | Potential to Emit (PTE)* | Units* | Emit (PTE) (Ibs/hr)* | Emit (PTE) (tons/yr)* | Determinatio n* |
| Particulate emissions (PE/PM) (formerly particulate matter, PM) | 0 | 0 | | 0 | 0 | |
| PM # 10 microns in | 0 | 0 | | 0 | 0 | |

| diameter (PE/PM10) | | | | | |
|------------------------------------------|------|---|---|---|-------|
| PM # 2.5 microns in diameter (PE/PM2.5) | 0 | 0 | 0 | 0 | |
| Sulfur dioxide (SO2) | 0 | 0 | 0 | 0 | |
| Nitrogen oxides (NOx) | 0 | 0 | 0 | 0 | |
| Carbon monoxide (CO) | 0 | 0 | 0 | 0 | |
| Volatile organic compounds (VOC) | 0.62 | 0 | 0 | 0 | AP-42 |
| Lead (Pb) | 0 | 0 | 0 | 0 | |
| Total Hazardous Air Pollutants (HAPs) | 0.02 | 0 | 0 | 0 | AP-42 |
| Fluoride (F) | 0 | 0 | 0 | 0 | |
| Hydrogen Sulfide (H2S) | 0 | 0 | 0 | 0 | |
| Mercury (Hg) | 0 | 0 | 0 | 0 | |
| Total Reduced Sulfur (TRS) | 0 | 0 | 0 | 0 | |
| Sulfuric Acid Mist (SAM) | 0 | 0 | 0 | 0 | |

| Pollutant | Pollutant | Pre- | Efficiency | Standards | | Potential to | |
|-----------|-----------|-------------------------------------|-----------------------------|-----------|-----------|--------------|--------------------|
| | Category | Potential Emissions (tons/yr) | Potential to Emit (PTE)* | Units* | (lbs/hr)* | (tons/yr)* | Determinati on* |

Greenhouse Gases (GHGs):

| Poll | utant | Pollutant | Pre- | Efficiency | Standards | Potential to | | |
|------|-------|-----------|---------------------------------------------------|-----------------------------|-----------|-------------------------|------------|--------------------|
| | | Category | Controlled Potential Emissions (tons/yr) | Potential to Emit (PTE)* | Units* | Emit (PTE) (Ibs/hr)* | (tons/yr)* | Determinati on* |

^{*} Provide your calculations as an attachment and explain how all process variables and emissions factors were selected.

Note the emission factor(s) employed and document origin. Example: AP-42, Table 4.4-3 (8/97); stack test, Method 5, 4/96; mass balance based on MSDS; etc.

Best Available Control Technology (BACT)

Was a BACT Analysis completed for this unit? No

- Lowest Achievable Emission Rate (LAER)

Was a LAER Analysis completed for this unit? No

- Federal and State Rule Applicability

New Source Performance Standards (NSPS) New Source Performance Standards are listed under 40 CFR 60 - Standards of Performance for New Stationary Sources. Subject to subpart

| NSPS Subpart | | | | | | | | | | |
|--------------|---|-------|-----|-----|---------|-----|-------------|------------------|--------------|--|
| 0000 | - | Crude | Oil | and | Natural | Gas | Production, | Transmission and | Distribution | |

^{**} AQD Calculated - See 'Help' for more information.

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 61)

National Emissions Standards for Hazardous Air Pollutants (NESHAP Part 61) are listed under 40 CFR 61. (These include asbestos, benzene, beryllium, mercury, and vinyl chloride).

Not affected

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63)

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63) standards are listed under 40 CFR 63.

Not affected

Prevention of Significant Deterioration (PSD)
These rules are found under WAQSR Chapter 6, Section 4.

Not Affected

Non-Attainment New Source Review

These rules are found under WAQSR Chapter 6, Section 13.

Not Affected

| Required Attachment | Public Document | Attachment Type | Description |
|------------------------|-----------------|-----------------|-------------|
| | | | |

AQD EU ID: TNK008

AQD EU description:

Company EU ID: T8

Company EU Description: 500-bbl water

storage tank

Source Installation or Modification Schedule - Select reason(s) for this emissions unit being included in this application (must be completed regardless of date of installation or modification):

Modification

When will you begin to modify the air contaminant source? 07/20/2015

Emission Unit Type Specific Information

Emission Unit Type: Storage Tank/Silo

Maximum Hourly Throughput 166.6700

Units: barrels/hr

Is Tank Heated: No

Operating Pressure (psig): 0.01

Vapor Pressure of Material 0.01

Stored (psig):

Potential Operating Schedule - Provide the operating schedule for this emissions unit

Hours/day: 24 Hours/year: 8760

Emissions Information "Potential to emit" means the maximum capacity of a source to emit any air pollutant under its physical and operational design. Any physical or operational limitation on the capacity of a source to emit an air pollutant, including air pollution control equipment and restrictions on hours of operation or on the type or amount of material combusted, stored or processed, shall be treated as part of its design if the limitation is enforceable by the EPA and the Division. This term does not alter or affect the use of this term for any other purposes under the Act, or the term "capacity factor" as used in Title IV of the Act or the regulations promulgated thereunder.

Basis for Determination Options:

- Manufacturer Data
- Test results for this source
- Similar source test results
- GRICalc
- Tanks Program
- AP-42
- Other. If this is selected, attach a document with a description of the method used.

| Pollutant | Pre- | Efficiency | Standards | Potential to | Potential to | Basis for |
|-----------------------------------------------------------------|---------------------------------------------------|-----------------------------|-----------|-------------------------|--------------------------|--------------------|
| | Controlled Potential Emissions (tons/yr) | Potential to Emit (PTE)* | Units* | Emit (PTE) (Ibs/hr)* | Emit (PTE) (tons/yr)* | Determinatio n* |
| Particulate emissions (PE/PM) (formerly particulate matter, PM) | 0 | 0 | | 0 | 0 | |
| PM # 10 microns in | 0 | 0 | | 0 | 0 | |

| diameter (PE/PM10) | | | | | |
|------------------------------------------|------|---|---|---|-------|
| PM # 2.5 microns in diameter (PE/PM2.5) | 0 | 0 | 0 | 0 | |
| Sulfur dioxide (SO2) | 0 | 0 | 0 | 0 | |
| Nitrogen oxides (NOx) | 0 | 0 | 0 | 0 | |
| Carbon monoxide (CO) | 0 | 0 | 0 | 0 | |
| Volatile organic compounds (VOC) | 0.62 | 0 | 0 | 0 | AP-42 |
| Lead (Pb) | 0 | 0 | 0 | 0 | |
| Total Hazardous Air Pollutants (HAPs) | 0.02 | 0 | 0 | 0 | AP-42 |
| Fluoride (F) | 0 | 0 | 0 | 0 | |
| Hydrogen Sulfide (H2S) | 0 | 0 | 0 | 0 | |
| Mercury (Hg) | 0 | 0 | 0 | 0 | |
| Total Reduced Sulfur (TRS) | 0 | 0 | 0 | 0 | |
| Sulfuric Acid Mist (SAM) | 0 | 0 | 0 | 0 | |

| Pollutant | Pollutant Category | Pre- Controlled Potential Emissions (tons/yr) | Efficiency Potential to Emit (PTE)* | | Potential to Emit (PTE) (lbs/hr)* | Potential to Emit (PTE) (tons/yr)* | Basis for Determinati on* |
|-----------|-----------------------|-----------------------------------------------------------|-------------------------------------------|--|-----------------------------------------|------------------------------------------|---------------------------------|
|-----------|-----------------------|-----------------------------------------------------------|-------------------------------------------|--|-----------------------------------------|------------------------------------------|---------------------------------|

Greenhouse Gases (GHGs):

| Γ | Pollutant | Pollutant | Pre- | Efficiency S | Standards | | Potential to | |
|---|-----------|-----------|---------------------------------------------------|-----------------------------|-----------|-------------------------|--------------|--------------------|
| | | Category | Controlled Potential Emissions (tons/yr) | Potential to Emit (PTE)* | Units* | Emit (PTE) (Ibs/hr)* | (tons/yr)* | Determinati on* |

^{*} Provide your calculations as an attachment and explain how all process variables and emissions factors were selected. Note the emission factor(s) employed and document origin. Example: AP-42, Table 4.4-3 (8/97); stack test, Method 5, 4/96; mass balance based on MSDS; etc.

- Best Available Control Technology (BACT)

Was a BACT Analysis completed for this unit? No

- Lowest Achievable Emission Rate (LAER)

Was a LAER Analysis completed for this unit? No

- Federal and State Rule Applicability

New Source Performance Standards (NSPS)
New Source Performance Standards are listed under 40
CFR 60 - Standards of Performance for New Stationary
Sources.

Subject to subpart

| | NSPS Subpart | | | | | | | | | | |
|------|--------------|-------|-----|-----|---------|-----|-------------|--------------|-----|--------------|--|
| 0000 | - | Crude | Oil | and | Natural | Gas | Production, | Transmission | and | Distribution | |

Page 64

^{**} AQD Calculated - See 'Help' for more information.

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 61)

Not affected

National Emissions Standards for Hazardous Air Pollutants (NESHAP Part 61) are listed under 40 CFR 61. (These include asbestos, benzene, beryllium, mercury, and vinyl chloride).

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63)

Not affected

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63) standards are listed under 40 CFR 63.

Prevention of Significant Deterioration (PSD)

Not Affected

These rules are found under WAQSR Chapter 6, Section 4.

Non-Attainment New Source Review
These rules are found under WAQSR Chapter 6, Section 13.

Not Affected

| Required Public Document Attachment Id | Attachment Type | Description |
|----------------------------------------|-----------------|-------------|
|----------------------------------------|-----------------|-------------|

AQD EU ID: TNK009

AQD EU description:

Company EU ID: T9

Company EU Description: 500-bbl water

storage tank

Source Installation or Modification Schedule – Select reason(s) for this emissions unit being included in this application (must be completed regardless of date of installation or modification):

Modification

When will you begin to modify the air contaminant source? 07/20/2015

- Emission Unit Type Specific Information

Emission Unit Type: Storage Tank/Silo

Maximum Hourly Throughput 166.6700

Units: barrels/hr

Is Tank Heated: No

Operating Pressure (psig): 0.01

Vapor Pressure of Material 0.01

Stored (psig):

- Potential Operating Schedule - Provide the operating schedule for this emissions unit

Hours/day: 24 Hours/year: 8760

Emissions Information "Potential to emit" means the maximum capacity of a source to emit any air pollutant under its physical and operational design. Any physical or operational limitation on the capacity of a source to emit an air pollutant, including air pollution control equipment and restrictions on hours of operation or on the type or amount of material combusted, stored or processed, shall be treated as part of its design if the limitation is enforceable by the EPA and the Division. This term does not alter or affect the use of this term for any other purposes under the Act, or the term "capacity factor" as used in Title IV of the Act or the regulations promulgated thereunder.

Basis for Determination Options:

- Manufacturer Data
- Test results for this source
- Similar source test results
- GRICalc
- Tanks Program
- AP-42
- Other. If this is selected, attach a document with a description of the method used.

| Pollutant | Pre- | Efficiency | Standards | Potential to | Potential to | Basis for |
|-----------------------------------------------------------------|---------------------------------------------------|-----------------------------|-----------|-------------------------|--------------------------|--------------------|
| | Controlled Potential Emissions (tons/yr) | Potential to Emit (PTE)* | Units* | Emit (PTE) (Ibs/hr)* | Emit (PTE) (tons/yr)* | Determinatio n* |
| Particulate emissions (PE/PM) (formerly particulate matter, PM) | 0 | 0 | | 0 | 0 | |
| PM # 10 microns in | 0 | 0 | | 0 | 0 | |

| diameter (PE/PM10) | | | | | |
|------------------------------------------|------|---|---|---|-------|
| PM # 2.5 microns in diameter (PE/PM2.5) | 0 | 0 | 0 | 0 | |
| Sulfur dioxide (SO2) | 0 | 0 | 0 | 0 | |
| Nitrogen oxides (NOx) | 0 | 0 | 0 | 0 | |
| Carbon monoxide (CO) | 0 | 0 | 0 | 0 | |
| Volatile organic compounds (VOC) | 0.62 | 0 | 0 | 0 | AP-42 |
| Lead (Pb) | 0 | 0 | 0 | 0 | |
| Total Hazardous Air Pollutants (HAPs) | 0.02 | 0 | 0 | 0 | AP-42 |
| Fluoride (F) | 0 | 0 | 0 | 0 | |
| Hydrogen Sulfide (H2S) | 0 | 0 | 0 | 0 | |
| Mercury (Hg) | 0 | 0 | 0 | 0 | |
| Total Reduced Sulfur (TRS) | 0 | 0 | 0 | 0 | |
| Sulfuric Acid Mist (SAM) | 0 | 0 | 0 | 0 | |

| Pollutant | Pollutant | Pre- | | Standards | Potential to | | |
|-----------|-----------|-------------------------------------|-----------------------------|-----------|-------------------------|--------------------------|--------------------|
| | Category | Potential Emissions (tons/yr) | Potential to Emit (PTE)* | Units* | Emit (PTE) (Ibs/hr)* | Emit (PTE) (tons/yr)* | Determinati on* |

Greenhouse Gases (GHGs):

| (tons/vr) | Pollutant | Pollutant Category | Pre- Controlled Potential Emissions | Efficiency Potential to Emit (PTE)* | | | Potential to Emit (PTE) (tons/yr)* | |
|-----------|-----------|-----------------------|----------------------------------------------|-------------------------------------------|--|--|------------------------------------------|--|
|-----------|-----------|-----------------------|----------------------------------------------|-------------------------------------------|--|--|------------------------------------------|--|

^{*} Provide your calculations as an attachment and explain how all process variables and emissions factors were selected. Note the emission factor(s) employed and document origin. Example: AP-42, Table 4.4-3 (8/97); stack test, Method 5, 4/96; mass balance based on MSDS; etc.

- Best Available Control Technology (BACT)

Was a BACT Analysis completed for this unit? No

- Lowest Achievable Emission Rate (LAER)

Was a LAER Analysis completed for this unit? No

- Federal and State Rule Applicability

New Source Performance Standards (NSPS) New Source Performance Standards are listed under 40 CFR 60 - Standards of Performance for New Stationary Sources. Subject to subpart

| NSPS Subpart | | | | | | | | |
|--------------|-------|-----|------------|-----|-------------|--------------|-----|--------------|
| 0000 - | Crude | Oil | and Natura | Gas | Production, | Transmission | and | Distribution |

^{**} AQD Calculated - See 'Help' for more information.

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 61)

Not affected

National Emissions Standards for Hazardous Air Pollutants (NESHAP Part 61) are listed under 40 CFR 61. (These include asbestos, benzene, beryllium, mercury, and vinyl chloride).

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63)

Not affected

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63) standards are listed under 40 CFR 63.

Prevention of Significant Deterioration (PSD)
These rules are found under WAQSR Chapter 6, Section 4.

Not Affected

Not Affected

Non-Attainment New Source Review These rules are found under WAQSR Chapter 6, Section

| Required Public Document Attachment Type Description |
|------------------------------------------------------|
|------------------------------------------------------|

AQD EU ID: TNK010

AQD EU description:

Company EU ID: T10

Company EU Description: 500-bbl water

storage tank

- Source Installation or Modification Schedule – Select reason(s) for this emissions unit being included in this application (must be completed regardless of date of installation or modification):

Modification

When will you begin to modify the air contaminant source? 07/20/2015

- Emission Unit Type Specific Information

Emission Unit Type: Storage Tank/Silo

Maximum Hourly Throughput 166.6700 Units: barrels/hr

Is Tank Heated: No

Operating Pressure (psig): 0.01 Vapor Pressure of Material 0.01

Stored (psig):

- Potential Operating Schedule - Provide the operating schedule for this emissions unit

Hours/day: 24 Hours/year: 8760

Emissions Information "Potential to emit" means the maximum capacity of a source to emit any air pollutant under its physical and operational design. Any physical or operational limitation on the capacity of a source to emit an air pollutant, including air pollution control equipment and restrictions on hours of operation or on the type or amount of material combusted, stored or processed, shall be treated as part of its design if the limitation is enforceable by the EPA and the Division. This term does not alter or affect the use of this term for any other purposes under the Act, or the term "capacity factor" as used in Title IV of the Act or the regulations promulgated thereunder.

Basis for Determination Options:

- Manufacturer Data
- Test results for this source
- Similar source test results
- GRICalc
- Tanks Program
- AP-42
- Other. If this is selected, attach a document with a description of the method used.

| Pollutant | Pre- | Efficiency | Standards | Potential to | Potential to | Basis for | |
|-----------------------------------------------------------------|---------------------------------------------------|-----------------------------|-----------|-------------------------|--------------------------|--------------------|--|
| | Controlled Potential Emissions (tons/yr) | Potential to Emit (PTE)* | Units* | Emit (PTE) (Ibs/hr)* | Emit (PTE) (tons/yr)* | Determinatio n* | |
| Particulate emissions (PE/PM) (formerly particulate matter, PM) | 0 | 0 | | 0 | 0 | | |
| PM # 10 microns in | 0 | 0 | | 0 | 0 | | |

| diameter (PE/PM10) | | | | | |
|------------------------------------------|------|---|---|---|-------|
| PM # 2.5 microns in diameter (PE/PM2.5) | 0 | 0 | 0 | 0 | |
| Sulfur dioxide (SO2) | 0 | 0 | 0 | 0 | |
| Nitrogen oxides (NOx) | 0 | 0 | 0 | 0 | |
| Carbon monoxide (CO) | 0 | 0 | 0 | 0 | |
| Volatile organic compounds (VOC) | 0.62 | 0 | 0 | 0 | AP-42 |
| Lead (Pb) | 0 | 0 | 0 | 0 | |
| Total Hazardous Air Pollutants (HAPs) | 0.02 | 0 | 0 | 0 | AP-42 |
| Fluoride (F) | 0 | 0 | 0 | 0 | |
| Hydrogen Sulfide (H2S) | 0 | 0 | 0 | 0 | |
| Mercury (Hg) | 0 | 0 | 0 | 0 | |
| Total Reduced Sulfur (TRS) | 0 | 0 | 0 | 0 | |
| Sulfuric Acid Mist (SAM) | 0 | 0 | 0 | 0 | |

| Pollutar | | Pre- | Efficiency | Standards | | Potential to | |
|----------|----------|---------------------------------------------------|-----------------------------|-----------|-----------|--------------|--------------------|
| | Category | Controlled Potential Emissions (tons/yr) | Potential to Emit (PTE)* | | (lbs/hr)* | (tons/yr)* | Determinati on* |

Greenhouse Gases (GHGs):

| Pollutant | Pollutant | Pre- | Efficiency Standards | | | Potential to | |
|-----------|-----------|---------------------------------------------------|-----------------------------|--------|-------------------------|--------------------------|-------------|
| | Category | Controlled Potential Emissions (tons/yr) | Potential to Emit (PTE)* | Units* | Emit (PTE) (lbs/hr)* | Emit (PTE) (tons/yr)* | Determinati |

^{*} Provide your calculations as an attachment and explain how all process variables and emissions factors were selected. Note the emission factor(s) employed and document origin. Example: AP-42, Table 4.4-3 (8/97); stack test, Method 5, 4/96; mass balance based on MSDS; etc.

- Best Available Control Technology (BACT)

Was a BACT Analysis completed for this unit? No

- Lowest Achievable Emission Rate (LAER)

Was a LAER Analysis completed for this unit? No

Federal and State Rule Applicability

New Source Performance Standards (NSPS) New Source Performance Standards are listed under 40 CFR 60 - Standards of Performance for New Stationary Sources.

Subject to subpart

| NSPS Subpart | | | | | | | | | |
|--------------|------|------|-----|-----|---------|-----|-------------|-----------------|----------------|
| 0000 - | · C: | rude | Oil | and | Natural | Gas | Production, | Transmission an | d Distribution |

^{**} AQD Calculated - See 'Help' for more information.

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 61)

National Emissions Standards for Hazardous Air Pollutants (NESHAP Part 61) are listed under 40 CFR 61. (These include asbestos, benzene, beryllium, mercury, and vinyl chloride).

Not affected

National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63) National Emission Standards for Hazardous Air Pollutants

(NESHAP Part 63) standards are listed under 40 CFR 63.

Not affected

Prevention of Significant Deterioration (PSD)

These rules are found under WAQSR Chapter 6, Section 4.

Not Affected

Non-Attainment New Source Review

These rules are found under WAQSR Chapter 6. Section

Not Affected

| Required Public Document Attachment Id | Attachment Type | Description |
|----------------------------------------|-----------------|-------------|
|----------------------------------------|-----------------|-------------|

Facility Detail Report
Facility Name: Fairway Compressor Station and Water Transfer Facility
ID: F026209

- Facility Information

Facility ID: F026209

FacilityName: Fairway Compressor Station and Water Transfer Facility

Facility Description:

Company Name: EOG Resources, Inc.

Operating Status: Operating

AFS:

Facility Class: Minor

Facility Type: Compressor Station

CERR Class: NON

- Location

| Physical Address | City | County | Lat/Long | PLSS | Effective Date |
|-------------------------|----------------|---------|-------------------------|-------------------------|----------------|
| Section 36, 13N, 65W | Laramie County | Laramie | 41.05360/- 104.60500 | QSWNW-S36- T13N-R65W | 08/21/2014 |

Location Detail For: Section 36, 13N, 65W

Latitude: 41.05360

Longitude: -104.60500

Quarter Quarter: SW

Quarter: NW

Section: 36

Township: 13N

Range: 65W

County: Laramie

State: Wyoming

Distict: District 1

Physical Address 1: Section 36, 13N, 65W

Physical Address 2:

City: Laramie County

Zip: 82001

Effective Date: 08/21/2014

- Notes

| User Name | Doto | Note |
|-----------|------|------|
| User Name | Date | Note |

- NAICS Codes

486210 Pipeline Transportation of Natural Gas (SIC 4922)

Contacts

| Contact Type | act Type Contact Person Ph | | Contact Person Phone Number Email | | Start Date End Da | |
|------------------------|--------------------------------|----------------|-----------------------------------|------------|-------------------|--|
| Environmental contact | Rice, Curtis | (303)262-9946 | Curtis_Rice@eo gresources.com | 03/09/2015 | | |
| NSR Permitting contact | Smith, Mark | (307) 399-2365 | mark_smith@eog resources.com | 01/05/2015 | | |

Contact Detail For: Rice, Curtis

Prefix: Mr.

First Name: Curtis

Middle Name:

Last Name: Rice

Suffix:

Company Title: Senior Environmental

Contac

Contact's Company Name: EOG Resources, Inc.

Specialist

Address 1: 600 17th Street, Suite 1000N

Address 2:

City: Denver

State: Colorado

Work Phone No: (303) 262-9946

Mobile Phone No.:

Fax No:

Address 2:

Secondary Phone No.:

Secondary Ext. No.:

Pager No.:

Zip Code: 80202

Pager PIN No.:

Email: Curtis Rice@eogresources.com

Email Pager Address:

Contact Detail For: Smith, Mark

Prefix: Mr.

Middle Name:

Suffix:

Company Title: Senior Environmental

Representative

Contact's Company Name: EOG Resources, Inc.

Zip Code: 82001

First Name: Mark Last Name: Smith

Address 1: 3001 E. Pershing Blvd.

Address 2:

City: Cheyenne

State: Wyoming

Work Phone No: (307) 399-2365

Address 2:

Mobile Phone No.:

Fax No:

Secondary Phone No.:

Secondary Ext. No.:

Pager No.:

Pager PIN No.:

Email: mark smith@eogresources.com

Email Pager Address:

Rules & Regs

Subject to Part 60 NSPS:

Subject to 112(r) Accidental Release

Prevention:

Subject to Part 61 NESHAP:

Subject to non-attainment NSR:

Subject to PSD: Subject Part 63 NESHAP:

Subject to Title IV Acid Rain:

Attachments

| Description | Туре | Modified By | Modified Date |
|--------------------------------|-------|---------------|---------------|
| Permit History as of 1/21/2015 | Other | Coffman, Ella | 01/21/2015 |

Version

| Version ID | Version Start Date | Version End Date | Preserved |
|------------|--------------------|------------------|-----------|
| CURRENT | 08/03/2015 | | |
| 31231 | 07/20/2015 | 08/03/2015 | X |
| 30795 | 06/18/2015 | 07/20/2015 | X |
| 30476 | 05/27/2015 | 06/18/2015 | X |
| 27703 | 08/21/2014 | 05/27/2015 | X |

AQD Emissions Unit ID: BVC001

Emission Unit Type: Blow-down/Venting/Well Completion

Type of Event: Blow-down

AQD Description: compressor blowdown - routed to flare

Company Equipment ID: BVC1

Company Equipment Description: compressor blowdown - routed to flare

Operating Status: Operating

Initial Construction Commencement 01/27/2015

Date:

Initial Operation Commencement 01/27/2015

Date:

Most Recent

Construction/Modification

Commencement Date:

Most Recent Operation Commencement Date:

Permitted Emissions

| Pollutant | Potential Emissions | Potential Emissions | Allowable Emissions | Allowable Emissions | Comments |
|-----------|------------------------|------------------------|------------------------|------------------------|----------|
| | (Lbs/hour) | (Tons/Year) | (Lbs/Hour) | (Tons/Year | |

Processes

- Emission Process Information

Process ID: PRC027

Process Name: compressor blowdown

Company Process Description: compressor blowdown

Source Classification Code (SCC): 3-06-004-01

Control equipment(s) directly associated with this process

AQD Emissions Unit ID: BVC002

Emission Unit Type: Blow-down/Venting/Well Completion

Type of Event: Pigging Activities

AQD Description: pigging - routed to flare

Company Equipment ID: BVC2

Company Equipment Description: pigging - routed to flare

Operating Status: Operating

Initial Construction Commencement 01/27/2015

Date:

Initial Operation Commencement 01/27/2015

Date:

Most Recent

Construction/Modification

Commencement Date:

Most Recent Operation Commencement Date:

- Permitted Emissions

| Pollutant | Potential Emissions | Potential Emissions | Allowable Emissions | Allowable Emissions | Comments |
|-----------|------------------------|------------------------|------------------------|------------------------|----------|
| | (Lbs/hour) | (Tons/Year) | (Lbs/Hour) | (Tons/Year | |

- Processes

- Emission Process Information

Process ID: PRC028

Process Name: pigging events

Company Process Description: pigging events

Source Classification Code (SCC): 3-06-004-01

Control equipment(s) directly associated with this process

AQD Emissions Unit ID: DHY001

Emission Unit Type: Dehydration Unit

Dehydration Type: TEG

Design Capacity (MMscf/day): 20.0

AQD Description: 20 MMCFD TEG dehydration unit w/reboiler overheads condenser, glycol flash

separator, two (2) Kimray Model 21015PV glycol circulation pumps, and 0.6 MMBtu/hr

reboiler heater

Company Equipment ID: DHY1

Company Equipment Description: 20 MMCFD TEG dehydration unit w/reboiler overheads condenser, glycol flash

separator, two (2) Kimray Model 21015PV glycol circulation pumps, and 0.6 MMBtu/hr

reboiler heater

Operating Status: Operating

Initial Construction Commencement 01/27/2015

Date

Initial Operation Commencement 01/27/2015

Date

Most Recent

Construction/Modification

Commencement Date:

Most Recent Operation

Commencement Date:

Permitted Emissions

| Pollutant | Potential Emissions (Lbs/hour) | Potential Emissions (Tons/Year) | | Allowable Emissions (Tons/Year | Comments |
|-----------|--------------------------------------|---------------------------------------|------------|--------------------------------------|----------|
| 1 | (LDS/HOUL) | (Tons/Year) | (LDS/MOUI) | (Tons/Year | |

Processes

- Emission Process Information

Process ID: PRC002

Process Name: TEG dehydration unit

 $\begin{center} \textbf{Company Process Description: } \textbf{TEG dehydration unit} \\ \end{center}$

Source Classification Code (SCC): 3-10-002-27

Control equipment(s) directly associated with this process

CON001

AQD Emissions Unit ID: ENGO01

Emission Unit Type: Engine

Name Plate Rating: 57.00

Units: hp

Site Rating: 57.00

Units: hp

Primary Fuel Type: Diesel

Secondary Fuel Type: Diesel

Model Name and Number: DCA-45USI2 (Isuzu 4JJ1T)

Engine: Compression Ignition

AQD Description:

Company Equipment ID: ENG001

Company Equipment Description: 57-hp WhisperWatt portable diesel generator engine

Operating Status: Not Yet Installed

Initial Construction Commencement

Date

Initial Operation Commencement

Date

Most Recent

Construction/Modification

Commencement Date:

Most Recent Operation

Commencement Date:

Serial Number Tracking

| Serial Number | | Constructio n/Installatio n Commence ment Date | Commence ment/Start- | Manufactur e Date | Shutdown Date | Removal Date |
|------------------|-----------------------|------------------------------------------------------------|-------------------------|----------------------|------------------|-----------------|
| 8202006 | WhisperWat t/Isuzu | | | | | |

- Permitted Emissions

| Pollutant | Potential Emissions | Emissions | Allowable Emissions | Allowable Emissions | Comments |
|-----------|------------------------|-------------|------------------------|------------------------|----------|
| | (Lbs/hour) | (Tons/Year) | (Lbs/Hour) | (Tons/Year | |

Processes

- Emission Process Information

Process ID: PRC029

Process Name: diesel generator

 ${\bf Company\ Process\ Description:\ diesel\ generator}$

Source Classification Code (SCC): 2-02-001-02

Release points(s) directly associated with this process

AQD Emissions Unit ID: FLR001

Emission Unit Type: Flare

Maximum Design Capacity: 200000000.0 Units: scf/day

Minimum Design Capacity: 0.01 Units: scf/day

Pilot Gas Volume (scf/min): 1.0800

AQD Description: Flare to control dehydration unit and for emergency/upset/maintenance activities

Company Equipment ID: FL1

Company Equipment Description: Flare to control dehydration unit and for emergency/upset/maintenance activities

Operating Status: Operating

Initial Construction Commencement 01/27/2015

Date:

Initial Operation Commencement 01/27/2015

Date:

Most Recent

Construction/Modification

Commencement Date:

Most Recent Operation Commencement Date:

Permitted Emissions

| Pollutant Potential Potential Emissions (Lbs/hour) (Tons/Year) | Allowable Emissions (Lbs/Hour) | Allowable Emissions (Tons/Year | Comments |
|----------------------------------------------------------------|--------------------------------------|--------------------------------------|----------|
|----------------------------------------------------------------|--------------------------------------|--------------------------------------|----------|

Processes

- Emission Process Information

Process ID: PRCCO1

Process Name: flare

Company Process Description: flare

Source Classification Code (SCC): 3-10-001-60

Release points(s) directly associated with this process

AQD Emissions Unit ID: FLR002

Emission Unit Type: Flare

Maximum Design Capacity: 31000.0

Units: scf/day

Minimum Design Capacity: 6000.0

Units: scf/day

Pilot Gas Volume (scf/min): 0.2800

AQD Description: 48" x 12' Cimarron standard enclosed combustion device

Company Equipment ID: FL2

Company Equipment Description: 48" x 12' Cimarron standard enclosed combustion device

Operating Status: Operating

Initial Construction Commencement 01/27/2015

Date:

Initial Operation Commencement 01/27/2015

Date:

Most Recent

Construction/Modification

Commencement Date:

Most Recent Operation

Commencement Date:

Permitted Emissions

| Pollutant Potential Potential Allowable Emissions (Lbs/hour) (Tons/Year) Allowable Emissions (Tons/Year) (Lbs/Hour) (Tons/Year) |
|---------------------------------------------------------------------------------------------------------------------------------|
|---------------------------------------------------------------------------------------------------------------------------------|

Processes

Emission Process Information

Process ID: PRC006

Process Name: 48"x12' LV Cimarron ECD

Company Process Description: 48"x12' LV Cimarron ECD

Source Classification Code (SCC): 3-10-001-60

Release points(s) directly associated with this process

AQD Emissions Unit ID: FLR003

Emission Unit Type: Flare

Maximum Design Capacity: 31000.0 Units: scf/day

Minimum Design Capacity: 6000.0 Units: scf/day

Pilot Gas Volume (scf/min): 0.2800

AQD Description: 48" x 12' Cimarron standard enclosed combustion device (Water Transfer Facility)

Company Equipment ID: FL3

Company Equipment Description: 48" \times 12' Cimarron standard enclosed combustion device

Operating Status: Not Yet Installed

Initial Construction Commencement

Date:

Initial Operation Commencement

Date:

Most Recent

Construction/Modification

Commencement Date:

Most Recent Operation Commencement Date:

Permitted Emissions

| Potential Emissions (Lbs/hour) | Potential Emissions (Tons/Year) | Allowable Emissions (Lbs/Hour) | Allowable Emissions (Tons/Year | Comments | |
|--------------------------------|---------------------------------------|--------------------------------------|--------------------------------------|----------|--|
|--------------------------------|---------------------------------------|--------------------------------------|--------------------------------------|----------|--|

- Processes

- Emission Process Information

Process ID: PRC009

Process Name: 48"x12' LV Cimarron ECD

Company Process Description: 48"x12' LV Cimarron ECD

Source Classification Code (SCC): 3-10-001-60

Release points(s) directly associated with this process

AQD Emissions Unit ID: FUG001

Emission Unit Type: Fugitive

AQD Description: process fugitives

Company Equipment ID: FUG1

Company Equipment Description: process fugitives

Operating Status: Operating

Initial Construction Commencement 01/27/2015

Date:

Initial Operation Commencement 01/27/2015

Date:

Most Recent

Construction/Modification

Commencement Date:

Most Recent Operation Commencement Date:

Permitted Emissions

| Pollutant | Potential Emissions (Lbs/hour) | Potential Emissions (Tons/Year) | Allowable Emissions (Lbs/Hour) | Allowable Emissions (Tons/Year | Comments | |
|-----------|--------------------------------------|---------------------------------------|--------------------------------------|--------------------------------------|----------|--|
|-----------|--------------------------------------|---------------------------------------|--------------------------------------|--------------------------------------|----------|--|

- Processes

- Emission Process Information

Process ID: PRC022

Process Name: fugitive emissions

Company Process Description: fugitive emissions

Source Classification Code (SCC): 3-10-888-11

AQD Emissions Unit ID: HET001

Emission Unit Type: Heater/Chiller

Firing Type: Indirect

Heat Input Rating: 0.5

Units: MMBtu/hr

Primary Fuel Type: Field Gas

Secondary Fuel Type: Field Gas

Heat Content of Fuel (BTU/scf): 1565

AQD Description: 0.5 MMBtu/hr tank heater

Company Equipment ID: HET1

Company Equipment Description: tank heater

Operating Status: Operating

Initial Construction Commencement 01/27/2015

Date:

Initial Operation Commencement 01/27/2015

Date:

Most Recent

Construction/Modification

Commencement Date:

Most Recent Operation Commencement Date:

Permitted Emissions

| Pollutant | Potential Emissions | Potential Emissions | Allowable Emissions | Allowable Emissions | Comments |
|---------------|------------------------|------------------------|------------------------|------------------------|----------|
| Landau Landau | (Lbs/hour) | (Tons/Year) | (Lbs/Hour) | (Tons/Year | |

Processes

- Emission Process Information

Process ID: PRC021

Process Name: tank heater

Company Process Description: tank heater

Source Classification Code (SCC): 3-10-004-04

Release points(s) directly associated with this process

AQD Emissions Unit ID: HET002

Emission Unit Type: Heater/Chiller

Firing Type: Indirect

Heat Input Rating: 0.5

Primary Fuel Type: Field Gas

Secondary Fuel Type: Field Gas

Units: MMBtu/hr

Heat Content of Fuel (BTU/scf): 1565

AQD Description: 0.5 MMBtu/hr Tank Heater

Company Equipment ID: HET2

Company Equipment Description: tank heater

Operating Status: Operating

Initial Construction Commencement 01/27/2015

Date:

Initial Operation Commencement 01/27/2015

Date:

Most Recent

Construction/Modification

Commencement Date:

Most Recent Operation Commencement Date:

Permitted Emissions

| Pollutant | Potential Emissions | Potential Emissions | | Allowable Emissions | Comments |
|-----------|------------------------|------------------------|------------|------------------------|----------|
| 1 | (Lbs/hour) | (Tons/Year) | (Lbs/Hour) | (Tons/Year | |

Processes

Emission Process Information

Process ID: PRC020

Process Name: tank heater

Company Process Description: tank heater

Source Classification Code (SCC): 3-10-004-04

Release points(s) directly associated with this process

AQD Emissions Unit ID: HET003

Emission Unit Type: Heater/Chiller

Firing Type: Indirect

Heat Input Rating: 0.5

Units: MMBtu/hr

Primary Fuel Type: Field Gas

Secondary Fuel Type: Field Gas

Heat Content of Fuel (BTU/scf): 1565

AQD Description: 0.5 MMBtu/hr tank heater

Company Equipment ID: HET3

Company Equipment Description: tank heater

Operating Status: Not Yet Installed

Initial Construction Commencement

Date

Initial Operation Commencement

Date

Most Recent

Construction/Modification

Commencement Date:

Most Recent Operation Commencement Date:

Permitted Emissions

| Pollutant | Potential Emissions | | Emissions | Emissions | Comments |
|-----------|------------------------|-------------|------------|------------|----------|
| | (Lbs/hour) | (Tons/Year) | (Lbs/Hour) | (Tons/Year | |

- Processes

- Emission Process Information

Process ID: PRC019

Process Name: tank heater

Company Process Description: tank heater

Source Classification Code (SCC): 3-10-004-04

Release points(s) directly associated with this process

AQD Emissions Unit ID: HET004

Emission Unit Type: Heater/Chiller

Firing Type: Indirect

Heat Input Rating: 0.25

Units: MMBtu/hr

Primary Fuel Type: Field Gas

Secondary Fuel Type: Field Gas

Heat Content of Fuel (BTU/scf): 1565

AQD Description: 0.25 MMBtu/hr Line Heater

Company Equipment ID: HET4

Company Equipment Description: line heater

Operating Status: Not Yet Installed

Initial Construction Commencement

Date

Initial Operation Commencement

Date

Most Recent

Construction/Modification

Commencement Date:

Most Recent Operation Commencement Date:

Permitted Emissions

| Pollutant | Potential Emissions (Lbs/hour) | Potential Emissions (Tons/Year) | Allowable Emissions (Lbs/Hour) | Allowable Emissions (Tons/Year | Comments |
|-----------|--------------------------------------|---------------------------------------|--------------------------------------|--------------------------------------|----------|
|-----------|--------------------------------------|---------------------------------------|--------------------------------------|--------------------------------------|----------|

- Processes

- Emission Process Information

Process ID: PRC018

Process Name: Line Heater

Company Process Description: Line Heater

Source Classification Code (SCC): 3-10-004-04

Release points(s) directly associated with this process

AQD Emissions Unit ID: HET005

Emission Unit Type: Heater/Chiller

Firing Type: Indirect

Heat Input Rating: 0.6

Primary Fuel Type: Field Gas

Units: MMBtu/hr

Secondary Fuel Type: Field Gas

Heat Content of Fuel (BTU/scf): 1565

AQD Description: 0.6 MMBtu/hr reboiler heater

Company Equipment ID: HET5

Company Equipment Description: reboiler heater

Operating Status: Operating

Initial Construction Commencement 01/27/2015

Date

Initial Operation Commencement 01/27/2015

Date:

Most Recent Construction/Modification

Commencement Date:

Most Recent Operation Commencement Date:

Permitted Emissions

| Pollutant | Potential Emissions | Potential Emissions | Allowable Emissions (Lbs/Hour) | Allowable Emissions (Tons/Year | Comments |
|-----------|------------------------|------------------------|--------------------------------------|--------------------------------------|----------|
| | (Lbs/hour) | (Tons/Year) | (LDS/HOUL) | (Tons/Year | |

- Processes

- Emission Process Information

Process ID: PRC023

Process Name: reboiler heater

Company Process Description: reboiler heater

Source Classification Code (SCC): 3-10-002-28

Release points(s) directly associated with this process

AQD Emissions Unit ID: LUD001

Emission Unit Type: Loading/Unloading/Dump

Type of Material: liquid

Material Description: 60 bbl/day condensate loading

Maximum Annual Throughput: 21900

Units: barrels/yr

AQD Description: truck loading from condensate tanks

Company Equipment ID: TL01

Company Equipment Description: truck loading from condensate tanks

Operating Status: Operating

Initial Construction Commencement 01/27/2015

Date

Initial Operation Commencement 01/27/2015

Date:

Most Recent

Construction/Modification

Commencement Date:

Most Recent Operation Commencement Date:

- Permitted Emissions

| (Lbs/hour) ((lons/year) ((lbs/Hour) ((lons/year) | | | Potential Emissions (Tons/Year) | Allowable Emissions (Lbs/Hour) | Allowable Emissions (Tons/Year | Comments |
|---------------------------------------------------|--|--|---------------------------------------|--------------------------------------|--------------------------------------|----------|
|---------------------------------------------------|--|--|---------------------------------------|--------------------------------------|--------------------------------------|----------|

Processes

- Emission Process Information

Process ID: PRC026

Process Name: truck loadout

Company Process Description: truck loadout Source Classification Code (SCC): 4-06-001-32

Release points(s) directly associated with this process

AQD Emissions Unit ID: SEP001

Emission Unit Type: Separator/Treater

Type Of Vessel: 3-Phase Separator is Vessel Heated: No

AQD Description: unheated 9'x30' horizontal inlet separator (slug catcher)

Company Equipment ID: SEP1

Company Equipment Description: unheated 9'x30' horizontal inlet separator (slug catcher)

Operating Status: Operating

Initial Construction Commencement 01/27/2015

Date:

Initial Operation Commencement 01/27/2015

Date:

Most Recent

Construction/Modification

Commencement Date:

Most Recent Operation Commencement Date:

Permitted Emissions

| Pollutant Potential Emissions (Lbs/hour) (Tons/Year) | Emissions | Allowable Emissions (Tons/Year | Comments |
|------------------------------------------------------|-----------|--------------------------------------|----------|
|------------------------------------------------------|-----------|--------------------------------------|----------|

Processes

- Emission Process Information

Process ID: PRC024

Process Name: inlet separator

Company Process Description: inlet separator

Source Classification Code (SCC): 3-10-001-07

AQD Emissions Unit ID: SEP002

Emission Unit Type: Separator/Treater

Type Of Vessel: 2-Phase Separator is Vessel Heated: No

AQD Description: unheated 60"x20' horizontal separator (flare knockout)

Company Equipment ID: SEP1

Company Equipment Description: unheated 60"x20' horizontal separator (flare knockout)

Operating Status: Operating

Initial Construction Commencement 01/27/2015

Date:

Initial Operation Commencement 01/27/2015

Date:

Most Recent

Construction/Modification

Commencement Date:

Most Recent Operation Commencement Date:

Permitted Emissions

| Pollutant | Potential Emissions | Potential Emissions (Tons/Year) | Allowable Emissions (Lbs/Hour) | Allowable Emissions (Tons/Year | Comments |
|-----------|------------------------|---------------------------------------|--------------------------------------|--------------------------------------|----------|
| 1 | (Lbs/hour) | (Tons/Year) | (LDS/HOUL) | (Tons/rear | |

Processes

- Emission Process Information

Process ID: PRC025

Process Name: flare knockout
Company Process Description: flare knockout
Source Classification Code (SCC): 3-10-001-07

AQD Emissions Unit ID: TNK001

Emission Unit Type: Storage Tank/Silo

Material Type: Liquid

Description of Material Stored: condensate liquid storage (60 bbls/day total)

Capacity: 400

Units: barrels

Maximum Throughput: 30.0000

Units: barrels/day

AQD Description: 400-bbl condensate storage tank

Company Equipment ID: T1

Company Equipment Description: 400-bbl condensate storage tank

Operating Status: Operating

Initial Construction Commencement 01/27/2015

Date

Initial Operation Commencement 01/27/2015

Date:

Most Recent

Construction/Modification

Commencement Date:

Most Recent Operation Commencement Date:

Permitted Emissions

| Pollutant | Potential Emissions (Lbs/hour) | Potential Emissions (Tons/Year) | Allowable Emissions (Lbs/Hour) | Allowable Emissions (Tons/Year | Comments |
|-----------|--------------------------------------|---------------------------------------|--------------------------------------|--------------------------------------|----------|
| | (LDS/HOUL) | (Tolls/Teal) | (Lusi loui) | (TOHS/Teal | |

- Processes

- Emission Process Information

Process ID: PRC003

Process Name: condensate storage tank

Company Process Description: condensate storage tank

Source Classification Code (SCC): 4-04-003-11

Control equipment(s) directly associated with this process

AQD Emissions Unit ID: TNK002

Emission Unit Type: Storage Tank/Silo

Material Type: Liquid

Description of Material Stored: condensate liquid storage (60 bbls/day total)

Capacity: 400

Units: barrels

Maximum Throughput: 30,0000

Units: barrels/day

AQD Description: 400-bbl condensate storage tank

Company Equipment ID: T2

Company Equipment Description: 400-bbl condensate storage tank

Operating Status: Not Yet Installed

Initial Construction Commencement

Date

Initial Operation Commencement

Date

Most Recent

Construction/Modification

Commencement Date:

Most Recent Operation Commencement Date:

- Permitted Emissions

| Pollutant |
|-----------|
|-----------|

- Processes

- Emission Process Information

Process ID: PRC004

Process Name: condensate storage tank

Company Process Description: condensate storage tank

Source Classification Code (SCC): 4-04-003-11

Control equipment(s) directly associated with this process

AQD Emissions Unit ID: TNK003

Emission Unit Type: Storage Tank/Silo

Material Type: Liquid

Description of Material Stored: water storage tank (25 bbls/day total)

Capacity: 400

Maximum Throughput: 25.0000

Units: barrels

Units: barrels/day

AQD Description: 400-bbl water storage tank

Company Equipment ID: T3

Company Equipment Description: 400-bbl water storage tank

Operating Status: Operating

Initial Construction Commencement 01/27/2015

Date:

Initial Operation Commencement 01/27/2015

Date:

Most Recent

Construction/Modification

Commencement Date:

Most Recent Operation Commencement Date:

Permitted Emissions

| Pollutant | Potential Emissions (Lbs/hour) | Potential Emissions (Tons/Year) | Allowable Emissions (Lbs/Hour) | Allowable Emissions (Tons/Year | Comments | |
|-----------|--------------------------------------|---------------------------------------|--------------------------------------|--------------------------------------|----------|--|
|-----------|--------------------------------------|---------------------------------------|--------------------------------------|--------------------------------------|----------|--|

- Processes

- Emission Process Information

Process ID: PRC005

Process Name: produced water storage tank

Company Process Description: produced water storage tank

Source Classification Code (SCC): 4-04-003-15

Control equipment(s) directly associated with this process

AQD Emissions Unit ID: TNK004

Emission Unit Type: Storage Tank/Silo

Material Type: Liquid

Description of Material Stored: methanol

Capacity: 6000

Maximum Throughput: 54000.0000

Units: gallons Units: gallons/yr

AQD Description: 6000 gallon storage tank

Company Equipment ID: T4

Company Equipment Description: 6000 gallon methanol storage tank

Operating Status: Not Yet Installed

Initial Construction Commencement

Initial Operation Commencement

Most Recent

Construction/Modification

Commencement Date:

Most Recent Operation

Commencement Date:

Permitted Emissions

| (Lbs/hour) (Tons/Year) (Lbs/Hour) (Tons/Year |
|----------------------------------------------|
|----------------------------------------------|

Processes

Emission Process Information

Process ID: PRC008

Process Name: methanol storage tank

Company Process Description: methanol storage tank

Source Classification Code (SCC): 4-07-008-16

Release points(s) directly associated with this process

Units: gallons

Units: gallons/yr

- Emission Unit Information

AQD Emissions Unit ID: TNK005

Emission Unit Type: Storage Tank/Silo

Material Type: Liquid

Description of Material Stored: methanol

Capacity: 6000

Maximum Throughput: 54000.0000

AQD Description: 6000 gallon methanol storage tank

Company Equipment ID: T5

Company Equipment Description: 6000 gallon methanol storage tank

Operating Status: Not Yet Installed

Initial Construction Commencement

Date

Initial Operation Commencement

Date:

Most Recent

Construction/Modification

Commencement Date:

Most Recent Operation Commencement Date:

- Permitted Emissions

| Emissions Em | tential Allowable Emissions Emissions ons/Year) (Lbs/Hour) | Allowable Emissions (Tons/Year | Comments |
|--------------|------------------------------------------------------------------|--------------------------------------|----------|
|--------------|------------------------------------------------------------------|--------------------------------------|----------|

- Processes

- Emission Process Information

Process ID: PRC007

Process Name: methanol storage tank

 $Company \ Process \ Description: \ methanol \ storage \ tank$

Source Classification Code (SCC): 4-07-008-16

Release points(s) directly associated with this process

Units: barrels

Units: barrels/day

Emission Unit Information

AQD Emissions Unit ID: TNK006

Emission Unit Type: Storage Tank/Silo

Material Type: Liquid

Description of Material Stored: water storage tank

Capacity: 500

Dapacity, 500

Maximum Throughput: 4000.0000

AQD Description: 500-bbl water storage tank

Company Equipment ID: T6

Company Equipment Description: 500-bbl water storage tank

Operating Status: Not Yet Installed

Initial Construction Commencement

Date:

Initial Operation Commencement

Date

Most Recent

Construction/Modification

Commencement Date:

Most Recent Operation Commencement Date:

- Permitted Emissions

| Pollutant | Potential Emissions (Lbs/hour) | Potential Emissions | Allowable Emissions | Allowable Emissions | Comments |
|-----------|--------------------------------------|------------------------|------------------------|------------------------|----------|
| | (LDS/HOUL) | (Tons/Year) | (Lbs/Hour) | (Tons/Year | |

- Processes

- Emission Process Information

Process ID: PRC010

Process Name: produced water storage tank

Company Process Description: produced water storage tank

Source Classification Code (SCC): 4-04-003-15

Control equipment(s) directly associated with this process

AQD Emissions Unit ID: TNK007

Emission Unit Type: Storage Tank/Silo

Material Type: Liquid

Description of Material Stored: water storage tank

Capacity: 500

Units: barrels

Maximum Throughput: 4000.0000

Units: barrels/day

AQD Description: 500-bbl water storage tank

Company Equipment ID: T7

Company Equipment Description: 500-bbl water storage tank

Operating Status: Not Yet Installed

Initial Construction Commencement

Date

Initial Operation Commencement

Date

Most Recent

Construction/Modification

Commencement Date:

Most Recent Operation Commencement Date:

Permitted Emissions

| Emissions Emissions Emissions (Lbs/hour) (Tons/Year) (Lbs/Hour) (Tons/Year |
|----------------------------------------------------------------------------|
|----------------------------------------------------------------------------|

Processes

- Emission Process Information

Process ID: PRC011

Process Name: produced water storage tank

 $\label{lem:company-process} \textbf{Company Process Description:} \ \ \texttt{produced water storage tank}$

Source Classification Code (SCC): 4-04-003-15

Control equipment(s) directly associated with this process

Units: barrels

Units: barrels/day

- Emission Unit Information

AQD Emissions Unit ID: TNK008

Emission Unit Type: Storage Tank/Silo

Material Type: Liquid

Description of Material Stored: water storage tank

Capacity: 500

Maximum Throughput: 4000.0000

AQD Description: 500-bbl water storage tank

Company Equipment ID: T8

Company Equipment Description: 500-bbl water storage tank

Operating Status: Not Yet Installed

Initial Construction Commencement

Date

Initial Operation Commencement

Date

Most Recent

Construction/Modification

Commencement Date:

Most Recent Operation Commencement Date:

- Permitted Emissions

| Pollutant | Potential Emissions (Lbs/hour) | | Emissions | Allowable Emissions (Tons/Year | Comments |
|-----------|--------------------------------------|--------------|--------------|--------------------------------------|----------|
| | (LDOTTIOUT) | (10110/1041) | (LDOIT TOUT) | (10110/1041 | |

- Processes

- Emission Process Information

Process ID: PRC012

Process Name: produced water storage tank

Company Process Description: produced water storage tank

Source Classification Code (SCC): 4-04-003-15

Control equipment(s) directly associated with this process

Units: barrels
Units: barrels/day

- Emission Unit Information

AQD Emissions Unit ID: TNK009

Emission Unit Type: Storage Tank/Silo

Material Type: Liquid

Description of Material Stored: water storage tank

Capacity: 500

Maximum Throughput: 4000.0000

AQD Description: 500-bbl water storage tank

Company Equipment ID: T9

Company Equipment Description: 500-bbl water storage tank

Operating Status: Not Yet Installed

Initial Construction Commencement

Date

Initial Operation Commencement

Date:

Most Recent

Construction/Modification

Commencement Date:

Most Recent Operation Commencement Date:

- Permitted Emissions

| Pollutant Potential Emissions (Lbs/hour | | Allowable Emissions (Lbs/Hour) | Allowable Emissions (Tons/Year | Comments | |
|-----------------------------------------|--|--------------------------------------|--------------------------------------|----------|--|
|-----------------------------------------|--|--------------------------------------|--------------------------------------|----------|--|

Processes

- Emission Process Information

Process ID: PRC013

Process Name: produced water storage tank

Company Process Description: produced water storage tank

Source Classification Code (SCC): 4-04-003-15

Control equipment(s) directly associated with this process

Units: barrels

Units: barrels/day

- Emission Unit Information

AQD Emissions Unit ID: TNK010

Emission Unit Type: Storage Tank/Silo

Material Type: Liquid

Description of Material Stored: water storage tank

Capacity: 500

Maximum Throughput: 4000.0000

AQD Description: 500-bbl water storage tank

Company Equipment ID: T10

Company Equipment Description: 500-bbl water storage tank

Operating Status: Not Yet Installed

Initial Construction Commencement

Date:

Initial Operation Commencement

Date:

Most Recent

Construction/Modification Commencement Date:

Most Recent Operation Commencement Date:

Permitted Emissions

| Pollutant | Potential Emissions (Lbs/hour) | Potential Emissions (Tons/Year) | Allowable Emissions (Lbs/Hour) | Allowable Emissions (Tons/Year | Comments |
|-----------|--------------------------------------|---------------------------------------|--------------------------------------|--------------------------------------|----------|
|-----------|--------------------------------------|---------------------------------------|--------------------------------------|--------------------------------------|----------|

- Processes

- Emission Process Information

Process ID: PRC014

Process Name: produced water storage tank

Company Process Description: produced water storage tank

Source Classification Code (SCC): 4-04-003-15

Control equipment(s) directly associated with this process

Units: gallons

Units: gallons/yr

- Emission Unit Information

AQD Emissions Unit ID: TNK011

Emission Unit Type: Storage Tank/Silo

Material Type: Liquid

Description of Material Stored: corrosion inhibitor

Capacity: 6000

Maximum Throughput: 72000.0000

AQD Description: 6000 gallon storage tank

Company Equipment ID: T11

Company Equipment Description: 6000 gallon storage tank

Operating Status: Not Yet Installed

Initial Construction Commencement

Date

Initial Operation Commencement

Date

Most Recent

Construction/Modification

Commencement Date:

Most Recent Operation Commencement Date:

- Permitted Emissions

| Pollutant Potential Potential Emissions (Lbs/hour) (Tons/Year) | Allowable Emissions (Lbs/Hour) | Allowable Emissions (Tons/Year | Comments |
|----------------------------------------------------------------|--------------------------------------|--------------------------------------|----------|
|----------------------------------------------------------------|--------------------------------------|--------------------------------------|----------|

- Processes

- Emission Process Information

Process ID: PRC015

Process Name: chemical tank

Company Process Description: chemical tank

Source Classification Code (SCC): 4-07-999-99

Release points(s) directly associated with this process

Units: gallons

Units: gallons/yr

Emission Unit Information

AQD Emissions Unit ID: TNK012

Emission Unit Type: Storage Tank/Silo

Material Type: Liquid

Description of Material Stored: paraffin inhibitor

Capacity: 6000

Maximum Throughput: 72000.0000

AQD Description: 6000 gallon storage tank

Company Equipment ID: T12

Company Equipment Description: 6000 gallon storage tank

Operating Status: Not Yet Installed

Initial Construction Commencement

Initial Operation Commencement

Most Recent

Construction/Modification

Commencement Date:

Most Recent Operation Commencement Date:

Permitted Emissions

| Pollutant | Potential Emissions (Lbs/hour) | Potential Emissions (Tons/Year) | Allowable Emissions (Lbs/Hour) | Allowable Emissions (Tons/Year | Comments |
|-----------|--------------------------------------|---------------------------------------|--------------------------------------|--------------------------------------|----------|
| | (LD3/110d1) | (Tollar Car) | (LD3/110di) | (10113/10a) | |

Processes

Emission Process Information

Process ID: PRC016

Process Name: chemical tank

Company Process Description: chemical tank

Source Classification Code (SCC): 4-07-999-99

Release points(s) directly associated with this process

AQD Emissions Unit ID: TNK013

Emission Unit Type: Storage Tank/Silo

Material Type: Liquid

Description of Material Stored: emulsion breaker

Capacity: 6000

Units: gallons

Maximum Throughput: 72000.0000

Units: gallons/yr

AQD Description: 6000 gallon storage tank

Company Equipment ID: T13

Company Equipment Description: 6000 gallon storage tank

Operating Status: Not Yet Installed

Initial Construction Commencement

Date

Initial Operation Commencement

Date

Most Recent

Construction/Modification

Commencement Date:

Most Recent Operation Commencement Date:

- Permitted Emissions

| Pollutant Potential Potential Emissions (Lbs/hour) Potential Emissions (Lbs/hour) Allowable Emissions (Lbs/Hour) Allowable Emissions (Lbs/Hour) Comment (Lbs/Hour) |
|--------------------------------------------------------------------------------------------------------------------------------------------------------------------|
|--------------------------------------------------------------------------------------------------------------------------------------------------------------------|

Processes

- Emission Process Information

Process ID: PRC017

Process Name: chemical tank

Company Process Description: chemical tank

Source Classification Code (SCC): 4-07-999-99

Release points(s) directly associated with this process

Control Equipment Information

Equipment Type: Condenser

Control Equipment ID: CON001

AQD Description: reboiler overheads condenser

Company Control Equipment ID: CON1

Company Control Equipment reboiler overheads condenser

Description:

Operating Status: Operating

Initial Installation Date: 01/27/2015

Model:

Manufacturer: Specific Equipment Type information

Condenser Type: Indirect Contact

Coolant Type: atmospheric air

Design Coolant Temp Range:

Design Coolant Flow Rate:

Max. Exhaust Gas Temp: 100

Inlet Gas Flow Rate:

Outlet Gas Flow Rate:

Inlet Gas Temp:

Operating Pressure: 12

Outlet Gas Temp:

- Pollutants Controlled

| Pollutant | Design Control Efficiency(%) | Operating Control Efficiency(%) | Capture Efficiency(%) | Total Capture Control(%) |
|-------------------------------------|---------------------------------|---------------------------------------|--------------------------|-----------------------------|
| Total HAP Pollutants | 98 | 98 | 100 | 98 |
| VOC - Volatile Organic Compounds | 98 | 98 | 100 | 98 |

Associated Control Equipments And Release Points

Control equipment(s) directly associated with this control equipment

Control Equipment Information

Equipment Type: Flare

Control Equipment ID: FLA001

AQD Description: 60 ft Flare Industries flare

Company Control Equipment ID: FL1

Company Control Equipment 60 ft Flare Industries flare

Manufacturer: Flare Industries

Description:

Operating Status: Operating

Initial Installation Date: 01/27/2015

Model:

Specific Equipment Type information

Flare Type: Elevated - Open

Elevated Flare Type: Air-Assisted

Ignition Device: Yes

Flame Presence Sensor: Yes

Inlet Gas Temp:

Flame Presence Type: Thermocouple

Gas Flow Rate:

Sec. Outlet Gas Temp:

- Pollutants Controlled

| Pollutant | Design Control Efficiency(%) | Operating Control Efficiency(%) | Capture Efficiency(%) | Total Capture Control(%) |
|-------------------------------------|---------------------------------|---------------------------------------|--------------------------|-----------------------------|
| Total HAP Pollutants | 98 | 98 | 100 | 98 |
| VOC - Volatile Organic Compounds | 98 | 98 | 100 | 98 |

Associated Control Equipments And Release Points

Release points(s) directly associated with this control equipment

- Control Equipment Information

Equipment Type: Flare

Control Equipment ID: FLA002

AQD Description: 48"x12' LV Cimarron ECD

Company Control Equipment ID: FL2

Company Control Equipment 48"x12' LV Cimarron ECD

Description:

Operating Status: Operating

Manufacturer: Cimarron

Initial Installation Date: 01/27/2015

Model: 48"x12' LV

- Specific Equipment Type information

Flare Type: Enclosed

Elevated Flare Type: Non-Assisted

Ignition Device: Yes

Flame Presence Sensor: Yes

Inlet Gas Temp:

Flame Presence Type: Thermocouple

Gas Flow Rate:

Sec. Outlet Gas Temp:

- Pollutants Controlled

| Pollutant | Design Control Efficiency(%) | Operating Control Efficiency(%) | Capture Efficiency(%) | Total Capture Control(%) |
|-------------------------------------|---------------------------------|---------------------------------------|--------------------------|-----------------------------|
| Total HAP Pollutants | 98 | 98 | 100 | 98 |
| VOC - Volatile Organic Compounds | 98 | 98 | 100 | 98 |

- Associated Control Equipments And Release Points

Release points(s) directly associated with this control equipment

Control Equipment Information

Equipment Type: Flare

Control Equipment ID: FLA003

AQD Description: 48"x12' LV Cimarron ECD

Company Control Equipment ID: FL3

Company Control Equipment 48"x12' LV Cimarron ECD

Description:

Operating Status: Not Operating

Manufacturer: Cimarron

Initial Installation Date:

Model: 48"x12' LV

Specific Equipment Type information

Flare Type: Enclosed

Elevated Flare Type: Non-Assisted

Ignition Device: Yes

Flame Presence Sensor: Yes

Inlet Gas Temp:

Flame Presence Type: Thermocouple

Gas Flow Rate:

Sec. Outlet Gas Temp:

- Pollutants Controlled

| Pollutant | Design Control Efficiency(%) | Operating Control Efficiency(%) | Capture Efficiency(%) | Total Capture Control(%) |
|-------------------------------------|---------------------------------|---------------------------------------|--------------------------|-----------------------------|
| Total HAP Pollutants | 98 | 100 | 98 | 98 |
| VOC - Volatile Organic Compounds | 98 | 100 | 98 | 98 |

Associated Control Equipments And Release Points

Release points(s) directly associated with this control equipment

Release Point ID: AVL002

Release Type: Fugitive (Area, Volume, Line)

AQD Description: truck loading - condensate tanks

Company Release Point ID: AVL2

Company Release Point Description: truck loading - condensate tanks

Operating Status: Operating

Release Height (ft): 3.0

- Release Latitude and Longitude

Latitude: 41.0536

Longitude: -104.605

| Description | H2S | SO2 | NOX | co | THC | HCL | HFL | 0 | TRS | CO2 | FLOW | OPACITY | РМ | |
|-------------|-----|-----|-----|----|-----|-----|-----|---|-----|-----|-------------------|---------|----|---|
| | | | | | | | | | | | | | | |
| | - | | - | | | - | - | | - | - | The second second | | - | 1 |

Release Point ID: AVL001

Release Type: Fugitive (Area, Volume, Line)

AQD Description: methanol storage tank

Company Release Point ID: FUG1

Company Release Point Description: methanol storage tank

Operating Status: Operating

Release Height (ft): 10.0

- Release Latitude and Longitude

Latitude: 41.0536

Longitude: -104.605

| Description | H2S | SO2 | NOX | CO | THC | HCL | HFL | 0 | TRS | CO2 | FLOW | OPACITY | PM |
|-------------|-----|-----|-----|----|-----|-----|-----|---|-----|-----|------|---------|----|
| | | | | | | | | | | | | | |

Release Point ID: VER001

Release Type: Vertical

AQD Description: Flare Stack

Company Release Point ID: VER1

Company Release Point Description: Flare Stack

Operating Status: Operating

Base Elevation (ft): 5920.0

- Stack Details

Stack Height (ft): 60.0

Exit Gas Velocity (ft/s): 2.46

Exit Gas Temp (F): 1400.0

Stack Diameter (ft): 6.0

Exit Gas Flow Rate (acfm): 4167.0

- Release Latitude and Longitude

Latitude: 41.0536

Longitude: -104.605

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|-------------|-----|-----|-----|----|-----|-----|-----|---|-----|-----|------|---------|----|
| Description | H2S | SO2 | NOX | CO | THC | HCL | HFL | 0 | TRS | CO2 | FLOW | OPACITY | PM |

Release Point ID: VER009

Release Type: Vertical

AQD Description:

Company Release Point ID: VER1

Company Release Point Description: Exhaust Stack

Operating Status: Not Operating

Base Elevation (ft): 5983.0

- Stack Details

Stack Height (ft): 10.0

Exit Gas Velocity (ft/s): 120.0

Exit Gas Temp (F): 900.0

Stack Diameter (ft): 0.25

Exit Gas Flow Rate (acfm): 353.0

- Release Latitude and Longitude

Latitude: 41.0536

Longitude: -104.605

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|-------------|-----|-----|-----|----|-----|-----|-----|---|-----|-----|------|---------|----|---|
| Description | H2S | SO2 | NOX | CO | THC | HCL | HFL | 0 | TRS | CO2 | FLOW | OPACITY | PM | |

Release Point ID: VER002

Release Type: Vertical

AQD Description: 48"x12' LV Cimarron ECD

Company Release Point ID: VER2

Company Release Point Description: 48"x12' LV Cimarron ECD

Operating Status: Operating

Base Elevation (ft): 5920.0

- Stack Details

Stack Height (ft): 12.0

Exit Gas Velocity (ft/s): 44.7

Exit Gas Temp (F): 1400.0

Stack Diameter (ft): 4.0

Exit Gas Flow Rate (acfm): 16.8

- Release Latitude and Longitude

Latitude: 41.0536

Longitude: -104,605

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|-------------|-----|-----|-----|----|-----|-----|-----|---|-----|-----|------|---------|----|---|
| Description | H2S | SO2 | NOX | CO | THC | HCL | HFL | 0 | TRS | CO2 | FLOW | OPACITY | PM | |

Release Point ID: VER003

Release Type: Vertical

AQD Description: 48"x12' LV Cimarron ECD

Company Release Point ID: VER3

Company Release Point Description: 48"x12' LV Cimarron ECD

Operating Status: Operating Base Elevation (ft): 5920.0

- Stack Details

Stack Height (ft): 12.0

Exit Gas Velocity (ft/s): 44.7

Exit Gas Temp (F): 1400.0

Stack Diameter (ft): 4.0

Exit Gas Flow Rate (acfm): 16.8

Release Latitude and Longitude

Latitude: 41.0536

Longitude: -104.605

CEM Data

| | | | THE SOURCE STATE | | | | | | | | | | | Ĺ |
|-------------|-----|-----|------------------|----|-----|-----|-----|---|-----|-----|------|---------|----|---|
| Description | H2S | SO2 | NOX | CO | THC | HCL | HFL | 0 | TRS | CO2 | FLOW | OPACITY | PM | ı |

Release Point ID: VER004

Release Type: Vertical

AQD Description: tank heater stack

Company Release Point ID: VER4

Company Release Point Description: tank heater stack

Operating Status: Operating

Base Elevation (ft): 5920.0

- Stack Details

Stack Height (ft): 15.0

Exit Gas Velocity (ft/s): 50.0

Exit Gas Temp (F): 600.0

Stack Diameter (ft): 1.0

Exit Gas Flow Rate (acfm): 1.0

- Release Latitude and Longitude

Latitude: 41.0536

Longitude: -104.605

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|-----------------------------------------|-----|-----|-----|--------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------|-----|------------|-----|---|-----|-----|------|------------------------|---------|
| Description | H2S | SO2 | NOX | CO | THC | HCL | HFL | 0 | TRS | CO2 | FLOW | OPACITY | PM |
| D C C C C C C C C C C C C C C C C C C C | | | | - The state of the | | 12/19/2015 | | | | | | | Was Was |

Release Point ID: VER005

Release Type: Vertical

AQD Description: tank heater stack

Company Release Point ID: VER5

Company Release Point Description: tank heater stack

Operating Status: Operating
Base Elevation (ft): 5920.0

- Stack Details

Stack Height (ft): 15.0

Exit Gas Velocity (ft/s): 50.0

Exit Gas Temp (F): 600.0

Stack Diameter (ft): 1.0

Exit Gas Flow Rate (acfm): 1.0

Release Latitude and Longitude

Latitude: 41.0536

Longitude: -104.605

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|-------------|-----|-----|-----|----|-----|-----|-----|---|-----|-----|------|---------|----|
| Description | H2S | SO2 | NOX | CO | THC | HCL | HFL | 0 | TRS | CO2 | FLOW | OPACITY | PM |

Release Point ID: VER006

Release Type: Vertical

AQD Description: tank heater stack

Company Release Point ID: VER6

Company Release Point Description: tank heater stack

Operating Status: Operating
Base Elevation (ft): 5920.0

Stack Details

Stack Height (ft): 15.0

Exit Gas Velocity (ft/s): 50.0

Exit Gas Temp (F): 600.0

Stack Diameter (ft): 1.0

Exit Gas Flow Rate (acfm): 1.0

Release Latitude and Longitude

Latitude: 41.0536

Longitude: -104.605

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|-------------|-----|-----|-----|----|-----|-----|-----|-----|-----|-----|------|---------|----|----|
| Description | H2S | SO2 | NOX | CO | THC | HCL | HFL | 0 7 | TRS | CO2 | FLOW | OPACITY | PM | ĺ |

Release Point ID: VER007

Release Type: Vertical

AQD Description: line heater stack

Company Release Point ID: VER7

Company Release Point Description: line heater stack

Operating Status: Operating

Base Elevation (ft): 5920.0

Stack Details

Stack Height (ft): 15.0

Exit Gas Velocity (ft/s): 50.0

Exit Gas Temp (F): 600.0

Stack Diameter (ft): 1.0

Exit Gas Flow Rate (acfm): 1.0

Release Latitude and Longitude

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Latitude: 41.0536

Longitude: -104,605

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|-------------|-----|-----|-----|----|-----|-----|-----|---|-----|-----|------|---------|----|----|
| Description | H2S | SO2 | NOX | CO | THC | HCL | HFL | 0 | TRS | CO2 | FLOW | OPACITY | PM | |

Release Point ID: VER008

Release Type: Vertical

AQD Description: reboiler heater stack

Company Release Point ID: VER8

Company Release Point Description: reboiler heater stack

Operating Status: Operating Base Elevation (ft): 5920.0

- Stack Details

Stack Height (ft): 15.0

Stack Diameter (ft): 1.0

Exit Gas Velocity (ft/s): 50.0

Exit Gas Flow Rate (acfm): 1.0

Exit Gas Temp (F): 600.0

Release Latitude and Longitude

Latitude: 41,0536

Longitude: -104,605

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|-------------|-----|-----|-----|----|-----|-----|-----|---|-----|-----|------|---------|----|---|
| Description | H2S | SO2 | NOX | CO | THC | HCL | HFL | 0 | TRS | CO2 | FLOW | OPACITY | PM | |